

RUSSIAN SPACE ENGINEERING WORKSHOP
Thermally Loaded Structures

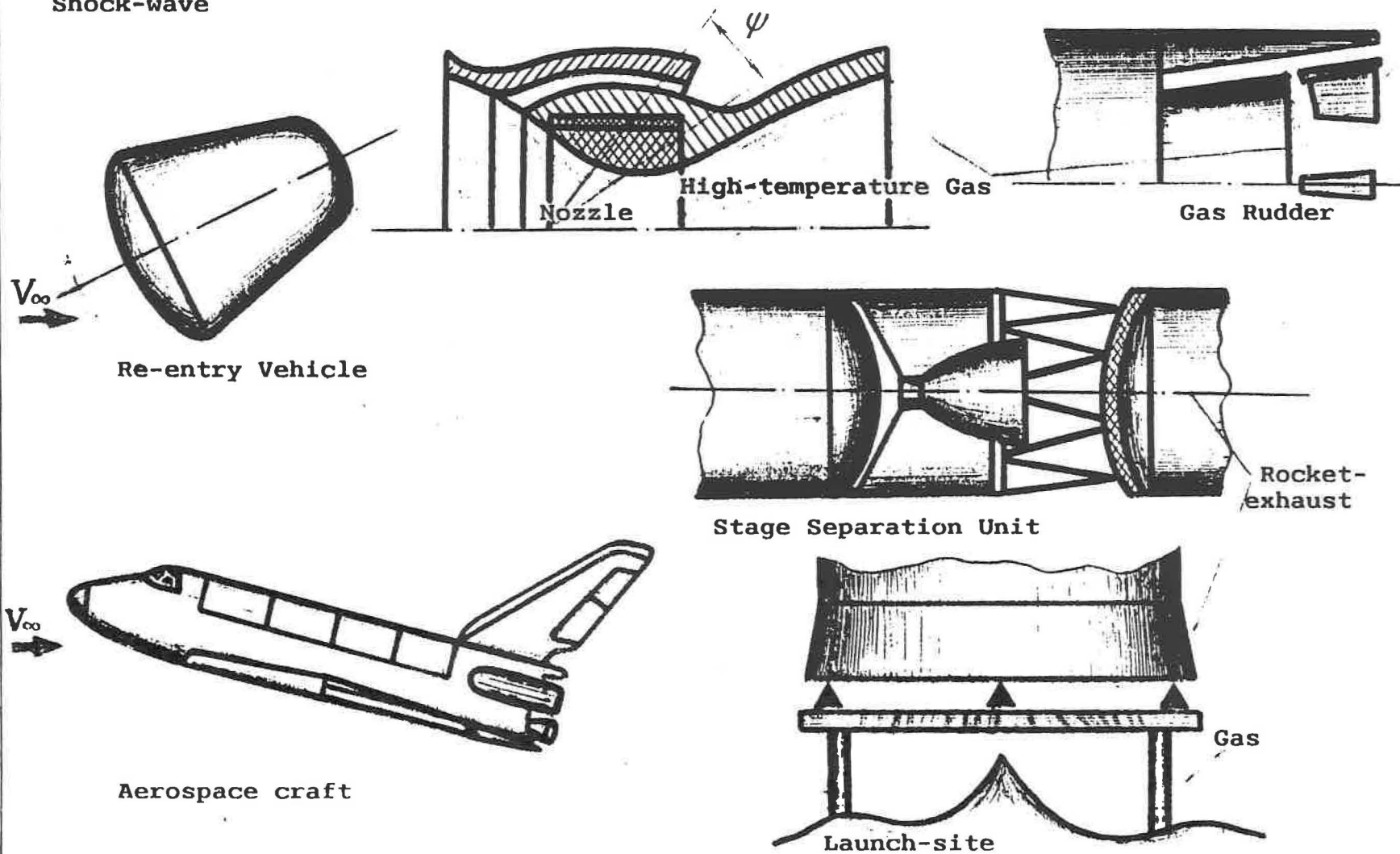
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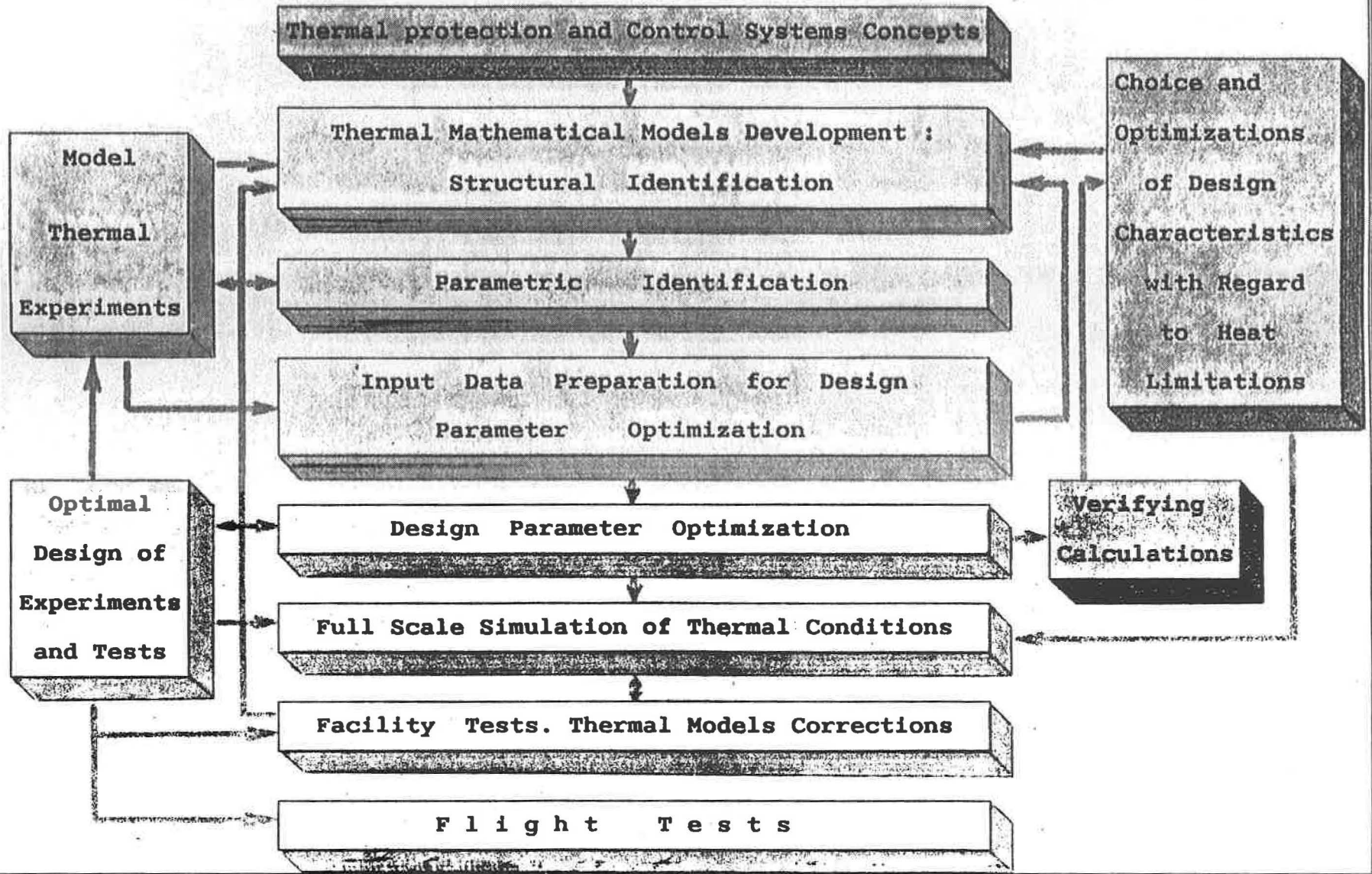
Course Notebook Contents

- I.
Introduction to Thermal Design and Testing
- II.
Direct and Inverse Problems
- III.
Statements of Inverse Heat Transfer Problems
- IV.
Practical Applications of Inverse Heat Transfer Methods
- V.
General Operator Form of an Inverse Problem and a Little on the History of the Subject Matter
- VI.
Principles of Solution for Ill-posed Problems
- VII.
Regularization of Unstable Problems by Tikhonov Method
- VIII.
Methods and Algorithms for Solving Inverse Heat Transfer Problems
Direct Semi-Analytical Methods
- IX.
Methods for Solving Linear Inverse Heat Conduction Problems for Bodies with Movable Boundaries
- X.
Numerical Solution of Nonlinear IHCP
- XI.
Artificial Hyperbolization of Heat Conduction Equation
- XII.
Tikhonov Regularization Method
- XIII.
Iterative Regularization Method
- XIV.
Comparison of Methods for Solving Boundary IHCPs
- XV.
Development and Validation of Mathematical Models of Heat Transfer
- XVI.
Application Results

I.
**Introduction to Thermal Design and
Testing**

Shock-wave





The main purpose of OTD is a determination of the design solutions and parameters of the thermal protection and control.

General statement of corresponding optimization problem:

$$\vec{p} : \min_{\vec{p} \in G} J[\vec{p}],$$

$$G = \{ \vec{p} : g_i(\vec{p}, T(\vec{x}, \tau, \vec{p})) \leq 0, i = 1, 2, \dots, l \},$$

$$T(\vec{x}, \tau, \vec{p}) = A[T(\vec{x}, \tau, \vec{p}), \vec{p}]; \quad \vec{p} \in R^k,$$

where \vec{p} is a vector of design parameters;

G is a set of admissible solutions;

$\{g_i\}_i^l$ are physical and technical restrictions;

J is a criterion function;

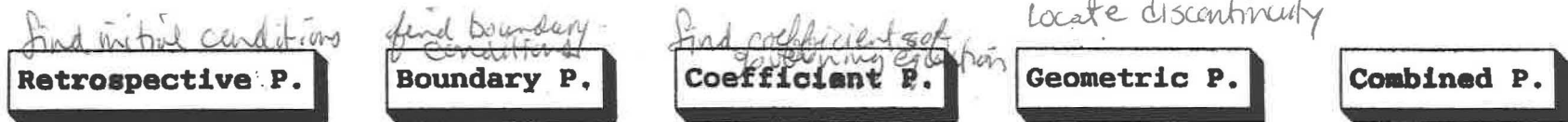
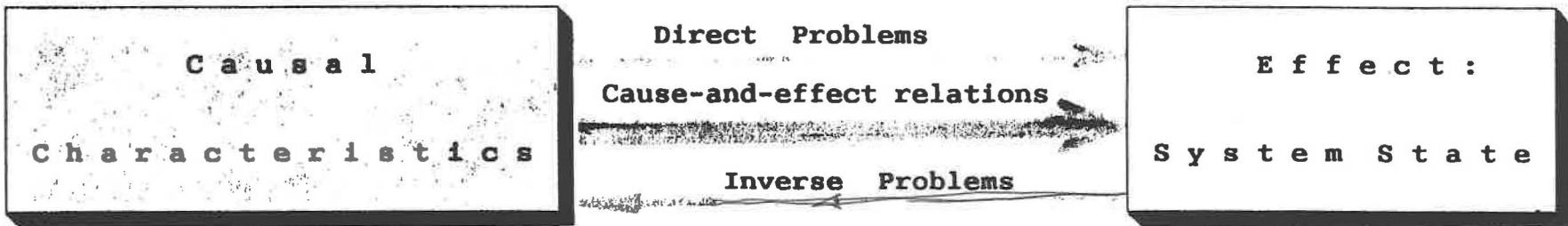
T is temperature;

τ is time;

\vec{x} is a vector of spatial variables;

A is an operator of thermal mathematical model of system under design

II.
Direct and Inverse Problems



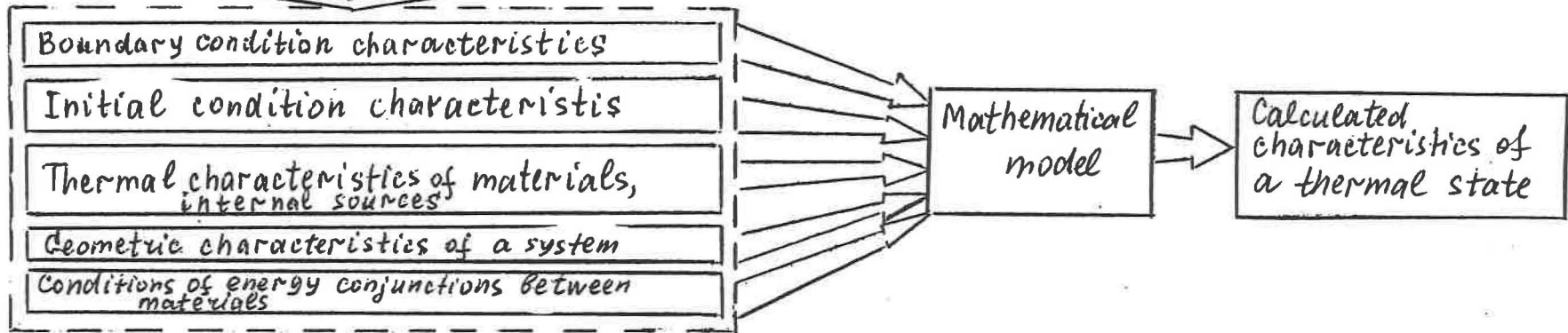
All are inverse problems!



Fundamentally different

Direct Problems in Mathematical Modeling

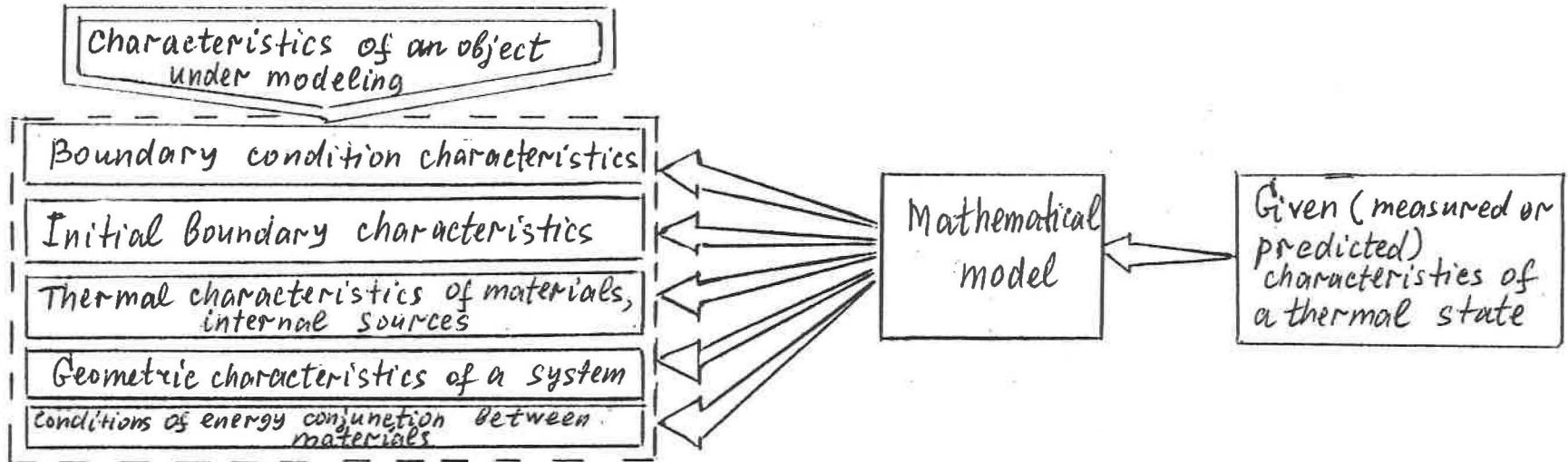
Characteristics of an object
under modeling



Cause-effect relations: direct problems

Direct problems are analysis problems

Inverse Problems in Mathematical Modeling

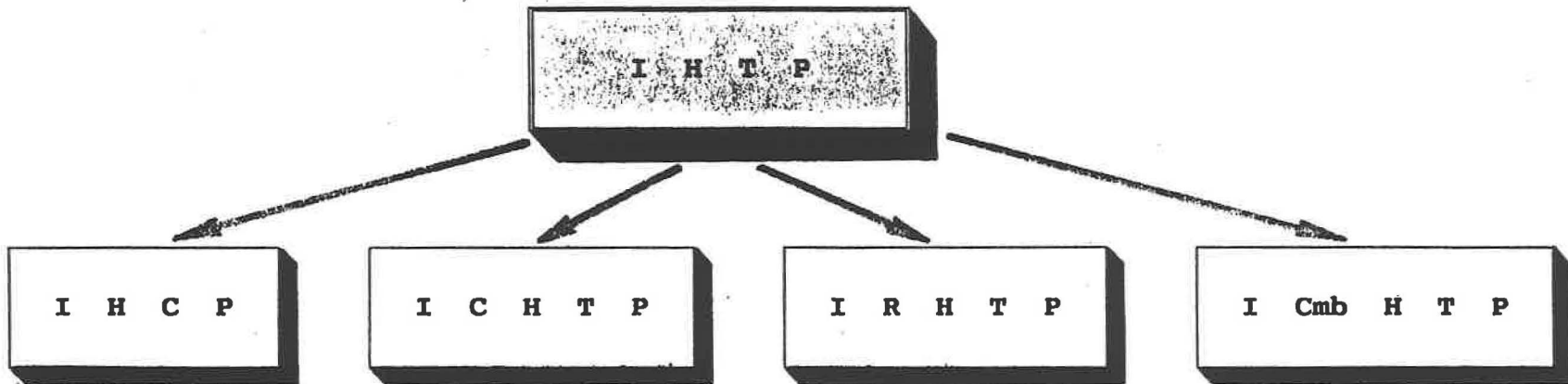


Reconstruction "causes" from "effect": inverse problems

ill-posed-ness

Inverse problems are design, diagnostics and identification problems

Another classification key - kinds of IHTP



best investigated
most widely used

I H T P

- Inverse Heat Transfer Problems

I H C P

- Inverse Heat Conduction Problems

I C H T P

- Inverse Convective Heat Transfer Problems

I R H T P

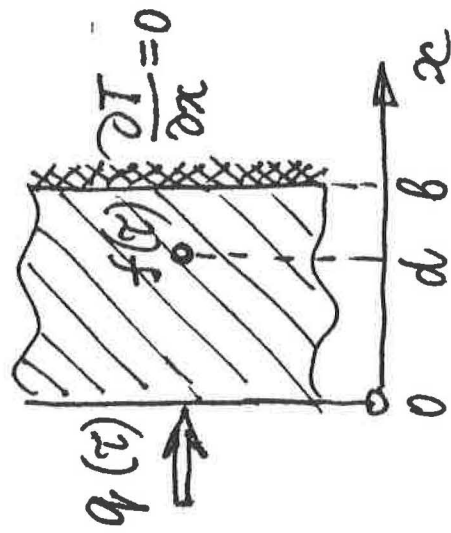
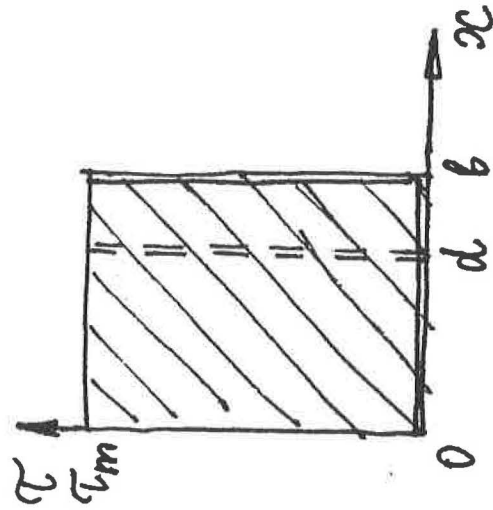
- Inverse Radiation Heat Transfer Problems

I Cmb H T P

- Inverse Combined Heat Transfer Problems

III.
**Statements of Inverse Heat Transfer
Problems**

Boundary IHCP (an example)



Heat - conduction equation :

$$C(T) \frac{\partial T}{\partial \tau} = \frac{\partial}{\partial x} \left(k(T) \frac{\partial T}{\partial x} \right), \quad 0 < x < b$$

$$0 < \tau \leq \tau_m$$

Initial temperature distribution :

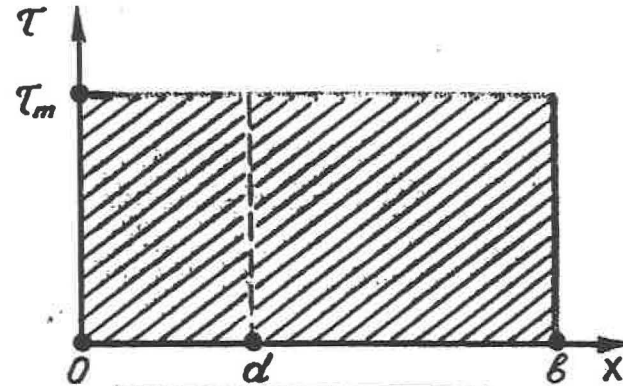
$$T(x, 0) = \varphi(x), \quad 0 \leq x \leq b$$

Internal temperature history :

$$T(d, \tau) = f(\tau), \quad 0 \leq \tau \leq \tau_m, \quad 0 < d \leq b$$

Boundary condition:

$$\frac{\partial T(b, \tau)}{\partial x} = 0, \quad 0 \leq \tau \leq \tau_m$$



Unknown functions :

$$q(\tau) = -k \left. \frac{\partial T}{\partial x} \right|_{x=0},$$

$$T_w(\tau) = T(0, \tau)$$

Heat balance equation :

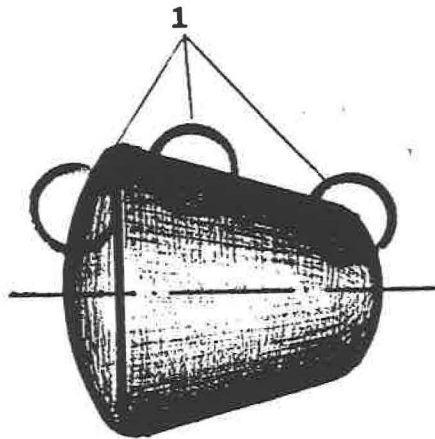
$$q_{\Sigma}(\tau) = q(\tau) + \overset{\text{emissivity}}{\varepsilon} \sigma T_w^4(\tau)$$

Heat transfer coefficient :

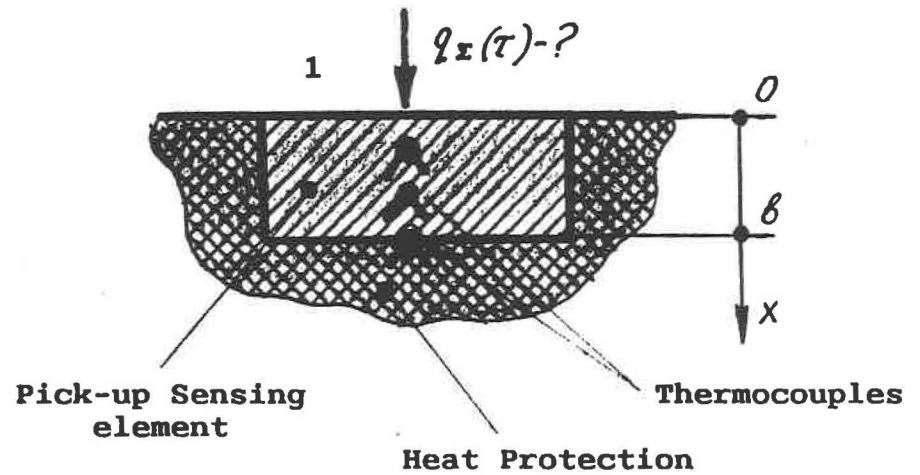
$$h(\tau) = \frac{q_{\Sigma}(\tau)}{T_{\delta}(\tau) - T_w(\tau)}$$

* Example 1:

Diagnostics of transient heat loads acting on the heat-stressed structures of flight vehicles and launching facilities

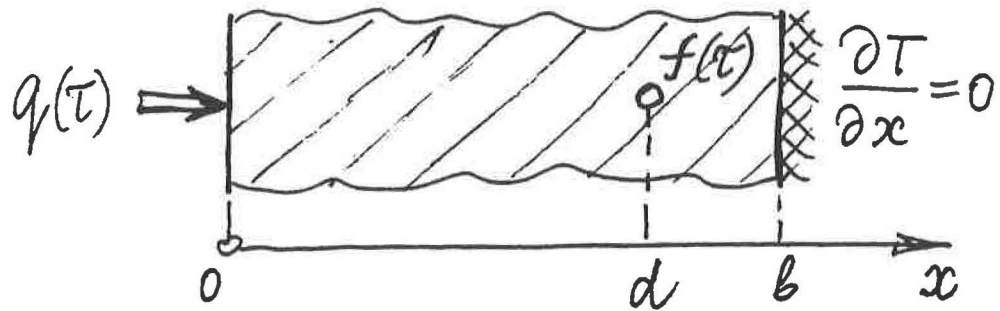


Re-entry vehicle

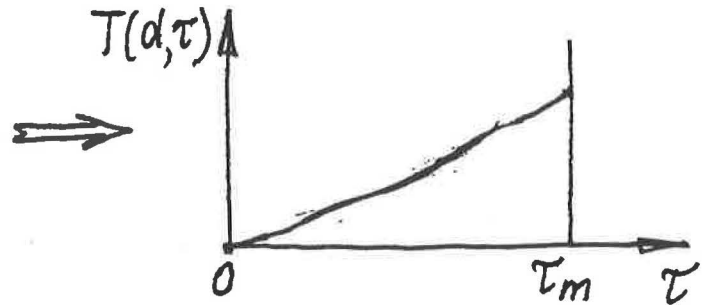
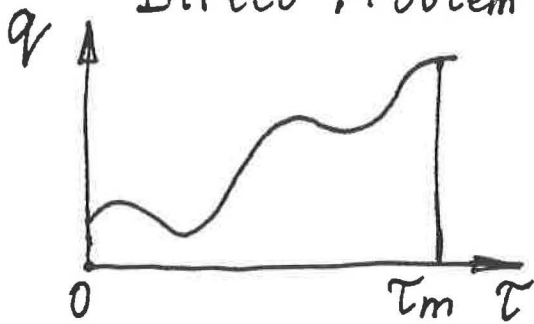


A lay - out of the sensor of unsteady heat fluxes

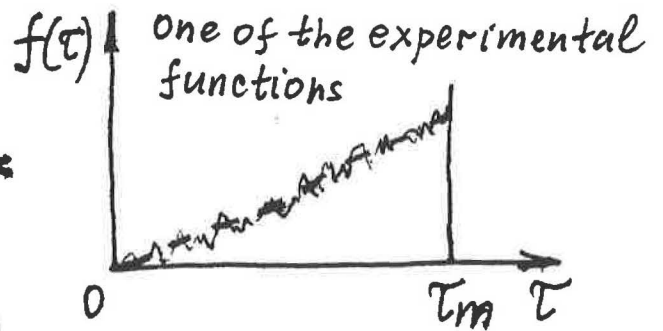
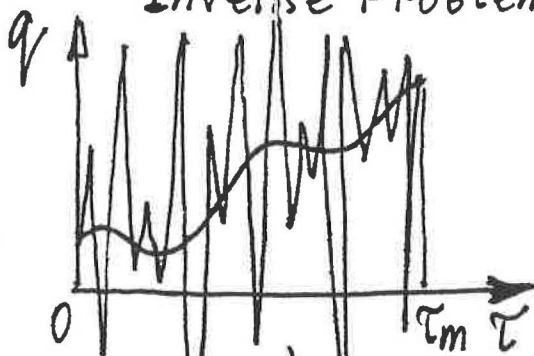
Physical explanation of ill-posedness of IHCi



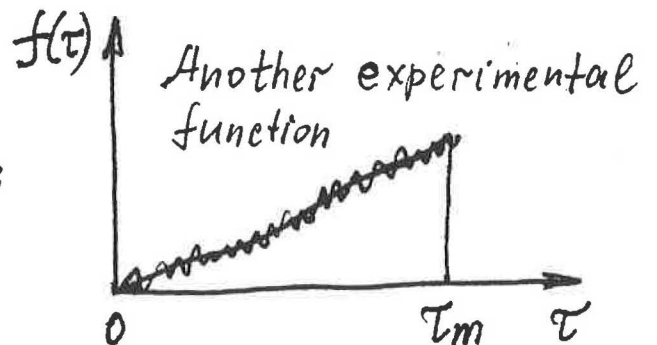
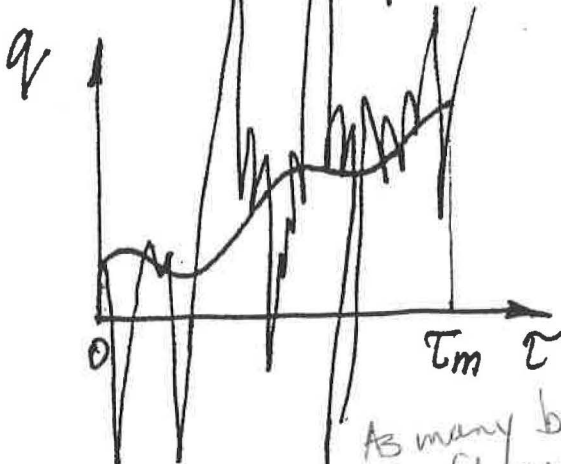
Direct Problem



Inverse Problem

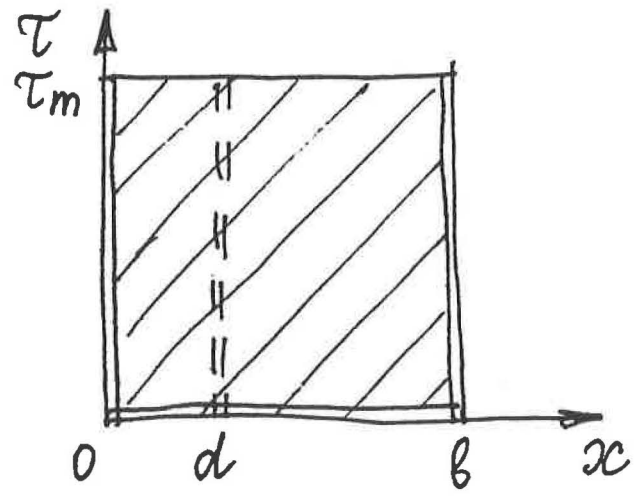
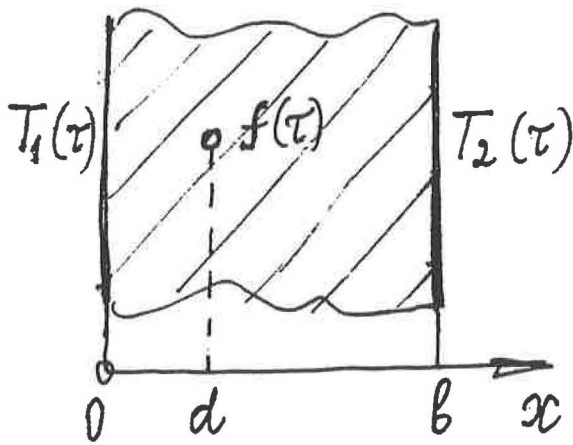


ill-posed problem



As many boundary heat fluxes as there are sensors in the body

Coefficient IHCP (a example)



$$c(\tau) \frac{\partial T}{\partial \tau} = \frac{\partial}{\partial x} \left(\lambda(\tau) \frac{\partial T}{\partial x} \right), \quad 0 < x < b, \quad 0 < \tau \leq \tau_m$$

$$T(x, 0) = \varphi(x), \quad 0 \leq x \leq b$$

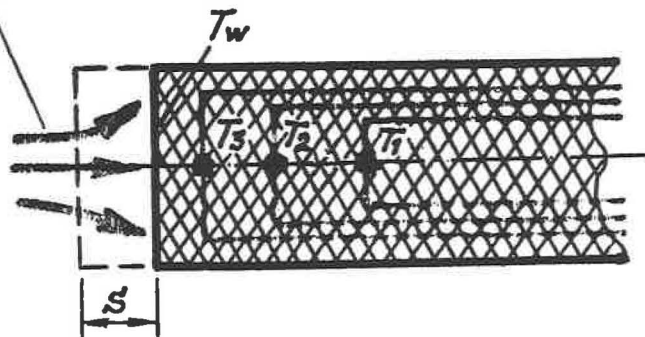
$$\left. \begin{aligned} T(0, \tau) &= T_1(\tau) \\ T(b, \tau) &= T_2(\tau) \\ T(d, \tau) &= f(\tau), \end{aligned} \right\} \quad 0 \leq \tau \leq \tau_m$$

$0 < d < b$

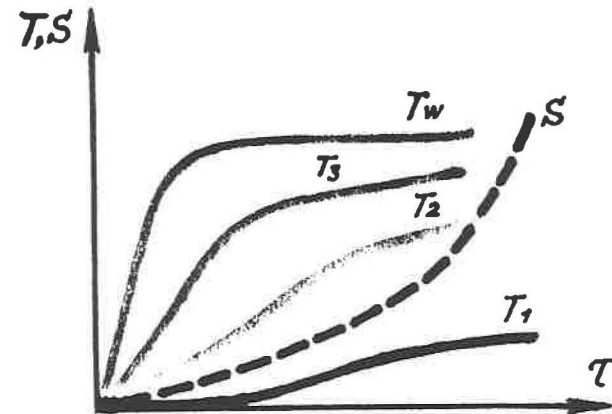
Unknown function : $\lambda = \lambda(\tau), T_{\min} \leq T \leq T_{\max}$
 can estimate as many coefficients
 as we have sensors

Example 2 : Simulation of the required conditions of specimen heating on special test facilities (plasmatrons, jets of rocket engines and others) with subsequent processing of temperature measurements by methods of inverse problems.

Hot gas flow

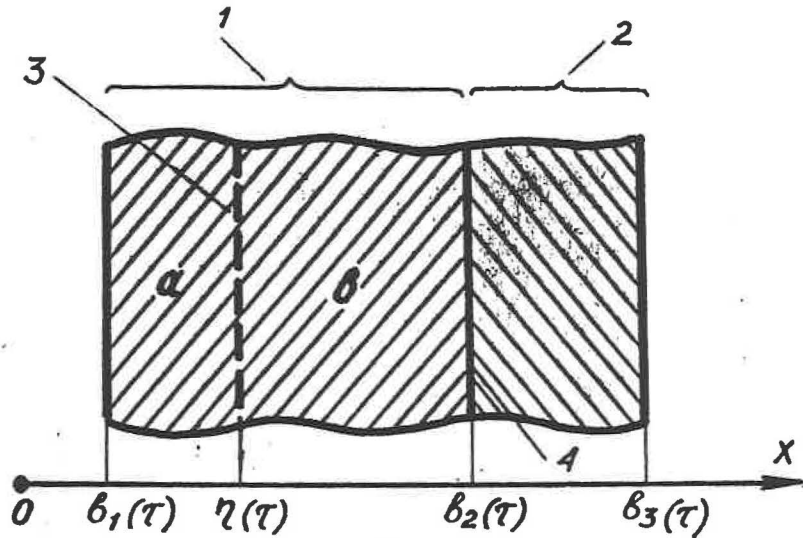


A specimen of the material with thermocouples
(S is a material ablation layer at a moment τ)



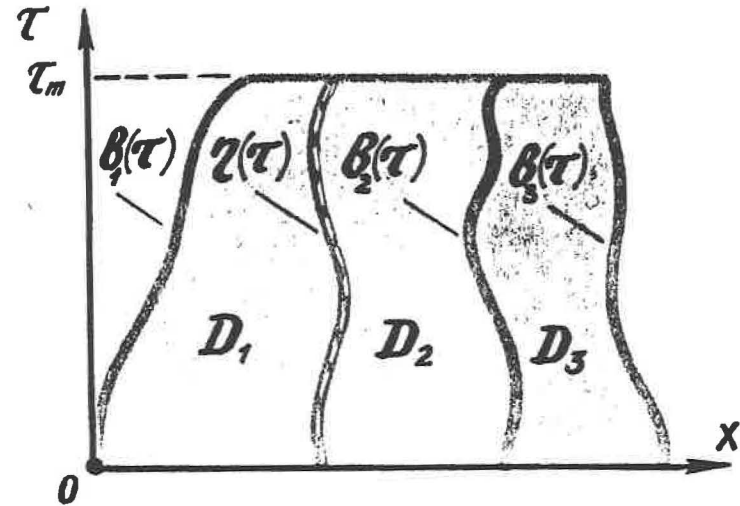
A Thermogram

One dimensional Statement



A two-layered plate with phase transition: *or ablation*

- 1, 2 - the first and the second layers;
- 3 - boundary of phase transition;
- 4 - the line of contact between layers;
- a, b - two phase states of material of the first layer



A domain with mobile boundaries

For porous materials

$$C_j \frac{\partial T_j}{\partial \tau} = \frac{\partial}{\partial x} \left(k_j \frac{\partial T_j}{\partial x} \right) + P_j \frac{\partial T_j}{\partial x} + S_j, \quad (x, \tau) \in D_j(\tau), \quad j = 1, 2, 3$$

↑ convective term
↑ distributed heat source

"generalized" heat conduction equations

Conjunction conditions

at interface surfaces

$$T_1(\eta(\tau) - 0, \tau) = T_2(\eta(\tau) + 0, \tau), \quad k_1 \frac{\partial T_1}{\partial x} \Big|_{x=\eta(\tau)-0} - k_2 \frac{\partial T_2}{\partial x} \Big|_{x=\eta(\tau)+0} = \tau \frac{\partial \eta}{\partial \tau}$$

$$T_2(b_2(\tau) - 0, \tau) = T_3(b_2(\tau) + 0, \tau) - R k_2 \frac{\partial T_2}{\partial x} \Big|_{x=b_2(\tau)-0}$$

r volumetric heat of melting

$$k_2 \frac{\partial T_2}{\partial x} \Big|_{x=b_2(\tau)-0} = k_3 \frac{\partial T_3}{\partial x} \Big|_{x=b_2(\tau)+0}$$

contact resistance between layers

Initial conditions:

$$T_j(x, 0) = \xi_j(x), \quad j = 1, 2, 3$$

$$j=1: b_1(0) \leq x \leq \eta(0); \quad j=2: \eta(0) \leq x \leq b_2(0); \quad j=3: b_2(0) \leq x \leq b_3(0)$$

Possible boundary conditions:

I. $T_j(\delta_j(\tau), \tau) = t_j(\tau), \quad j = 1, 3$

II. $-k_j \frac{\partial T_j}{\partial x} \Big|_{x=\delta_j(\tau)} = q_j(\tau), \quad j = 1, 3$

III. Newton conditions

$-k_j \frac{\partial T_j}{\partial x} \Big|_{x=\delta_j(\tau)} = h_j [T_j(\delta_j(\tau), \tau) - T_j^*(\tau)], \quad j = 1, 3$

Newton coeff. convective ambient temp absorptivity

IV. $-k_j \frac{\partial T_j}{\partial x} \Big|_{x=\delta_j(\tau)} = h_j [T_j(\delta_j(\tau), \tau) - T_j^*(\tau)] + A_j q_{rj}$

$- \epsilon_j \sigma T_j^4(\delta_j(\tau), \tau) + q_j$

convective radiating temp radiations heat source

- * Volumetric heat capacities C_j
- * Thermal conductivity k_j
- * Convection coefficients P_j
- * Sources S_j
- * Movement of boundaries B_1, B_2, B_3 and of phase transfer front η
- * Volumetric heat of phase transfer λ
- * Thermal contact resistance R
- * Initial temperatures $\xi_j(x)$
- * Boundary temperatures t_j
- * Heat fluxes q_j
- * Heat transfer coefficients h_j
- * Environmental temperatures T_j^*
- * Absorptivity A_j
- * Emissivities ϵ_j
- * Surface heat sources q_j

Additional conditions:

$$T(d_i, \tau) = f_i(\tau), \quad i = \overline{1, N}, \quad d_i \in \overline{D}_1 \cup \overline{D}_2 \cup \overline{D}_3$$

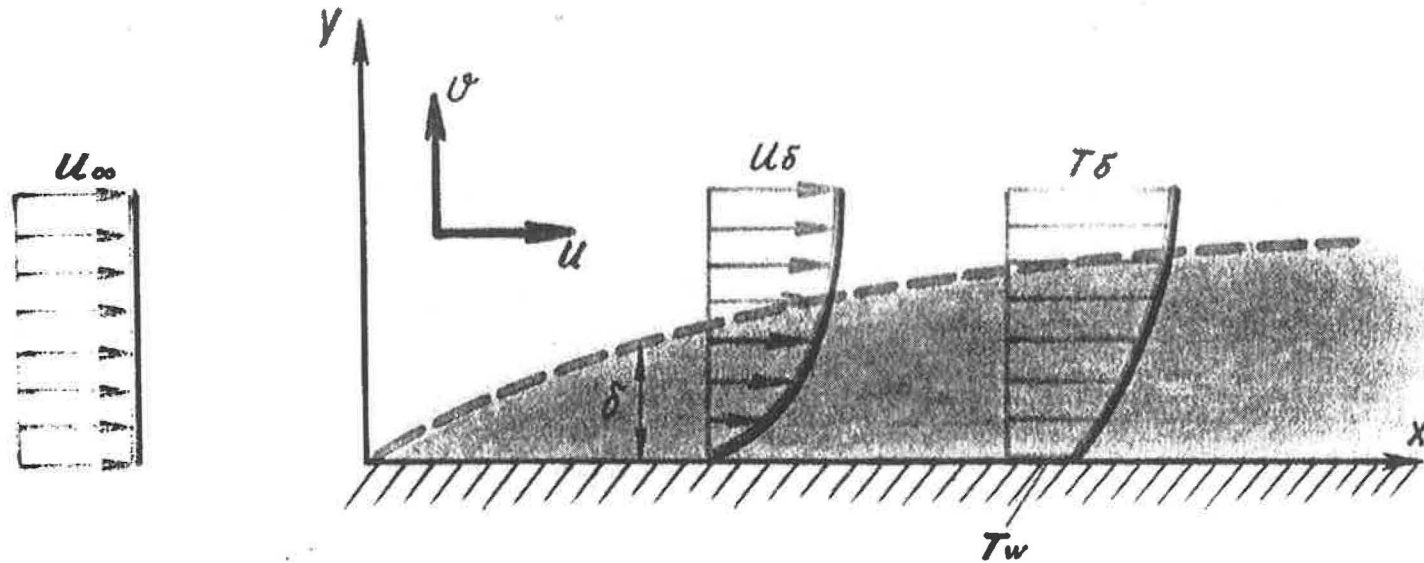
$$d_i = \text{const } i \quad \text{or} \quad d_i = d_i(\tau)$$

I H C P : $T(x, \tau)$ + some causal characteristics - ?

Kinds of I H C P:

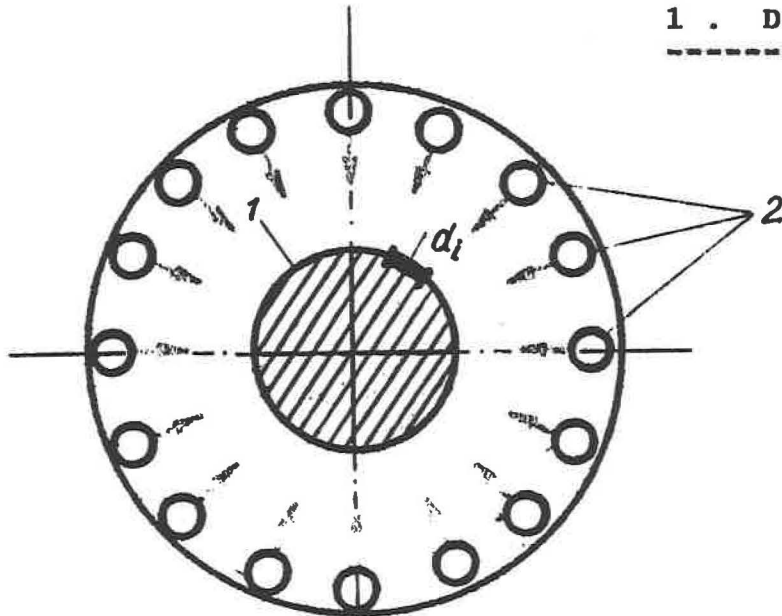
1. Retrospective Heat ^{"Reverse Time"} Conduction Problem : $\{ \xi_j(x) \}_{j=1,2,3} = ?$
2. Boundary I H C P : $\{ t_j(\tau), q_j(\tau), T_j^*(\tau), A_j(T_{w_j}, \tau), \varepsilon_j(T_{w_j}, \tau), q_j(T_{w_j}, \tau) \}_{j=1,3} = ?$
3. Coefficient I H C P :
 $\{ C_j(x, \tau, T_j(x, \tau)), k_j(x, \tau, T_j(x, \tau)), P_j(x, \tau, T_j(x, \tau)), S_j(x, \tau, T_j(x, \tau)) \}_{j=1,2,3} = ?$
4. Geometric I H C P : $\{ b_j(\tau), \eta(\tau) \}_{j=1,2,3} = ?$

one ← 5. Combined I H C P
or
more



- 1 . Reconstruction of $T(y)$
- 2 . Estimation of turbulent viscosity μ_T and thermal conductivity k_T
- 3 . Determination of catalytic activity of a solid wall

1. Discrete form



Heat balance equations :

$$\pi \sum_{j=1}^m J_j \sum_{k=1}^n \psi_{d_{i-jk}} A_{i-j} = q_i, \quad i = \overline{1, m},$$

where $\psi_{d_{i-jk}}$ is a local angular coefficient ,

A_{i-j} is an absorptivity ,

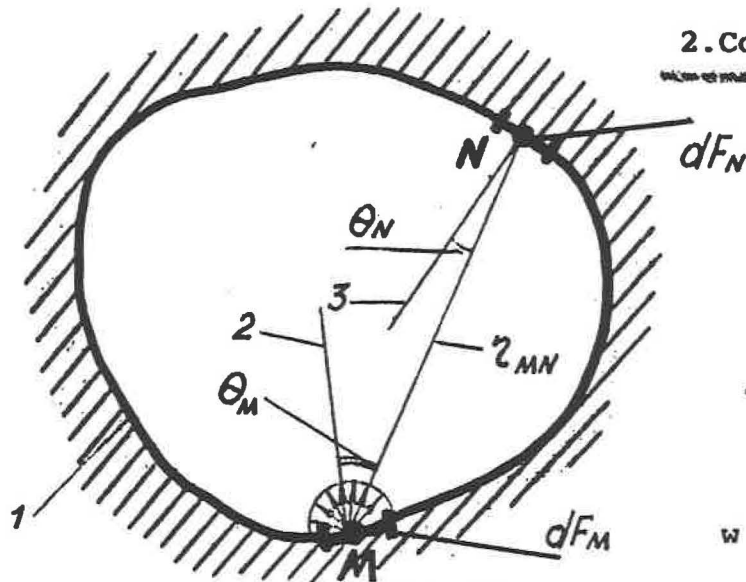
q_i is a known heat flow

An infrared simulator :

1 - test object

2 - radiative heaters

Radiation intensities of modules J_j - ?



2. Continuous form

$$\int_F E_{\text{eff}}(N) \frac{\cos \theta_M \cos \theta_N}{\pi r_{MN}^2} dF_N = E_{\text{in}}(M), \quad M \in F$$

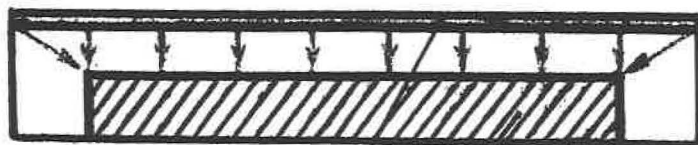
Temperature field :

$$T(N) = \left\{ \frac{1}{\sigma \epsilon} \left[E_{\text{eff}} - (1-A) E_{\text{in}} \right] \right\}^{1/4}, \quad N \in F,$$

where E_{eff} , E_{in} are half-spherical densities of effective and incident radiation respectively

A closed system of bodies :

- 1 - diffusively radiating surface F ;
- 2,3 - normals to the surface at points M and N , respectively

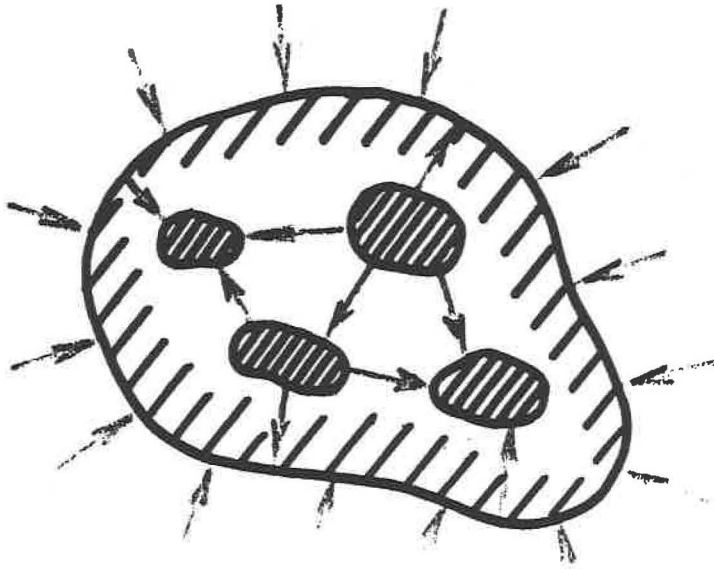


heater ($T(N) - ?$) / treated body ($T(M)$, $q_{\text{res}}(M)$ are given distributions)

Temperature distribution on body surfaces $T(M) - ?$

Stationary and linear problems

1. Inverse problem of heat transfer in engineering systems



A system of bodies
(the heat fluxes are
arbitrary shown by arrows)

*Conduction
or
convection
or both*

Heat balance equations : l, j

$$C_l \frac{dT_l}{d\tau} = \sum_{j=1}^n a_{lj} (T_j - T_l) + \sigma \sum_{j=1}^n b_{lj} (T_j^4 - T_l^4) + Q_l$$

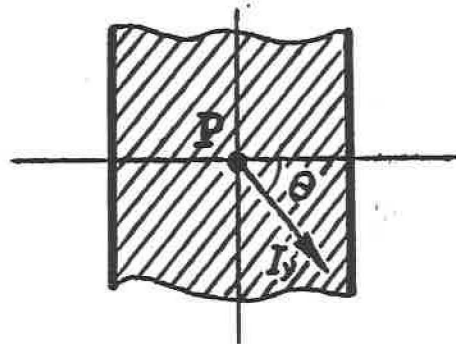
$$T_l(0) = T_0, \quad l = \overline{1, n}, \quad 0 < \tau \leq \tau_m$$

Direct measurements :

$$T_l(\tau) = f_l(\tau), \quad l = \overline{1, \kappa}, \quad \kappa \leq n$$

Causal characteristics :

- * C_l is a heat capacity of node l
- * a_{lj} is a conductive and convective heat exchange coefficient between nodes l and j
- * b_{lj} is a radiative heat exchange coefficient between nodes l and j
- * Q_l is a heat input from space to node and internal generated heat power within node l



A semi-transparent body

$$C \frac{\partial T}{\partial \tau} = \text{div}(k \text{ grad } T) - \text{div} \vec{q}_r,$$

$$q_r = \int_0^\infty \int \vec{l} I_\nu d\vec{l} d\nu, \quad \text{spectrum of radiant energy}$$

$$\vec{l} \text{ grad } I_\nu = (K_\nu + \beta_\nu) [-I_\nu(\vec{l}, P) + (1 - Sc_\nu) B_\nu(P) + \frac{Sc_\nu}{4\pi} \int_{4\pi} I_\nu(\vec{l}', P) \theta_\nu(\vec{l}, \vec{l}') d\omega -$$

- equation of radiation transport,

where:

\vec{q}_r is a radiation energy flow vector; I_ν is a radiation spectral intensity;

\vec{l} is a single direction vector of radiation propagation in point P;

K_ν, β_ν are coefficients of absorption and dispersion of radiation with the frequency ν ; $Sc_\nu = \beta_\nu / (K_\nu + \beta_\nu)$ is a Schuster number;

B_ν is a spectral radiation intensity of the absolutely black body;

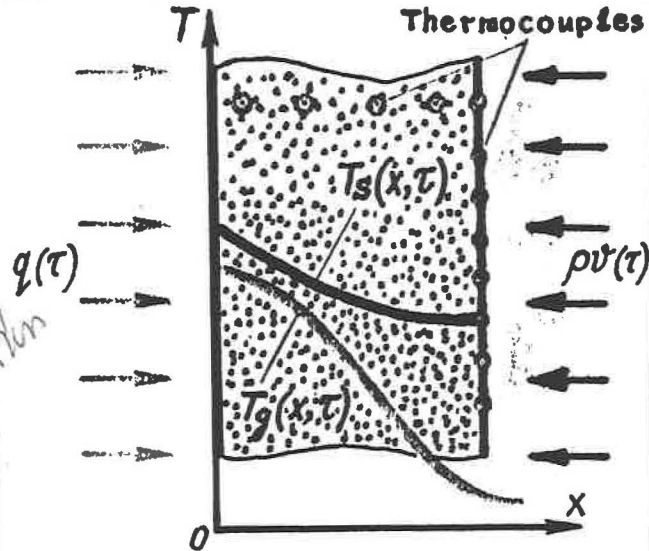
θ_ν is a indicatrice of dispersion; ω is a solid angle

Schuster number - (like Nusselt number in convection)

Input data: temperature measurements in the body

$C(T)$ and $k(T)$ are unknown coefficients

*blowing
suction*



A. porous cooling :
1 are temperature -
sensitive elements

Energy equations for solid (s) and gaseous (g) phases:

$$C_s \frac{\partial T_s}{\partial \tau} = \frac{\partial}{\partial x} \left(k_s \frac{\partial T_s}{\partial x} \right) - \frac{h_v}{1-P} (T_s - T_g), \quad \text{porosity}$$

$$(\rho C_p) \frac{\partial T_g}{\partial \tau} = \frac{\partial}{\partial x} \left(k_g \frac{\partial T_g}{\partial x} \right) - (\rho v C_p)_g \frac{\partial T_g}{\partial x} + \frac{h_v}{P} (T_s - T_g),$$

$$x \in (0, b), \quad \tau \in (0, \tau_m];$$

may be unknown

Initial conditions:

$$T_s(x, 0) = \xi_s(x), \quad T_g(x, 0) = \xi_g(x);$$

Boundary conditions:

$$-k_s \frac{\partial T_s(b, \tau)}{\partial x} = h_o [T_s(b, \tau) - T_{g0}], \quad -k_s \frac{\partial T_s(0, \tau)}{\partial x} = q(\tau);$$

$$(\rho v C_p)_g T_g(b, \tau) = (\rho v C_p)_g T_{g0} + h_o [T_s(b, \tau) - T_{g0}], \quad \frac{\partial^2 T_g(b, \tau)}{\partial x^2} = 0;$$

Darcy modified law : $-\frac{dP_g}{dx} = \alpha (\mu v)_g + \beta (\rho v)_g^2;$

Equation of state for gas : $\rho_g = \frac{P_g M_g}{8314 T_g}$

pressure

w h e r e

C_p is a specific heat capacity at constant pressure;

v is velocity; P is body porosity; p is pressure;

ρ is density; μ is viscosity; M is a molecular weight;

α, β are hydraulic coefficients;

T_{g0} is an initial temperature of the insufflated gas

Measurement data:

$$T_s(d_i, \tau) = f_i(\tau), \quad \tau \in [0, \tau_m], \quad i = \overline{1, N}, \quad N \geq 1, \quad 0 \leq d_1 < d_2 < \dots < d_N \leq B$$

Unknown causal characteristics:

- heat fluxes $q(\tau)$,
- thermal conductivity $k_s(T_s)$,
- inner heat transfer coefficients h_v of the porous body,
- heat transfer coefficients h_0 at a coolant inlet into a porous body

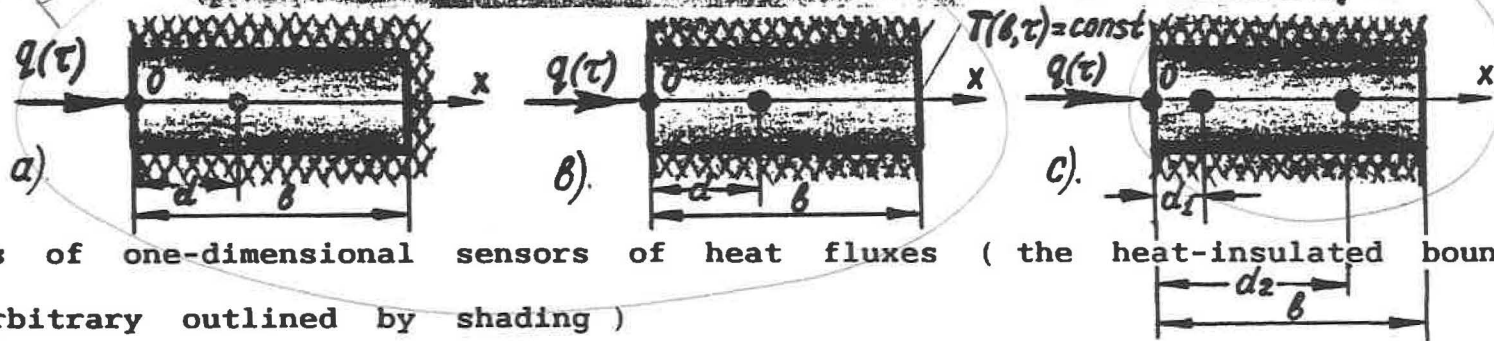
IV.
**Practical Applications of Inverse Heat
Transfer Methods**

* NON-STATIONARY HEAT DIAGNOSTICS

General principles of onedimensional heat measuring

one measurement point

two measurement points



Schemes of one-dimensional sensors of heat fluxes (the heat-insulated boundaries are arbitrary outlined by shading)

The determination of functions and parameters included in the boundary conditions (h, R, A, ϵ) can usually be reduced to a boundary inverse problem.

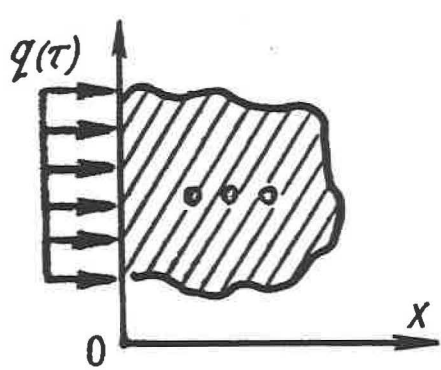
Example: heat transfer coefficient $h(\tau)$ - ?

$$h(\tau) = q_w(\tau) / [T^*(\tau) - T_w(\tau)],$$

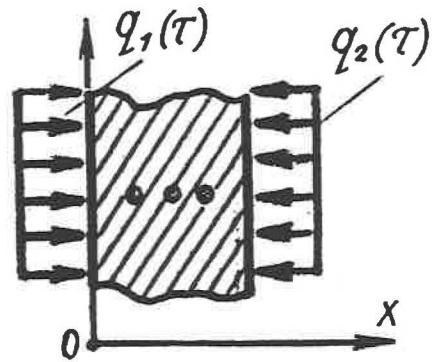
where T^* -- characteristic (recovery) temperature of gas (liquid);

T_w -- body surface temperature;

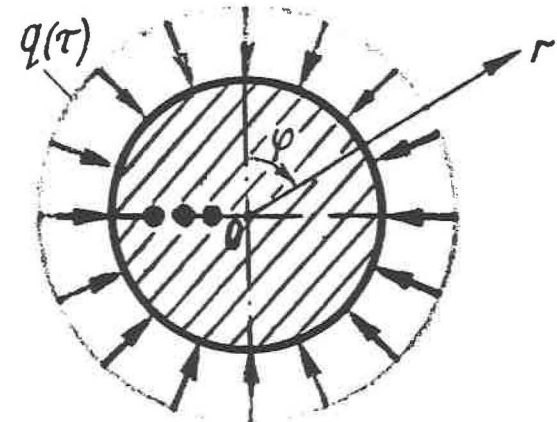
$$q_w(\tau) = q(\tau) + \epsilon \sigma T_w^4(\tau) \quad (q(\tau) \text{ and } T_w(\tau) \text{ are from I H C P })$$



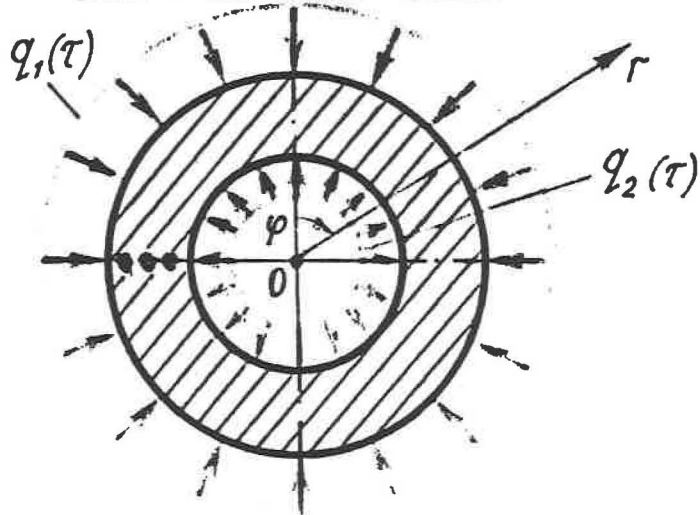
Semi - infinite Solid



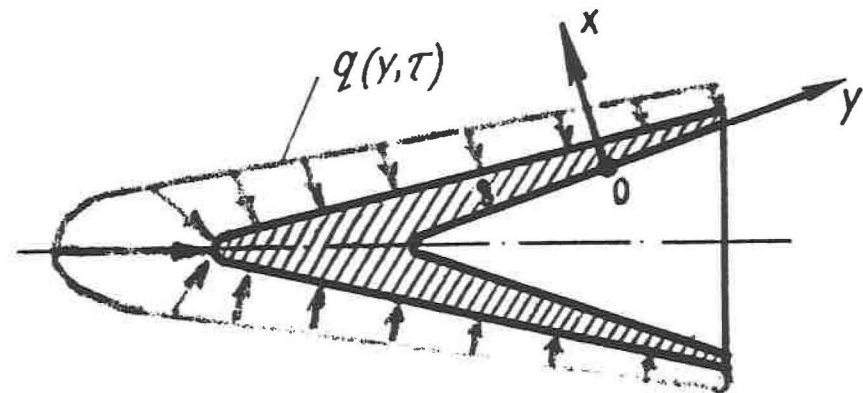
Slab



Solid cylinders and spheres

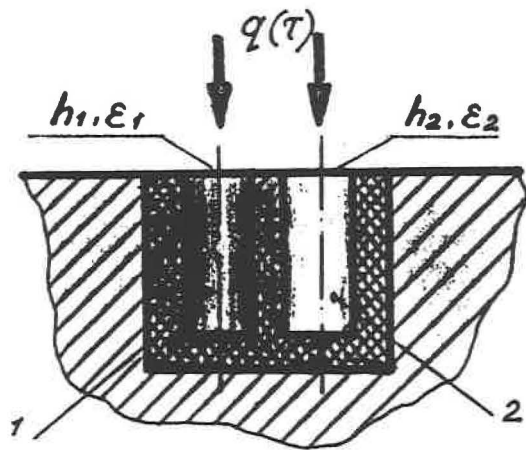


Hollow cylinders and spheres



Specimen with wall of variable thickness

ooo - points of temperature measurements



The scheme of a sensor with two sensitive elements 1 and 2

Unknown values:

- a local coefficient of heat transfer $h(T_w/T^*)$
- an integral coefficient of the surface radiation (emissivity) $\epsilon(T_w)$

if $h_1(\tau) = h_2(\tau) = h(\tau), \tau \in [0, \tau_m],$

and common coating
 $\epsilon_1(\tau) = \epsilon_2(\tau) = \epsilon(\tau), \tau \in [0, \tau_m],$

a heat balance equations are

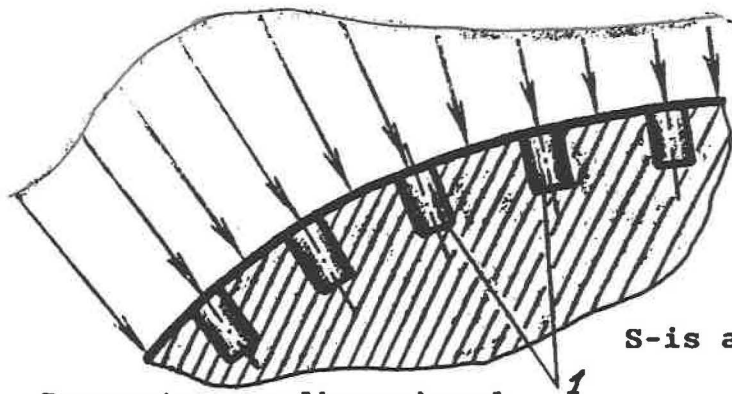
$$(i) \quad \begin{cases} h(T^* - T_{w1}) = \epsilon \sigma T_{w1}^4 + q_1, \\ h(T^* - T_{w2}) = \epsilon \sigma T_{w2}^4 + q_2, \quad \tau \in [0, \tau_m] \end{cases}$$

$T_{w1}(\tau), T_{w2}(\tau), q_1(\tau), q_2(\tau)$ are obtained the solution of IHCP

Afterwards $h(\tau), \epsilon(\tau)$ are obtained from (i) for each moment τ

$$\{h(\tau), \epsilon(\tau)\} \Rightarrow \{h(T_w/T^*), \epsilon(T_w)\}$$

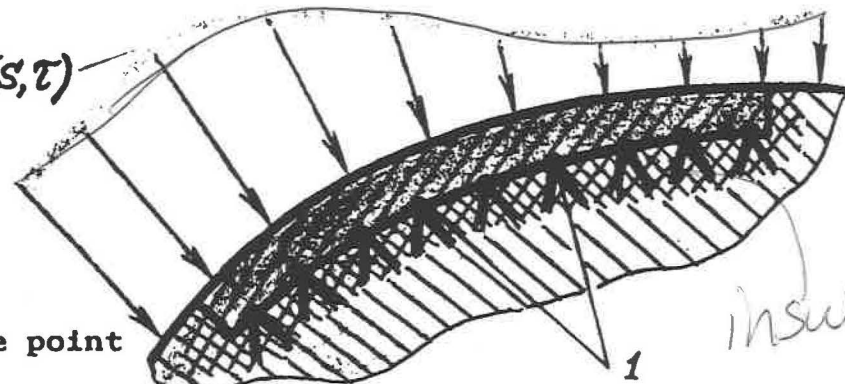
Add a third sensor, can introduce T^* as add unknown.



Discrete one-dimensional sensors (1) for reconstruction of the spatial-time distribution of heat fluxes

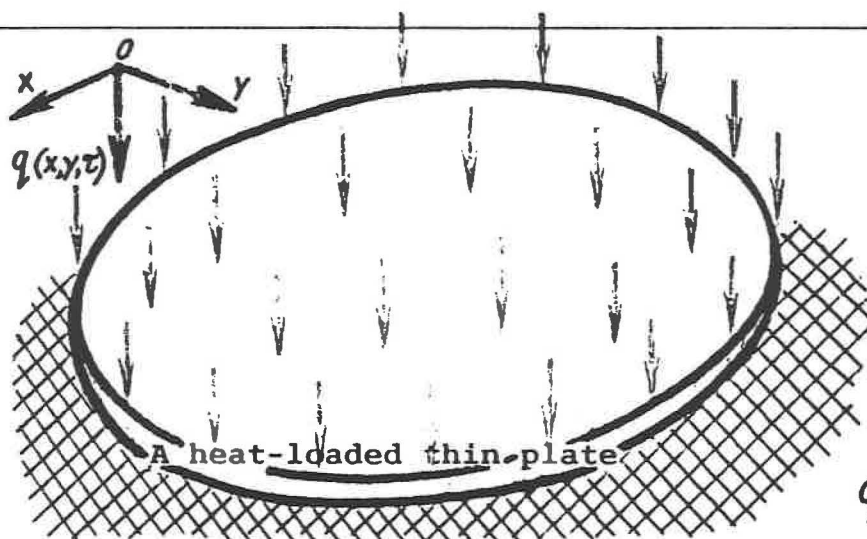
$q(s, \tau)$

S-is a surface point



A two-dimensional sensor of heat fluxes:
1 - thermocouples

insulated



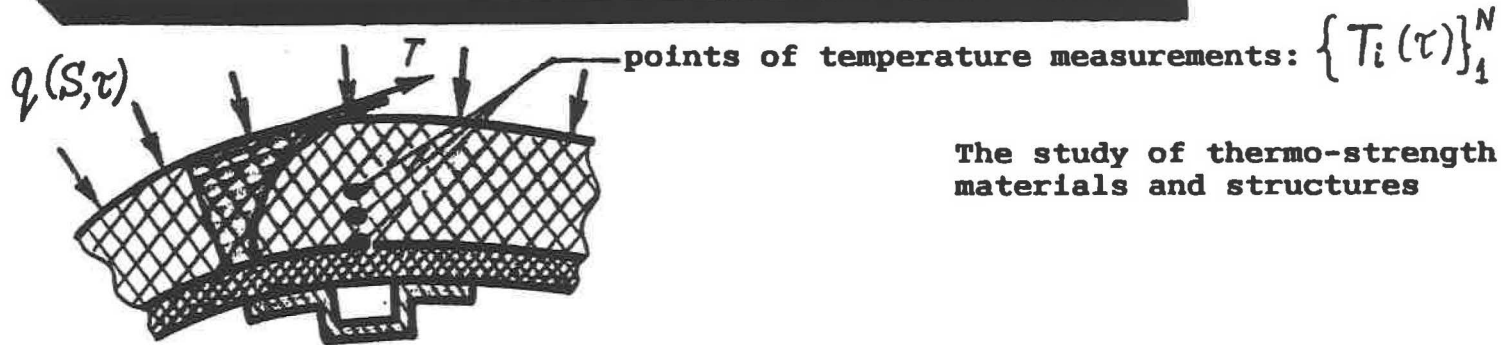
A heat-loaded thin-plate

$$c \frac{\partial T}{\partial \tau} = \frac{\partial}{\partial x} \left(k \frac{\partial T}{\partial x} \right) + \frac{\partial}{\partial y} \left(k \frac{\partial T}{\partial y} \right) + \frac{q(x, y, \tau)}{b}$$

a source

Where b is a thickness of plate,
 $T(x, y, \tau)$ is the measured temperature field,
 $q(x, y, \tau)$ is an unknown value

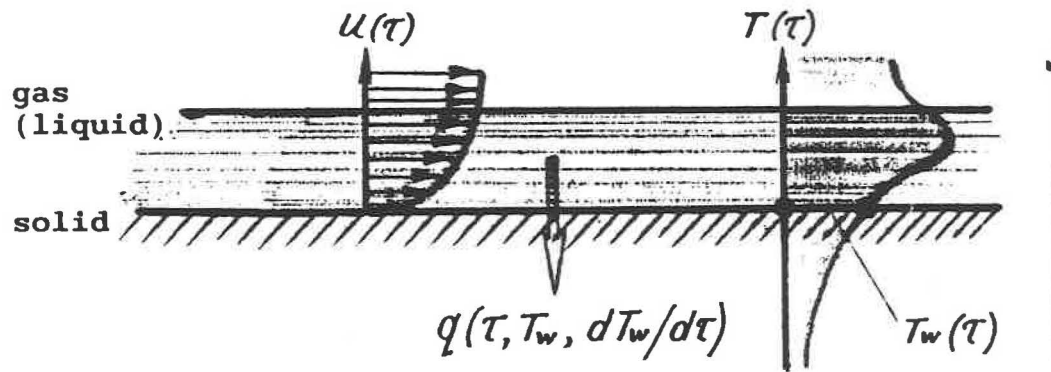
THE RECONSTRUCTION OF TEMPERATURE FIELDS AND HEAT FLOWS



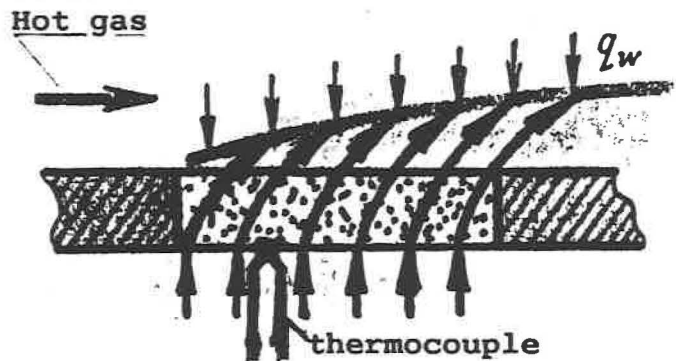
The study of thermo-strength of materials and structures

Example of a structure

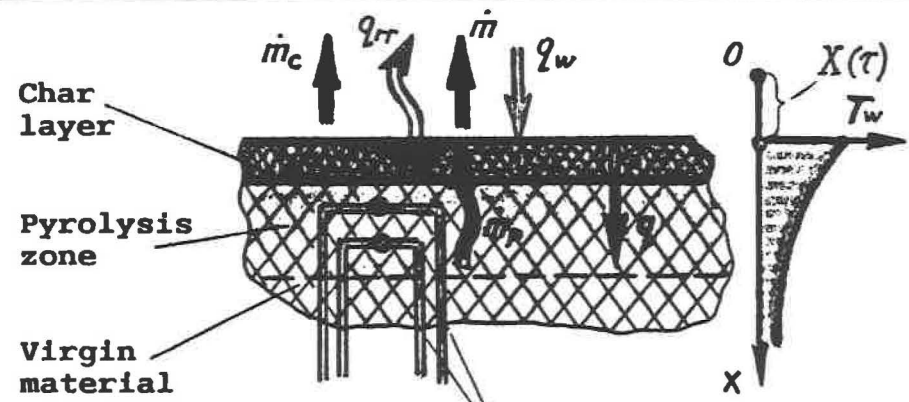
THE STUDY OF NON-STATIONARY HEAT TRANSFER



joint problem of heat-and mass transfer



Porous cooling



thermocouples

Heat protection (char-forming) material

$$q_w^0 = q_{rr} + q + q_{ph.ch} + q_{bl}$$

where q_w is a rate of heat transfer to surface by convection and radiation (0 - with no account for injection),

$q_{rr} = \epsilon \sigma T_w^4$ are radiative heat losses on the surface,

q is a net heat flux in solid at surface,

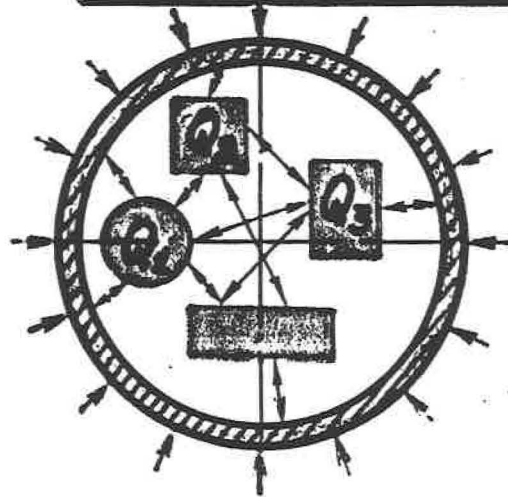
$q_{ph.ch}$ is a heat release or absorption due to physio-chemical processes,

q_{bl} is a reduction of the surface heat transfer due to blowing,

\dot{m}_c is a surface rate of ablation;

\dot{m}_p is a rate of depolymerization of the virgin material

IDENTIFICATION OF HEAT TRANSFER PROCESSES IN ENGINEERING DEVICES



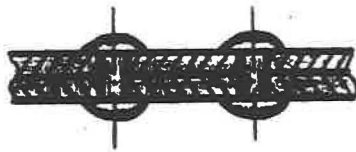
Identification and correction of mathematical models of engineering systems:

- * integral factors of absorption A and hemispherical emittance ϵ of the outer surface;
- * coefficients for conduction and / or convection between the selected elements of the module; and so on

DETERMINATION OF THERMAL PROPERTIES OF MATERIALS

- * determination of thermophysical properties and kinetic characteristics of heat-shield materials;
 - * determination of temperature dependence of heat conduction coefficient of a cooling ingot during steel tempering;
 - * determination of properties of freezing-and-melting soils;
- and so on

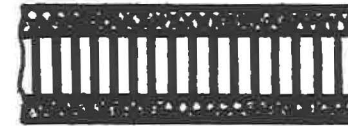
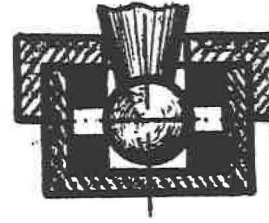
* CONTACT HEAT TRANSFER STUDIES



Rivetted and bolted joints



Hinged joints



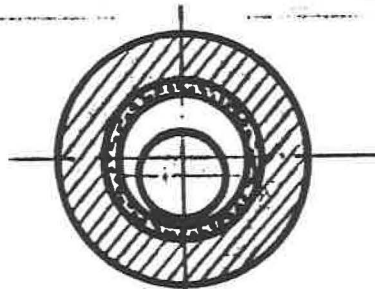
Multi-layer thermal shields

aghesive joints

* EVALUATION AND MONITORING OF THE OPTIC RADIATION CHARACTERISTICS

Optic radiation properties of the spacecraft outer surface, radiators, solar batteries ets.

* DETERMINATION OF HEAD LOADINGS DURING FRICTION

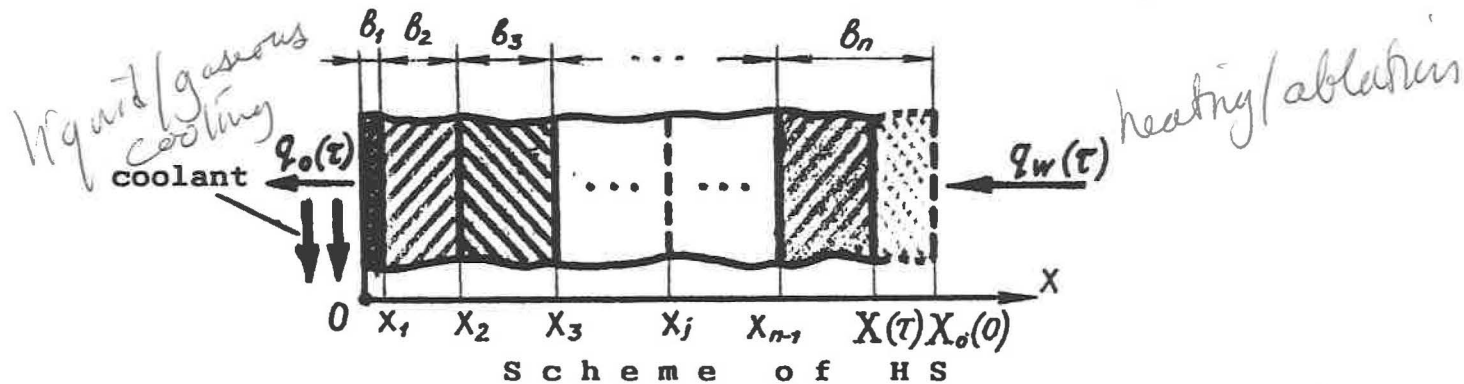


Bearing

- * heat release during friction of two solid surfaces;
- * heat transfer influence in the friction zone on friction mechanism;
- * friction moment

*on end
sp of
short course*

One-dimensional thermal mathematical model for n-layers H S



$$C_j(T) \frac{\partial T_j}{\partial \tau} = \frac{\partial}{\partial x} \left(k_j(T) \frac{\partial T}{\partial x} \right), \quad (x, \tau) \in D_j,$$

$$D_j = \{ (x, \tau) : x_{j-1} < x < x_j ; x_0 = 0 ; 0 < \tau \leq \tau_m \}, \quad j = \overline{1, n-1};$$

Generalized heat conduction equation

$$C_n(T, \gamma) \frac{\partial T}{\partial \tau} = \frac{\partial}{\partial x} \left(k_n(T, \gamma) \frac{\partial T}{\partial x} \right) + P(T, \gamma) \frac{\partial T}{\partial x} + S(T, \gamma), \quad (x, \tau) \in D_n,$$

$$D_n = \{ (x, \tau) : x_{n-1} < x < X(\tau) ; 0 < \tau \leq \tau_m \},$$

where

γ

is a parameter taking into account dynamic character

of changes in the properties of material during heating

and destructing (for example, $\gamma = \frac{\partial T}{\partial \tau}$);

$X(\tau)$ is a moving boundary of a shield

*known*Initial conditions : $T_j(x, 0) = \xi_j(x), \quad j = \overline{1, n};$

Boundary conditions :

$$k_1 \frac{\partial T_1}{\partial x} \Big|_{x=0} + q_0(\tau) = 0,$$

$$k_n \frac{\partial T_n}{\partial x} \Big|_{x=X(\tau)} + q_n(\tau) = 0,$$

$$q_0(\tau) = h [T_1(0, \tau) - T_{\text{coolant}}],$$

$$q_n(\tau) = q_w(T_w(\tau), \tau) - \epsilon \sigma T_w^4(\tau) - q_{\text{ph.ch}}(T_w(\tau), \tau),$$

where h is a heat transfer coefficient; $T_w(\tau) = T_n(X(\tau), \tau);$

$q_{\text{ph.ch}}$ is a heat release or absorption due to physico-chemical processes on surface

Conjunction conditions :

$$T_j(x_j - 0, \tau) = T_{j+1}(x_j + 0, \tau) - R_j k_j \frac{\partial T_j}{\partial x} \Big|_{x=x_j - 0}, \quad j = \overline{1, n-1}$$

$$k_j \frac{\partial T_j}{\partial x} \Big|_{x=x_j - 0} - k_{j+1} \frac{\partial T_{j+1}}{\partial x} \Big|_{x=x_j + 0} = 0, \quad j = \overline{1, n-1}$$

possible temp jump across layers (due to resistance)

*left end**right end*

Unknown solution :

{ number of layers; types of materials; thicknesses of layers b_2, \dots, b_n }

Criterion :

Specific mass of HS at given point ζ of a surface

$$m_\zeta = \sum_{j=2}^n \rho_j b_j^\zeta$$

where ρ_j is a material density of layer j ;

b_j^ζ is thickness of a layer j at a point ζ

Restrictions :

• on admissible temperatures of layers $T_j(x, \tau) \leq T_j^{max}$;

• on ranges of change of unknown parameters;

• on coolant heat capacity $\int_0^{\tau_m} q_0 d\tau \leq Q^{max}$

This problem is a combined coefficient - geometric inverse problem

TWO SUBPROBLEMS:

1. Determination of the thicknesses vector $\vec{b}_2 = \{b_j^2\}_{j=2}^n$ of layers for given materials and number of layers (geometric inverse problem)

$$\vec{b}_2 : \min_{\vec{b}_2 \in G} m_2(\vec{b}_2),$$

$$G = \{ \vec{b} : q_i(\vec{b}, T(x, \tau, \vec{b})) \leq 0; i = \overline{1, \ell} \},$$

$$T(x, \tau, \vec{b}) = A[T(x, \tau, \vec{b}), \vec{b}]; \vec{b} \in R^{n-1}$$

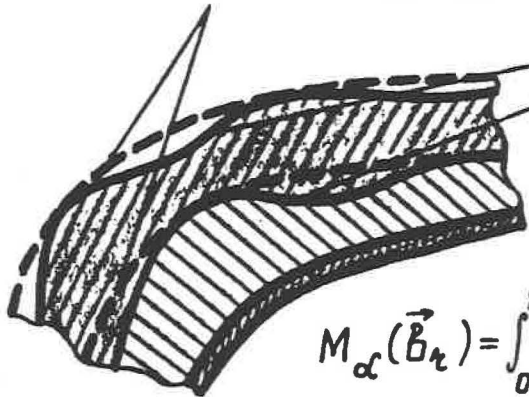
This subproblem may be solved by penalty functions method in combination with gradient methods

2. Determination of suitable materials and number of layers (this subproblem may be solved by the trial-and-error method)

take
to 1.2

Smoothed curves

Values of thicknesses, obtained by solving above-stated problem



previous objective function

Modified criterion:

smoothing term (regularizer)

$$M_{\alpha}(\vec{B}_n) = \int_0^S \left[\sum_{j=2}^n \rho_j b_j(s) \right] ds + \sum_{j=2}^n \alpha_j \int_0^S \left[x_j^{(\gamma_j)}(s) \right]^2 ds, \quad \alpha_j > 0, j = \overline{2, n}$$

where S is a contour length of support (i.e., at $x = 0$) surface;

γ_j is a degree of derivative chosen for j -th layer

Simplification:

$$\alpha_2 = \alpha_3 = \dots = \alpha_n = \alpha; \quad \gamma_2 = \gamma_3 = \dots = \gamma_n = 1 \text{ or } 2$$

Choice of parameter α :

$$\alpha_{opt} : |M(\alpha) - M_{min}| - \Delta M_{\alpha} \rightarrow \min_{\alpha}$$

trial error?

where $M(\alpha) = \int_0^S \left[\sum_{j=2}^n \rho_i b_j^{\alpha}(s) \right] ds;$

ΔM_{α} - maximum admissible deviation of linear mass of H S from the linear mass, corresponding to initial criterion m_n

V.
General Operator Form of an Inverse
Problem and a Little on the History
of the
Subject Matter

General formulation of an inverse problem in the form of operation equation is

$$Au = f, \quad u \in U, \quad f \in F, \quad (i)$$

where u and f are unknown and observed elements respectively (vectors, function or vector - functions),

U, F are metric spaces,

A - is a continuous operator.

The Hadamard conditions of well - posedness (1902) :

- * Solution of problem (i) exists for any $f \in F$;
 - * it is unique in U ;
 - * it depends continuously on f .
- existence
uniqueness
Stability*

If at least one of the requirements is violated, the (i) problem is called ill - posed. This is the very situation, which is observed in solving the IHTP.

P r o b l e m	R e s e a r c h e r s	T i m e
<p>* Historical climate and heat conduction of Earth's ground layer</p>	<p>Fourier , Poisson , Kelvin</p>	<p>19th century</p>
<p>* Detemination of unsteady heat fluxes</p>	<p><u>Mirsepassi T.J.</u> Stolz G Beck J.V. Aldoshin G.T. Golosov A.S. Zhuk V.I. Alifanov O.M.</p>	<p>1958 1960 1962 and later 1968 and later 1969 and later</p>

First name in USA in inverse methods (by Oleg's account)

Boussinesq 1901

* Application of the principle of regular regime for heat fluxes recovery

Shumakov N.V.

1955 and later

* Pseudo - inverse heat conduction problem

Giedt W.H.

1955

Kastelin O.N.

Bronsky L.N.

1956

* Heat conduction problem in the Cauchy generalized formulation

Stefan J.

1890

Tyomkin A.G.

1961

Burggraf O.R.

1964

first exact solution to 1-D IHP w/ constant coefficients

M e t h o d
(S t a t e m e n t)

R e s e a r c h e r s

T i m e

* Conditionally -
well - posed problems

Hadamard - 1902
Carleman T.

first attempt to solve inverse problem

1926

Tikhonov A.N.

Formulated "Conditionally well-posed" problem

1943

Lavrentiev M.M.

1953 and later

Ivanov V.K.

1956 and later

John F.

Solves heat conduction by equation of inverse time

1955 and later

* Integral equations of
the first kind

Phillips D.L.

1962

Twomey S.

1963 and later

* Regularization
method (variational
principle)

Tikhonov A.N.

Felix, 1962 also

1963 and later

Lavrentiev M.M., Ivanov V.K.,

Arsenin V.Ya., Morozov V.A.,

Bakushinsky A.B., Glasko V.B.

* Iterative regularization

Alifanov O.M.

1974 and later

Rumyantsev S.V.

mathematically grounded

universal - most effective method

monograph - ? Lions? Lyons

- for solving inverse
heat conduction problems

Tikhonov A.N.,
Glasko V.B.
Alifanov O.M.
Artyukhin E.A.

1967
1971 and later

* Iterative regularization
method

Alifanov O.M.
Artyukhin E.A.
Rumyantsev S.V.
Mikhailov V.V.
Yudin V.M.

1974 and later

* Quasi - inversion
method

Latt'es R., }
Lions J. - L. }

1967

* Artificial hyperbolization
method

Alifanov O.M.

1971

TP
1

H e u r i s t i c r e g u l a r i z a t i o n

1 / 22

A p p r o a c h	R e s e a r c h e r s	T i m e
* Direct methods	Shumakov N.V., Stolz G. Beck J.V.	1955 and later 1960 1962 and later
* Trial - and - error method	<u>Kozdoba L.A.</u>	1968 and later
* Linear dynamic filtration	Symbirsky D.F. <u>Matsevitly Yu. M.,</u> <u>Myltanovsky A.V.</u>	1976 and later 1977 and later

VI.
**Principles of Solution for Ill-posed
Problems**

Principles of Solution for Ill-posed Problems

1. Conditionally well-posed statements
2. Approximation of the inverse operator A^{-1} by a family of continuous operators

$$Au = f$$

1. A conditionally well-posed problem statement:
 - 1) a solution $u \in M \subseteq \text{DA}$ - the domain of the operator definition
 - 2) a solution is unique
 - 3) a solution is stable for $\tilde{f} = f + \Delta f \in M$

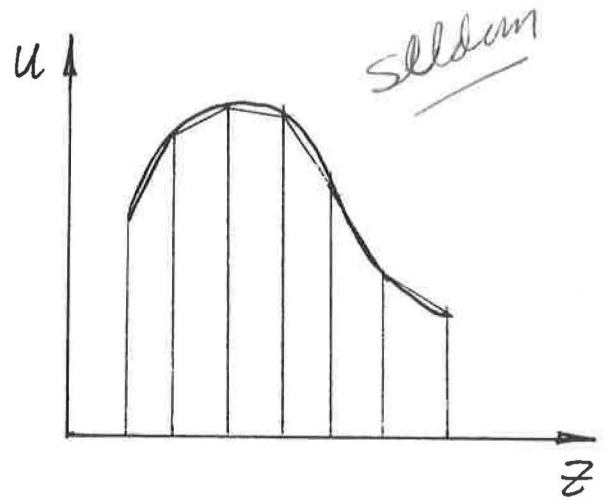
A class of well-posedness (acceptable solutions)

-
2. - self-regularization \rightarrow by adjusting parameters in the solution (direct methods)
 - Tikhonov's regularization

Sources of the self (natural)-regularization:

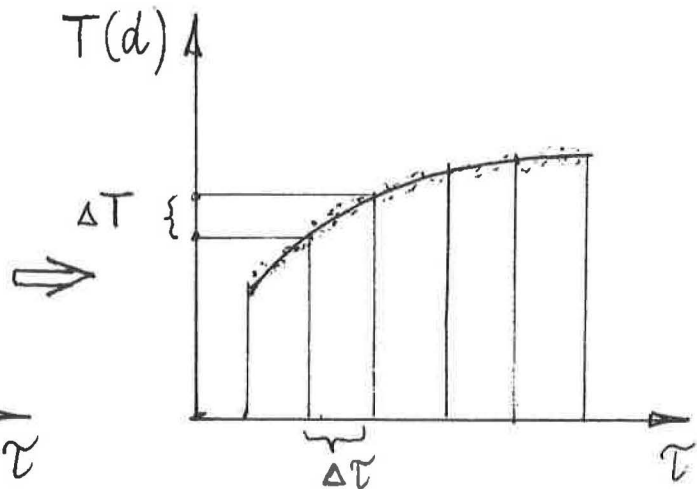
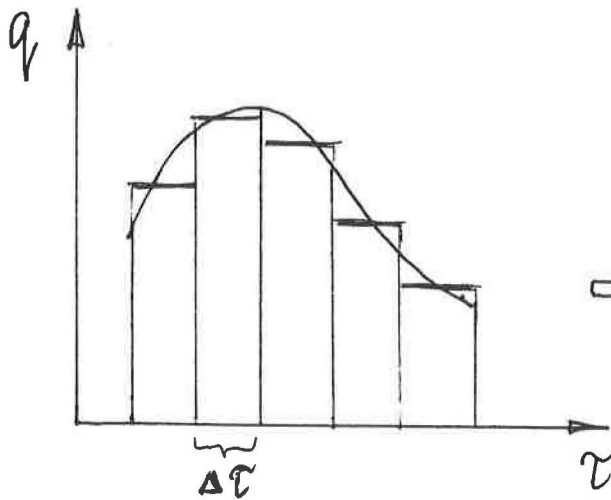
- 1) a regularization effect of heating
- 2) "viscous" properties of computational algorithms \rightarrow natural filtration of high frequency components of solution

Step Regularization



Approximations

$$\Delta z_n = z_n - z_{n-1}, \quad n = 1, 2, \dots, N$$



$\Delta \tau$ must be chosen so that ΔT resulting will be significant relative to noise in the data

Viscous Properties of Algorithms

- a choice of approximation steps
- a choice of the degree of a polynomial, etc.

Want to compare error with expected error in data, etc.
residual

VII.
Regularization of Unstable Problems
by Tikhonov Method

Tikhonov Regularization Method

$$Au = f, \quad u \in U, \quad f \in F$$

metric spaces

A^{-1} is the inverse operator

If A^{-1} is bounded: $u = A^{-1}f$

But A^{-1} is not obligatory continuous (!)

Regularizing operator R_α : α is a scalar

Domain of operator

1. $D_{R_\alpha} = F, \alpha > 0$; 2. R_α is continuous in F ;
3. $R_\alpha Au \xrightarrow{\alpha \rightarrow 0} u$ $\alpha =$ "regularizing parameter"

$\{A_h, f_\delta\}$ - are some approximations $\{A, f\}$

metric in space F

(distance between members in space F)

$$\rho_F(f_\delta, f) \leq \delta$$

unknown

$$\rho_U(A_h, A) \equiv \sup_{u \in U} \rho(A_h u, Au) \leq h (> 0)$$

$G = \{\delta, h\}$ is the error of input data

$\delta > 0$

$h > 0$

$u_\alpha(\sigma) =$ an approximate solution

Regularizing operator:

1. $\exists \delta_0 > 0, h_0 > 0$: R_α is specified for $\alpha > 0$ and A_h, f_δ :

$$P_F(f_\delta, f) \leq \delta \leq \delta_0, \quad d_{ij}(A_h, A) \leq h \leq h_0$$

2. $\exists \alpha = \alpha(\epsilon)$: $\lim_{\epsilon \rightarrow 0} u_{\alpha(\epsilon)} = \bar{u}$

Regularizing algorithm = Regularizing operator

Choice of α uses same information about the problem being solved.

+ Method for α selection

Variational method proposed by Tikhonov widely used in Russia

Smoothing functional

$$P_\alpha[u, A, f] = P_F^2(Au, f) + \alpha \Omega[u], \quad u \in D(\Omega)$$

where

P_F is the residual in the space F ; function Ω .

$D(\Omega)$ is the domain of $\Omega[u]$;

$\Omega[u]$ is stabilizing functional:

$$M_c = \{ u : \Omega[u] \leq c \}, \quad c \geq 0 = \\ = \text{compact in } U$$

Example: $\Omega = P_V(u, u^*),$

$$P_V(u_1, u_2) \leq P_V(u_1, u_2)$$

compact with any sequence contains a subsequence.

A is continuous, single-valued and additive;
 $\Omega[u]$ is rigorously convex;
 $\forall f \in F \exists u_\alpha \in \mathcal{D}(\Omega) : \min_u \Phi_\alpha[u] = \Phi_\alpha[u_\alpha],$
 $\alpha > 0$

Procedure for minimization of Φ_α
 + a proper role for choosing α is
a regularizing algorithm for
 an ill-posed problem

Iterative Regularization
 is another effective method for solving
 ill-posed problems

Iteration number is
 the regularization
 parameter.

VIII.
Methods and Algorithms for Solving
Inverse Heat Transfer Problems
Direct Semi-Analytical Methods

METHODS OF SOLVING ILL-POSED INVERSE PROBLEMS

Universal methods: a priori information of most general character

Examples: Tikhonov's regularization method;
~~~~~ Iterative regularization method

Problem-oriented methods: specific data on the problem

Example: Direct methods -

Boundary IHCP:

1. A boundary-value formulation.
2. The Cauchy formulation.
3. A variational formulation.

Direct Semi analytical  
Direct Numerical methods  
Regularization of semi-analytical forms  
Regularization of numerical forms  
Iterative Regularization

# Direct Semi-Analytical Method

## Boundary IHCP

$$\frac{\partial T}{\partial \tau} = a \frac{\partial^2 T}{\partial x^2}, \quad x \in (0, b), \tau \in (0, \tau_m],$$

where  $a = \text{const} > 0$ .

$$T(x, 0) = \varphi(x), \quad x \in [0, b]$$

$$-\lambda \frac{\partial T(b, \tau)}{\partial x} = q^*(\tau), \quad \tau \in [0, \tau_m], \quad \text{known}$$

where  $\lambda = \text{const} > 0$ .

$$T(d, \tau) = T^*(\tau), \quad \tau \in [0, \tau_m] \quad 0 < d \leq b$$

$$q(\tau) = -\lambda \frac{\partial T(0, \tau)}{\partial x} \quad - ?$$

*object of investigation*

Boundary value statement of the inverse problem

*Superposition principle  
about Duhamel's  
Integral*

$$T(x, \tau) = \int_0^\tau q(\xi) \frac{\partial \vartheta(x, \tau - \xi)}{\partial \tau} d\xi + \int_0^\tau q^*(\xi) \frac{\partial \vartheta(b - x, \tau - \xi)}{\partial \tau} d\xi,$$

where

$$\vartheta(x, \tau) = \frac{1}{\lambda} \left\{ \frac{a\tau}{b} + \frac{3(b-x)^2 - b^2}{6b} + \frac{2b}{\pi^2} \sum_{k=1}^{\infty} \frac{(-1)^{k+1}}{k^2} \times \right. \\ \left. \times \exp \left[ -k^2 \pi^2 \frac{a\tau}{b^2} \right] \cos \left( k \pi \frac{b-x}{b} \right) \right\}.$$

*Solution for step change in  $q_{0v} = 0$  with  $q_{0v} = 0$*

Integral form of IHCP:

$$Au \equiv \int_0^{\tau} u(\xi) K(\tau - \xi) d\xi = f(\tau), \quad \tau \in (0, \tau_m],$$

$$u(\tau) = q(\tau); \quad K(\tau - \xi) = \partial \vartheta(d, \tau - \xi) / \partial \tau;$$

$$f(\tau) = T^*(\tau) - \int_0^{\tau} q^*(\xi) \frac{\partial \vartheta(b - d, \tau - \xi)}{\partial \tau} d\xi.$$

Volterra  
Integral  
equation  
of  
first kind

Instability of the problem:

↓  
Solution  
well-known  
to be  
unstable

$$u_{\delta}(\tau) = u(\tau) + \Delta u(\tau)$$

$$\Delta u(\tau) = C \sin \omega \tau$$

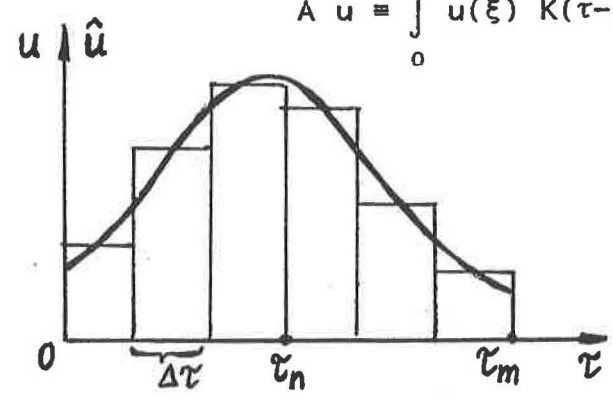
$$u(\tau) \in U, \quad u_{\delta}(\tau) \in U$$

$$\int_0^{\tau} u_{\delta}(\xi) K(\tau - \xi) d\xi \rightarrow \int_0^{\tau} u(\xi) K(\tau - \xi) d\xi$$

from  
Mirzabassi  
Stoltz

# Approximation

$$A u \equiv \int_0^{\tau} u(\xi) K(\tau - \xi) d\xi = f(\tau), \quad \tau \in (0, \tau_m]$$



$$\Delta \tau_n = \tau_n - \tau_{n-1}, \quad n = \overline{1, m}$$

$$\hat{u}_n = u\left(\tau_n - \frac{\tau_n - \tau_{n-1}}{2}\right)$$

lower  
triangular  
matrix

$$\sum_{i=1}^n \hat{u}_i \Delta \vartheta_{in} = f_n, \quad n = \overline{1, m}$$

where  $f_n = f(\tau_n)$ ,  $\Delta \vartheta_{in} = \int_{\tau_{i-1}}^{\tau_i} K(\tau_n - \xi) d\xi$

$K(\tau - \xi)$

time derivative  
of  
solution

$$T(x, \tau) = \int_0^{\tau} u(\xi) \frac{\partial \vartheta(x, \tau - \xi)}{\partial \tau} d\xi$$

$$\Delta \vartheta_{in} = \vartheta[d, \tau_n - \tau_{i-1}] - \vartheta[d, \tau_n - \tau_i]$$

result of ~~constant~~ Constant time steps:  $\Delta \tau = \frac{\tau_m}{m}$  # intervals  
in time domain

$$\Delta \mathcal{V}_{1n} = \Delta \mathcal{V}_{2, n+1} = \dots = \Delta \mathcal{V}_{m-n+1, m}$$

$$\sum_{i=1}^n \hat{u}_i \Delta \mathcal{V}_{n-i} = f_n, \quad n=1, 2, \dots, m$$

$$A_{\Delta} u = f$$

where

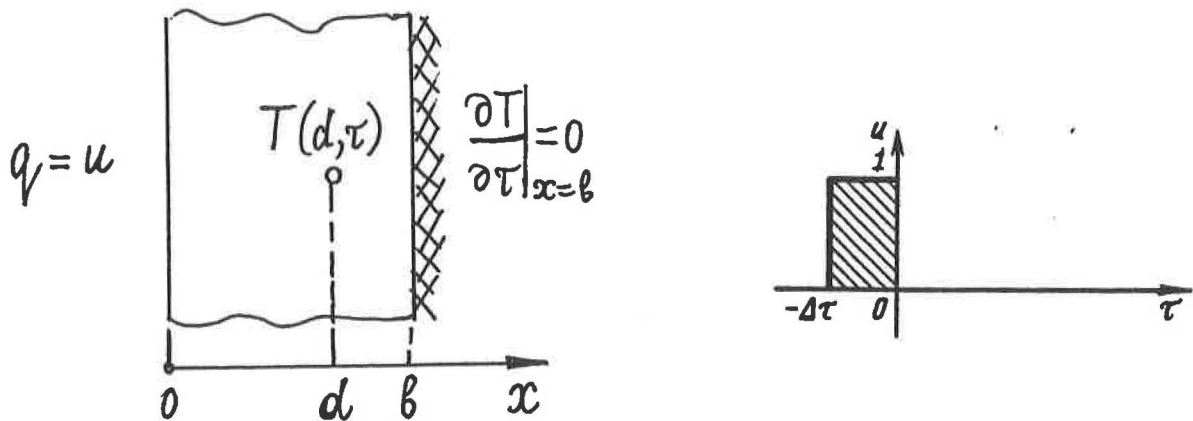
$$\Delta \mathcal{V}_{n-i} \equiv \Delta \mathcal{V}_{in} = \mathcal{V}(d, \Delta \tau (n-i+1)) - \mathcal{V}(d, \Delta \tau (n-i))$$

bi-diagonal  
equality  $\rightarrow$

$$A_{\Delta} = \begin{bmatrix} \Delta \mathcal{V}_0 & & & & & & \\ \Delta \mathcal{V}_1 & \Delta \mathcal{V}_0 & & & & & \\ \Delta \mathcal{V}_2 & \Delta \mathcal{V}_1 & \Delta \mathcal{V}_0 & & & & \\ \vdots & & & \ddots & & & \\ \Delta \mathcal{V}_m & \Delta \mathcal{V}_{m-1} & \dots & \Delta \mathcal{V}_2 & \Delta \mathcal{V}_1 & \Delta \mathcal{V}_0 & \end{bmatrix}$$

m coefficients instead of  $\frac{m(m+1)}{2} !$

$$\det A_{\Delta} = (\Delta \mathcal{V}_0)^m$$



$$\Delta \mathcal{V}_{n-i} = T(d, \Delta \tau(n-i)) \Big|_{q=u, \frac{\partial T}{\partial \tau} \Big|_{x=b} = 0}$$

$$\det A_{\Delta} > 0 \Rightarrow A_{\Delta}^{-1}$$

$$\hat{u}_n = \frac{1}{\Delta \mathcal{V}_0} \left( f_n - \sum_{i=1}^{n-1} \hat{u}_i \Delta \mathcal{V}_{n-i} \right), \quad n = \overline{1, m}$$

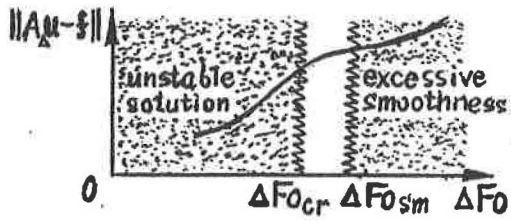
recurrent relation for  
upper triangular form

$$\Delta \mathcal{V}_{n-i} \xrightarrow{\Delta \tau \rightarrow 0} 0 \quad (!)$$

unstable for small  $\Delta \tau$



# STEP REGULARIZATION PRINCIPLE



Critical step values  
(the kernels have maximums):

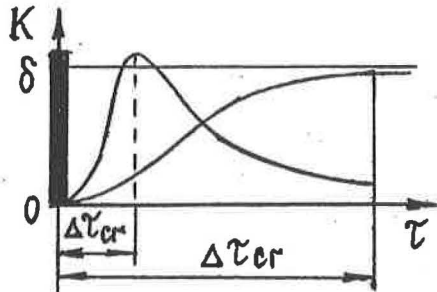
$$\Delta Fo_{cr} = Fo_e^* \text{ (thermal diffusivity)}$$

$$Fo_e^* = \frac{\alpha(\tau - \xi)^*}{l^2}$$

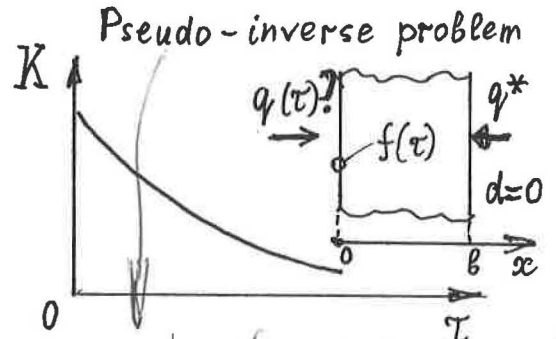
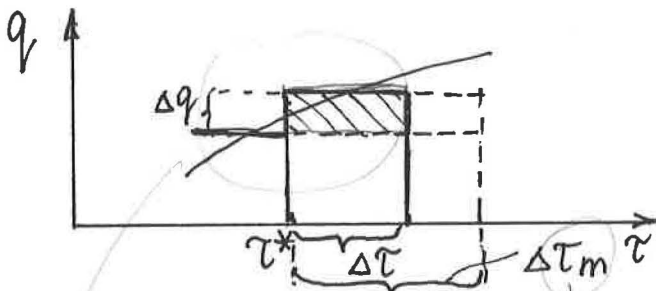
$l = d \text{ or } b$

characteristic length  
plate =  $l$   
semi-infinite =  $\infty$

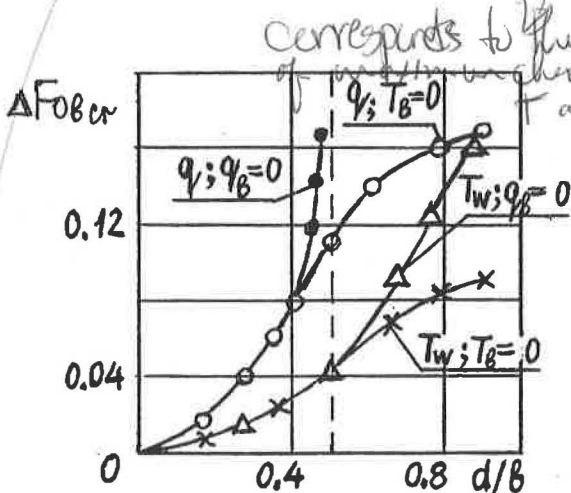
$$\Delta Fo_e > \Delta Fo_{cr}$$



Kernels of the integral equation



Construct  $q(x)$  at surface based on  $T_0(t)$  measured



$\Delta Fo_{cr}$  for a plate with a thickness  $b$

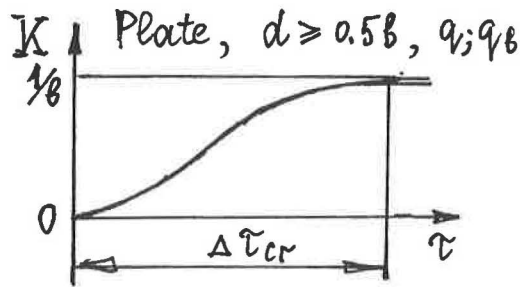
$$\Delta Fo_b > \Delta Fo_{bcr}$$

For  $\Delta Fo < \Delta Fo_{sm}$ , data w/ noise, can get oscillatory behavior, ~~even~~  
"Wh. Effect" data  
This method of finding  $\Delta Fo_{bcr}$  only applies to  $T_m$  with a maximum

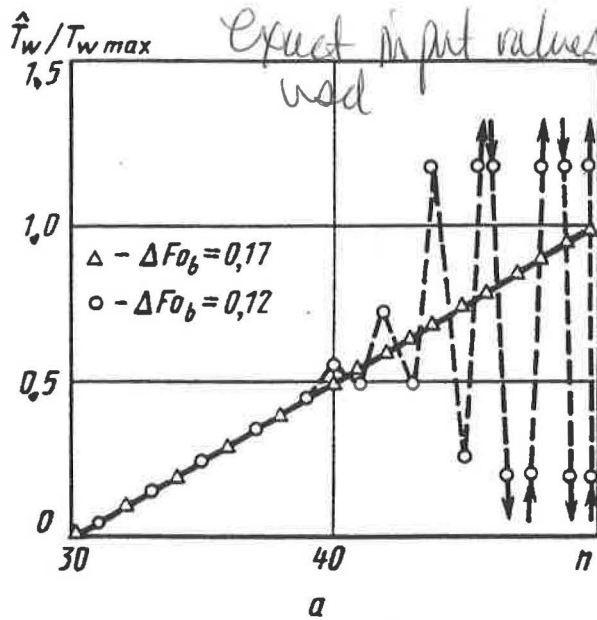
*Plus data, but*

If a kernel does not reach its maximum at the finite time:

$$\Delta \tau_{cr} = l^2 Fo^{**} / a$$

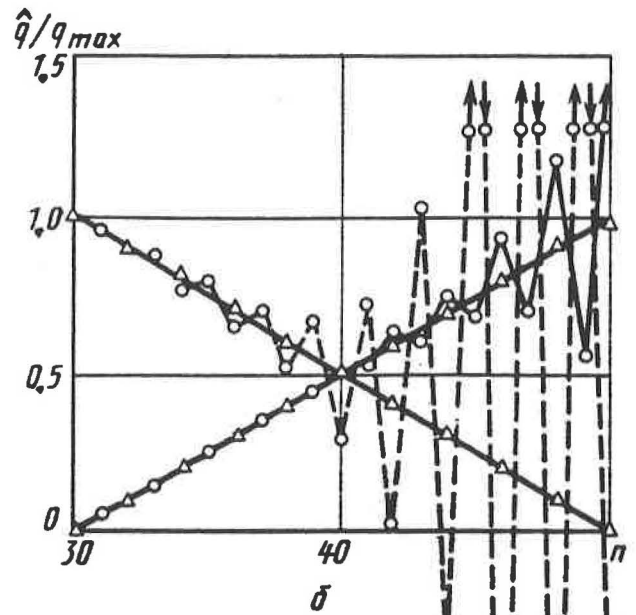


*Shser at  $x=l$ .*



$d=b, \Delta Fo_{bcr} \approx 0.17$

Plate



$d=b, \Delta Fo_{bcr} \approx 0.5$

## Perturbated Input Data

either

1. Preliminary smoothing of the input temperature data

OR

2. Matching of a temperature residual with the measurement error

$$m = \frac{\tau_m}{\Delta \tau} : \int_0^{\tau_m} [T(d, \tau, q_m) - f(\tau)]^2 d\tau \approx \delta_f^2$$

$$\text{where } \delta_f^2 = \int_0^{\tau_m} \sigma^2(\tau) d\tau$$

Smoothing of experimental data by cubic splines then can interpolate to find  $T_c(\text{spline})$

## Two-dimensional IHCP

General form of the recurrent algorithms:

$$u_n = A_0^{-1} \left( f_n - \sum_{i=1}^{n-1} \underbrace{A_{n-i}}_{\text{square matrix}} u_i \right), \quad n = 1, m, \quad \# \text{ intervals in time} \quad (1)$$

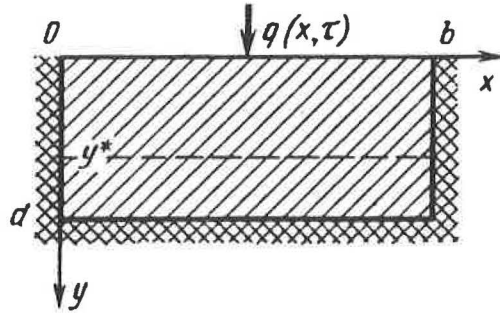
where  $u_n$  are vectors of unknown parameters;

$f_n$  are known vectors;

$A_s, s = 0, m-1$  are square matrixes;

$m$  is a number of time intervals.

## Two-dimensional Plate



$$\frac{\partial T}{\partial \tau} = a \left( \frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} \right), \quad x \in (0, b), \quad y \in (0, d), \quad \tau \in (0, \tau_m];$$

$$T(x, y, 0) = \psi(x, y), \quad x \in [0, b], \quad y \in [0, d];$$

$$-\lambda \frac{\partial T(x, 0, \tau)}{\partial y} = q(x, \tau), \quad \tau \in [0, \tau_m] \quad - \text{unknown function};$$

$$\frac{\partial T(x, d, \tau)}{\partial y} = \frac{\partial T(0, y, \tau)}{\partial x} = \frac{\partial T(b, y, \tau)}{\partial x} = 0, \quad \tau \in [0, \tau_m],$$

$$T(x, y^*, \tau) = f(x, \tau), \quad \tau \in [0, \tau_m], \quad 0 < y^* \leq d.$$

Integral form of the inverse problem:

$$\frac{a}{\lambda} \int_0^{\tau} d\xi \int_0^b q(x', \xi) G(x, y^*; x', 0; \tau - \xi) dx' = \bar{f}(x, y^*, \tau), \quad (4.7)$$

$$\tau \in (0, \tau_m], \quad x \in (0, b),$$

*Vollwert  
equation of  
Abz. Kind*

where

$$\bar{f}(x, y^*, \tau) = f(x, \tau) - \int_0^b dx' \int_0^d \psi(x', y') G(x, y^*; x', y'; \tau - \xi) dy';$$

*Green's function*

$$G(x, y; x', y'; \tau - \xi) = \frac{1}{bd} \left\{ 1 + 2 \sum_{r=1}^{\infty} \cos \frac{r\pi x}{b} \cos \frac{r\pi x'}{b} \times \right.$$

$$\left. \times \exp \left[ -\frac{ar^2 \pi^2 (\tau - \xi)}{b^2} \right] \right\} \left\{ 1 + 2 \sum_{r=1}^{\infty} \cos \frac{r\pi y}{d} \cos \frac{r\pi y'}{d} \times \right.$$

$$\left. \times \exp \left[ -\frac{ar^2 \pi^2 (\tau - \xi)}{d^2} \right] \right\},$$

where

$G(x, y; x', y'; \tau - \xi)$  is the Green's function

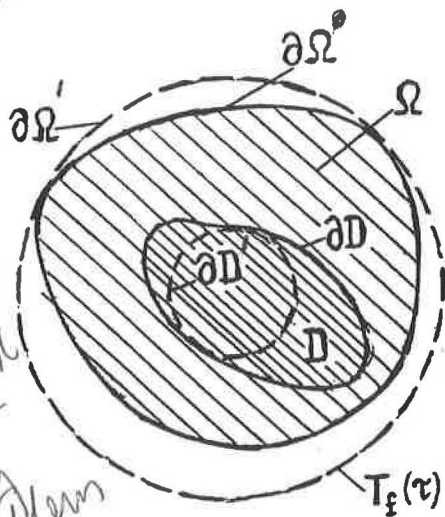


**IX.**  
**Methods for Solving Linear Inverse**  
**Heat Conduction Problems for**  
**Bodies with**  
**Movable Boundaries**

# METHOD OF FICTITIOUS BOUNDARIES

*Al-Saman 1974*

*Non characteristic Cauchy problem*



Let domain  $\Omega$  contains another domain  $D$ . Temperature  $T(p, \tau)$   $p \in \partial D$  is known.

## Four stages of the method:

1. Transfer from domain  $\bar{\Omega}$  and  $\bar{D}$  to new domains  $\bar{\Omega}'$  and  $\bar{D}'$  :

$$\bar{\Omega} \subseteq \bar{\Omega}', \quad \bar{D} \supseteq \bar{D}' ;$$

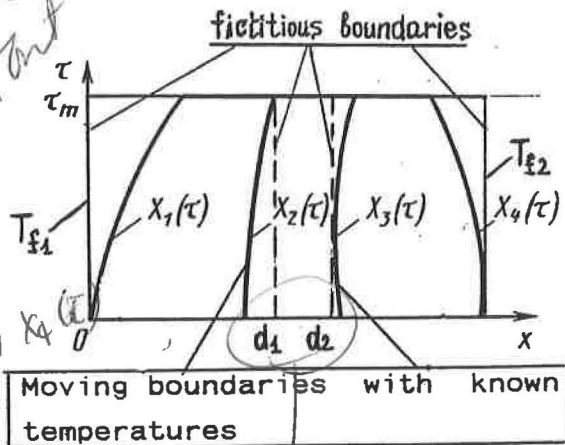
$\bar{\Omega}' - \bar{D}'$  is the domain of simple form,

2. Solve an appropriate direct problem in  $\bar{D}' : T(\tau)|_{\partial D'}, q(\tau)|_{\partial D}'$ .
3. Solve of IHCP in  $\bar{\Omega}' - \bar{D}' : T_f(\tau) = T(\tau)|_{\partial \Omega}'$ .
4. Solve a direct problem in  $\bar{\Omega}' - \bar{D}'$  and define the unknown boundary conditions at  $\partial \Omega$ .

## Examples of application (bodies with movable boundaries)

*Thermal properties of body are constant*

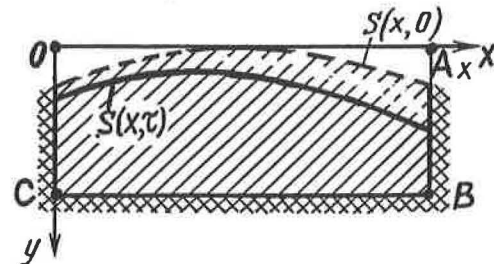
### 1. One-dimensional problem



*Fixed  $x_1(\tau), x_4(\tau)$*

*two fixed points*

### 2. Two-dimensional problem



The rectangle OABC is domain  $\bar{\Omega}'$

**X.**  
**Numerical Solution of Nonlinear**  
**IHCP**



non linear IHCP

Direct Finite difference (step regularization)

SOLUTION OF BOUNDARY IHCPs BY DIRECT NUMERICAL METHODS

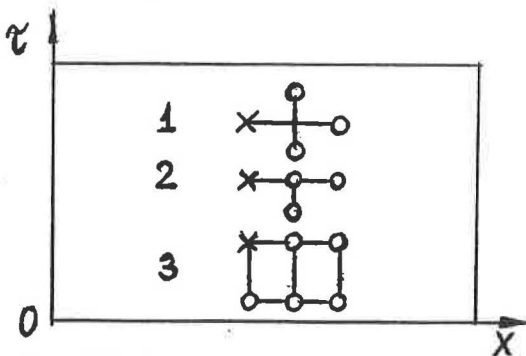
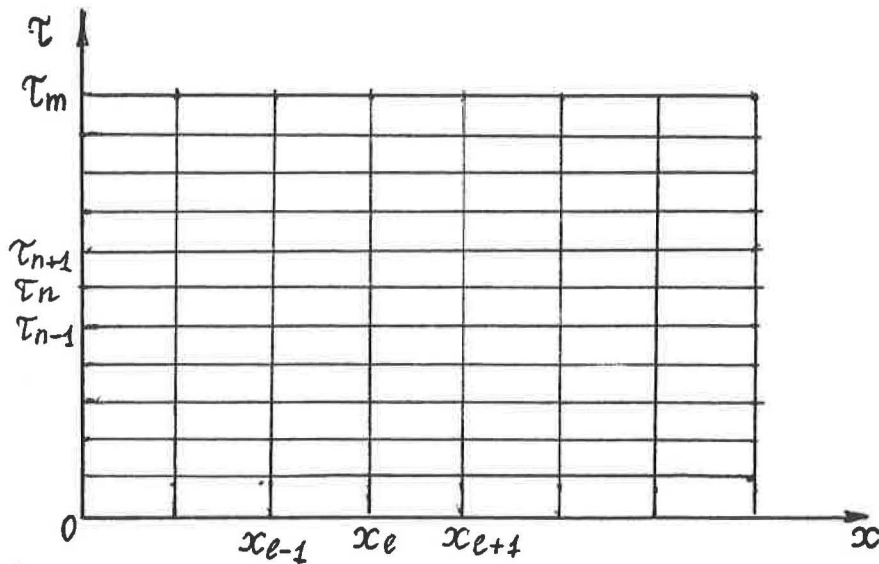
$$C(T) \frac{\partial T}{\partial \tau} = \frac{\partial}{\partial x} (\lambda(T) \frac{\partial T}{\partial x}), \quad x \in (0, b), \quad \tau \in (0, \tau_m];$$

$$T(x, 0) = \varphi(x), \quad x \in [0, b];$$

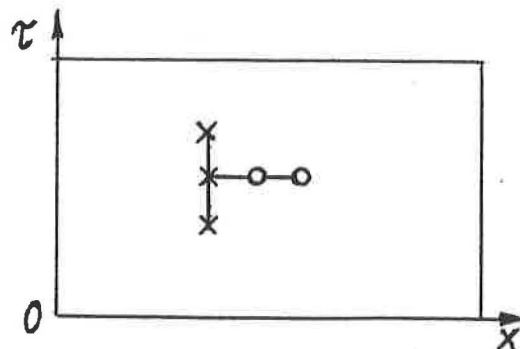
$$T(d, \tau) = f(\tau), \quad \tau \in [0, \tau_m];$$

$$-\lambda(T(b, \tau)) \frac{\partial T(b, \tau)}{\partial x} = q^*(\tau), \quad \tau \in [0, \tau_m],$$

where  $C(T), \lambda(T), \varphi(x), f(\tau), q^*(\tau)$



Explicit schemes



Implicit scheme

o = known  
x = T.B.D.

Condition of weak stability of finite-difference solution of IHCP:

$$\| u_n \| \leq C_n \| f_n \|, \quad (5)$$

where  $C_n$  is a positive constant, depending on parameters of approximation.

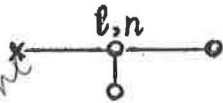
Condition of the weak stability:

Supplemental regularizing parameter  $\Delta Fo \geq \Delta Fo_{allowable}$

Scheme viscosity as a regularizing factor

The first differential approximation of a difference scheme:

"T-type" scheme



$$\frac{\partial T}{\partial \tau} |_{ln} + \frac{\Delta \tau}{2} \frac{\partial^2 T}{\partial \tau^2} |_{ln} = a \frac{\partial^2 T}{\partial x^2} |_{ln}$$

improves stability of inverse solution

Hyperbolic heat conduction equation:

$$\frac{w^2}{a} \frac{\partial T}{\partial \tau} + \frac{\partial^2 T}{\partial \tau^2} = w^2 \frac{\partial^2 T}{\partial x^2}$$

non-characteristic Cauchy problem?

Semi-infinite body, the first boundary-value problem

$$T(1, Fo) = T_w \left( Fo - \sqrt{\frac{\Delta Fo}{2}} \right) \exp \left[ -\frac{1}{\sqrt{2 \Delta Fo}} \right] +$$

Solution for hyperbolic equation

Modified Bessel function of first kind

$$\frac{1}{\sqrt{2 \Delta Fo}} \int_0^{Fo} T_w(\xi) \exp \left[ -\frac{Fo - \xi}{\Delta Fo} \right] \times$$

$$\times \frac{I_1 \left( \frac{\sqrt{(Fo - \xi)^2 - \Delta Fo/2}}{\Delta Fo} \right)}{\sqrt{(Fo - \xi)^2 - \Delta Fo/2}} d\xi,$$

where  $T_w(Fo)$  is the surface temperature ( $T(0, Fo) = T_w(Fo)$ );

$I_1(\cdot)$  is the modified Bessel's function of the first kind

$$\Delta Fo_{cr} \approx 0.04$$

The implicit difference scheme possesses higher viscous regularizing properties than the explicit scheme:

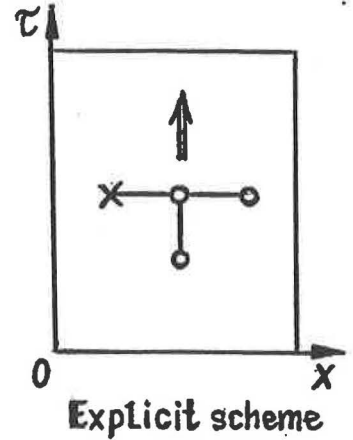
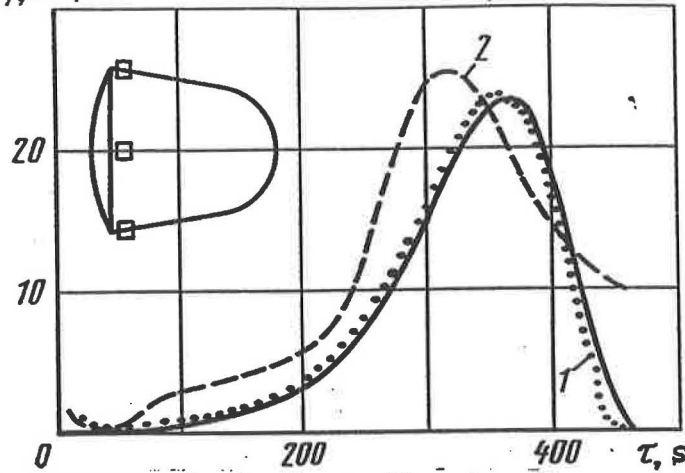
$$\Delta Fo_{cr} = 0.01 - 0.02$$

estimate of critical value for "T-type" discretization.

## PRELIMINARY SMOOTHING OF THE INPUT TEMPERATURE DATA

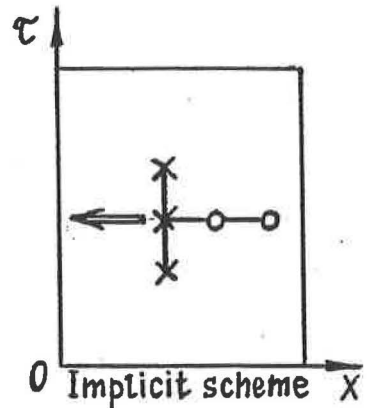
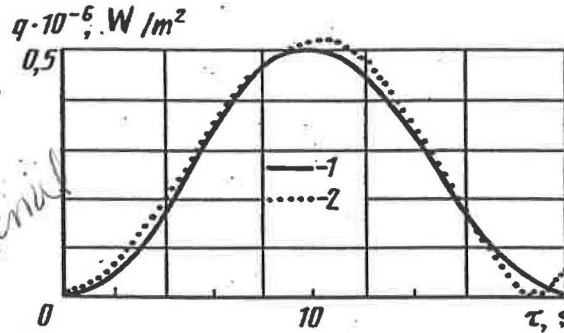
It is advisable to use algorithms of smoothing which give uniform approximation of the function and its derivatives.

$q, kW/m^2$



Recovery of the heat flux by the explicit T-type scheme in mentioned points of re-entry vehicle: — is a true solution. Error of input data  $3\sigma(\tau) = 0.08 \cdot T_{max}$ ,

$\Delta Fo_d = 0.05$ ; Results: ..... is for smoothing  $T_\delta(\tau)$  by the regularization method of the second order; --- is for smoothing  $T_\delta(\tau)$  by the least-squares technique (by "five points"),  $N = 10^3$ .



Recovery of the heat flux by the implicit scheme:

$$b = 0.002; a = 0.4 \cdot 10^{-6} - 0.143 \cdot 10^{-9} T + 0.408 \cdot 10^{-12} T^2, \frac{m^2}{s};$$

$$\lambda = 0.721 + 0.288 \cdot 10^{-3} T, \frac{kW}{mK}; \text{ — is a true solution;}$$

..... is the results of IHCP solution,  $\Delta\tau = 0.4 s$

**XI.**  
**Artificial Hyperbolization of Heat  
Conduction Equation**

Artificial Hyperbolization of Heat Conduction Equation  
in Solving a Boundary Inverse Problem

proposed by  
A. I. Ivanov in  
1971

$$\frac{\partial T}{\partial \tau} + \alpha \frac{\partial^2 T}{\partial x^2} = a \frac{\partial^2 T}{\partial x^2}, \quad x \in (0, b), \quad \tau \in (0, \tau_m], \quad (9)$$

noncharacteristic  
initial value  
Cauchy  
problem

where parameter  $\alpha$  corresponds to fictitious relaxation time

Inverse problem: it is required to find function  $T(x, \tau)$  if

$$T(x, 0) = 0, \quad 0 \leq x \leq b; \quad \frac{\partial T(x, \tau_m)}{\partial \tau} = 0, \quad 0 \leq x \leq d;$$

$$T(d, \tau) = T^*(\tau), \quad -\lambda \frac{\partial T(b, \tau)}{\partial x} = q^*(\tau), \quad 0 \leq \tau \leq \tau_m,$$

where  $T^*(\tau)$  and  $q^*(\tau)$  are known functions.

Condition for choice of  $\alpha$ :  $\left| \sum_{n=1}^m \left( T_{x_n}^\alpha - T_n^* \right)^2 - \delta^2 \right| = \min_{\alpha}$

where  $T_{x_n}^\alpha$  are temperatures, obtained from a solution of Fourier general heat conduction equation using a known boundary condition  $q^*(\tau)$  and condition  $q^\alpha(\tau)$  computed in the result of IHCP solution for hyperbolic equation (9);

$\delta$  is the known error of temperature data  $T^*$ .

hyperbolic is  
well posed  
where  
parabolic is  
ill posed

**XII.**  
**Tikhonov Regularization Method**

# REGULARIZATION OF VARIATIONAL FORMS OF IHCP

## Onedimensional problems

General integral form of linear boundary IHCPs:

$$\int_0^{\tau} u(\xi)K(\tau, \xi)d\xi = f(\tau), \tau \in (0, \tau_m],$$

where  $u(\tau)$  is the unknown function (heat flux, temperature of the surface, heat potential density).

$$Au = f, u \in U, f \in F$$

*Hilbert spaces*

$A^{-1}$  can be unbounded

$$f = f_{\delta}, \|\bar{f} - f_{\delta}\|_F \leq \delta$$

*known error*

$$\|Au - f_{\delta}\|_F \leq \delta$$

$\Rightarrow$

$D_{\delta}$

*Set of suspected solutions to*

$\Delta = \|Au - f_{\delta}\|$  is a residual

$$u = u_{\delta} \in D_{\delta} : \min_{u \in D_{\delta}} \|u - u^*\|_U$$

$U = W_2^k [0, \tau_m]$  is the Sobolev space

$$f \in L_2 [0, \tau_m]$$

$$\min_{u \in D_{\delta}} \|u - u^*\|_{W_2^k}^2;$$

$$D_{\delta} = \{u : \|Au - f_{\delta}\|_{L_2}^2 \leq \delta^2\},$$

*continuous and linear*

# Lagrange multiplier Lagrangian Method

$$F[u, u^*, \lambda, \gamma] = \|u - u^*\|_{W_2^k}^2 + \lambda (\|Au - f_\delta\|_{L_2}^2 + \gamma^2 - \delta_{L_2}^2)$$

auxiliary variable

$$\partial F[u, u^*, \lambda, \gamma] / \partial \lambda = 0$$

$$\partial F[u, u^*, \lambda, \gamma] / \partial \gamma = 0$$

$$\gamma = 0$$

$$\lambda: \|Au^\lambda - f_\delta\|_{L_2}^2 = \delta_{L_2}^2$$

$$\alpha = \frac{1}{\lambda} :$$

$$\min_{u \in W_2^k} \{ \Phi[u, u^*, \alpha] = \|Au - f_\delta\|_{L_2}^2 + \alpha \|u - u^*\|_{W_2^k}^2 ;$$

$$\|Au^\alpha - f_\delta\|_{L_2}^2 = \delta_{L_2}^2. \quad (A')$$

residual                      known error

(A)

Condition (A') is the principle (method) of residual

Norm in  $L_2$

$$\|z\|_{L_2}^2 = \int_0^{\tau_m} z^2(\xi) d\xi;$$

Norm in  $W_2^k$

$$\|z\|_{W_2^k}^2 = \int_0^{\tau_m} \sum_{j=0}^k \left[ \frac{d^j z(\xi)}{d\xi^j} \right]^2 r_j(\xi) d\xi,$$

$$\min_{u \in W_2^k} \{ \Phi[u, u^*, \alpha] = \int_0^{\tau_m} d\tau \left[ \int_0^{\tau} u(\xi) K(\tau, \xi) d\xi - f_\delta(\tau) \right]^2 + \quad (B)$$

$$+ \alpha \int_0^{\tau_m} \sum_{j=0}^k r_j(\xi) [u(\xi) - u^*(\xi)]^{(j)2} d\xi \},$$

$$\alpha: \int_0^{\tau_m} \left[ \int_0^{\tau} u^\alpha(\xi) K(\tau, \xi) d\xi - f_\delta(\tau) \right]^2 d\tau = \delta_{L_2}^2 \quad (C)$$

The number  $k=1$  or  $2$  is usually taken.

Also,  $r_j(\xi) = 1 \quad j = \text{all}$



Euler equation for  $\Phi$  :

$$\int_0^{\xi} u(\zeta) K_1(\xi, \zeta) d\zeta + \int_{\xi}^{\tau_m} u(\zeta) K_2(\xi, \zeta) d\zeta - \bar{b}(\xi) + \alpha \sum_{j=0}^k (-1)^j [r_j(\xi) (u(\xi))^{(j)}]^{(j)} = 0,$$

where  $K_1(\xi, \zeta) = \int_{\xi}^{\tau_m} K(\tau, \xi) K(\tau, \zeta) d\tau;$

$$K_2(\xi, \zeta) = \int_{\xi}^{\tau_m} K(\tau, \xi) K(\tau, \zeta) d\tau;$$

$$\bar{b}(\xi) = \int_{\xi}^{\tau_m} f_0(\tau) K(\tau, \xi) d\tau.$$

Boundary conditions:

$$\sum_{j=p}^k (-1)^j [r_j(\xi) u^{(j)}(\xi)]^{(j-p)} \Big|_{\xi=0; \tau_m} = 0, \quad p=1, 2, \dots, k$$

$$\Downarrow$$

$$\{u^\alpha(\xi)\} \Rightarrow u_\delta^\alpha(\xi)$$

Can discretize and

Solve  $\rightarrow$  but another approach suggested by

Alisanar  $\rightarrow$

# Regularization of Semi-analytical Solution of IHCP

$$\sum_{i=1}^n \hat{u}_i \varphi_{ni} = f_{\delta n}, \quad n = \overline{1, m}$$

$$\boxed{\mathbf{A}_{\Delta} \mathbf{u} = \mathbf{f}_{\delta}}$$

*Same as before*

where  $\mathbf{A}_{\Delta}$  is the lower triangular matrix;

$$\mathbf{u} = \{\hat{u}_i\}_1^m; \quad \mathbf{f}_{\delta} = \{f_{\delta n}\}_1^m$$

If  $k = 2, u^* = 0; \quad r_0 = 0, r_1(\tau) = r_1 = \text{const} \geq 0, r_2(\tau) = r_2 = \text{const} \geq 0,$

$$\begin{aligned} \Phi_{\alpha}[u] = & \sum_{n=1}^m \left( \sum_{i=1}^n \hat{u}_i \varphi_{ni} - f_{\delta n} \right)^2 + \frac{\alpha r_1}{\Delta \tau^2} \sum_n (\hat{u}_n - \hat{u}_{n-1})^2 + \\ & + \frac{\alpha r_2}{\Delta \tau^4} \sum_n (\hat{u}_{n+1} - 2\hat{u}_n + \hat{u}_{n-1})^2. \end{aligned}$$

$$\mathbf{d}: \quad \sum_{n=1}^m \left( \sum_{i=1}^n \hat{u}_i^{\alpha} \varphi_{ni} - f_{\delta n} \right)^2 = \delta_{Em}^2$$

*Choice determined by degree of smoothness and B.C.'s*

$$(\mathbf{B} + \alpha \mathbf{C}) \mathbf{u} = \mathbf{d} + \mathbf{g}$$

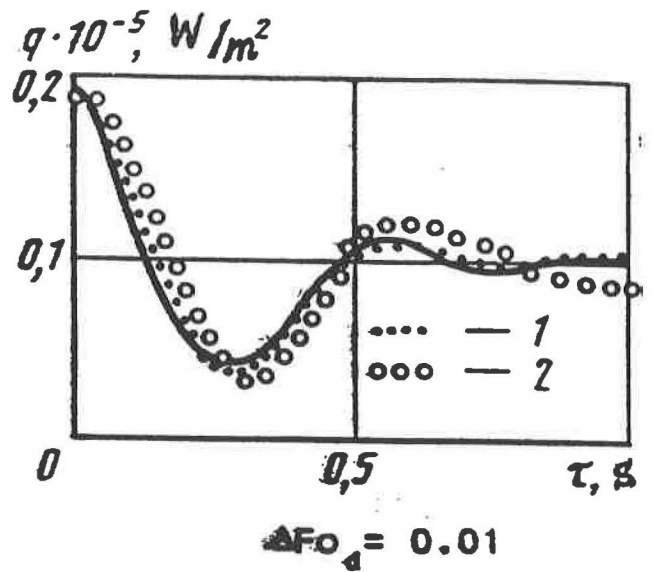
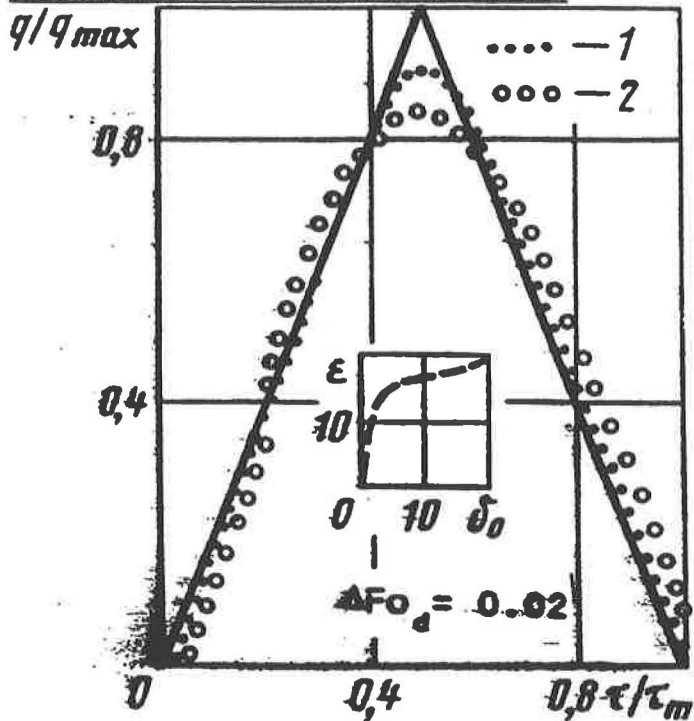
where

$$\mathbf{B}: \quad b_{kl} = \sum_{n=l}^m \varphi_{nk} \varphi_{nl}, \quad b_{kl} = b_{lk}, \quad k, l = \overline{1, m}$$

$$\mathbf{d}: \quad d_k = \left\{ \sum_{n=k}^m f_{\delta n} \varphi_{nk} \right\}, \quad k = \overline{1, m}$$



Examples of computations



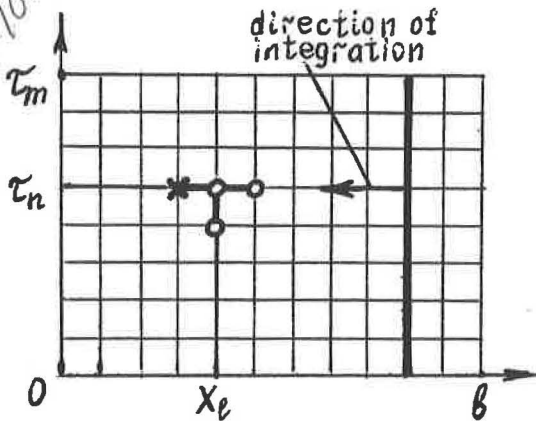
Normal distribution of errors in input temperatures;  
 — is true solutions; .... is solutions of IHCP when  $3\sigma = 0.01 T_{max}^*$ ; ..... is solutions of IHCP when  $3\sigma = 0.1 T_{max}^*$ .

## REGULARIZATION OF NONLINEAR IHCP

depend on choice of discretization scheme

Suggested by A. I. Priglas in 1970's

1. By-interval of time regularization.
2. Regularized continuation of the solution of a heat conduction equation.



System of regularizing functions:

$$\Phi_\alpha [T_l] = \|M_l T_l - g_l\|_{E_m}^2 + \alpha_l \Omega_l,$$

where  $l$  is an index of the space levels;

$M_l$  is a transition matrix from space layers  $l+2, l+1$  to layer  $l$ ;

$T_l = [T_{l1}, T_{l2}, \dots, T_{lm}]^T$  is an unknown vector of temperatures in  $l$ th layer;

$g_l$  is a vector of known parameters;  $\alpha_l$  is a regularization parameter;  $\Omega_l$  is a stabilization function, for example:

$$\Omega_l = k_1 \|\Delta T_l\|_{E_m}^2 + k_2 \|\Delta^2 T_l\|_{E_m}^2, \quad k_1 \geq 0, \quad k_2 > 0,$$

where  $\Delta$  and  $\Delta^2$  are the first and second finite differences, respectively.

$$d = d_p : \rho_l(\alpha) \equiv \sum_{n=1}^m (T_{Ln}^\alpha - T_n^*)^2 = \delta^2$$

$$\delta^2 \approx \sum_{n=1}^m \sigma_n^2$$

$$q(\tau) = -\lambda(T(0, \tau)) \partial T(0, \tau) / \partial x$$

Same finite difference scheme must be used in forward solver and  $\alpha$  solver?

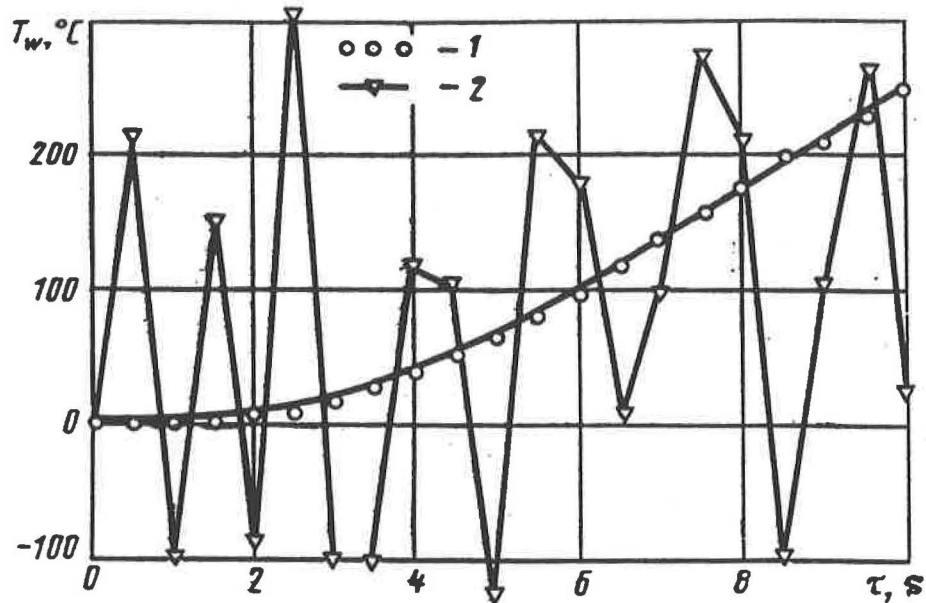
Choice of regularization parameters  $\alpha_1$ :

$$\alpha_1 = \alpha_{1 \text{ residual}} : \sum_{n=1}^m \left( T_{Ln}^\alpha - T_n^* \right)^2 = \delta_{E_m}^2,$$

where  $T_{Ln}^\alpha$  is temperature calculated at the point  $x = b$  (from

the solution of a direct problem);

$T_n^*$  is the experimental temperature.



Example of computations: — is an exact solution;

Normal distribution of errors in the input temperatures,

$3\sigma = 0.05 \cdot T_{\max}^*$ ;  $\lambda(T)$  and  $C(T)$  corresponded to a graphite

$q^*(\tau) = 0$ ;

1 - the regularized numerical method;

2 - the direct numerical method ( $\alpha_1 = 0$ ,  $l = 1, L$ ).



**XIII.**  
**Iterative Regularization Method**



## ITERATIVE REGULARIZATION

The iterative regularization method can be used for solving various inverse problems (retrospective, boundary, coefficient geometric and combined problems) both linear and nonlinear, in nonoverdetermined and overdetermined formulations.

### Linear case

$$\boxed{Au = f}, \quad A : U \Rightarrow F; \quad (20)$$

$A \in \mathcal{L}(U, F)$ ;  $U, F$  are Hilbert spaces;

$A^{-1}$  - unbounded or does not exist;

$\{f, A\}$  is precise initial data.

Assume that  $U_f = \{u \in U : Au = f\} \neq \emptyset$ .

$$\Delta(u) = \|Au - f\|_F, \quad J(u) = \frac{1}{2} \|Au - f\|_F^2 = \frac{1}{2} \Delta^2(u)$$

$$\boxed{J'u = A^*(Au - f)}; \quad \omega = -J'u$$

$$A^*: F \rightarrow U \quad (Au, f)_F = (u, A^*f)_U, \quad u \in D_A, f \in D_{A^*}$$

### Steepest descent method

$$u_{n+1} = u_n - \beta_n J'u_n, \quad \beta_n = \|J'u_n\|_U^2 / \|A J'u_n\|_F^2. \quad (21)$$

### Conjugate gradient method

$$u_{n+1} = u_n - \beta_n p_n, \quad p_n = J'u_n + \gamma_{n-1} p_{n-1}, \quad p_0 = J'u_0, \quad (22)$$

$$\beta_n = \left( J'u_n, p_n \right)_U / \|A p_n\|_F^2,$$

$$\gamma_{n-1} = \left( J'u_n, J'u_n - J'u_{n-1} \right) / \|J'u_{n-1}\|^2,$$

where  $J'u_n = A^*(Au_n - f)$  - the gradient of residual functional.

### Exact initial data

V.M.Friedman (1962), W.J.Kammerer, M.Z.Nashed (1972):

$$\lim_{n \rightarrow \infty} u_n = u^\circ, \quad u^\circ = \operatorname{argmin}_{u \in U_f} \|u - u_0\| - \text{normal solution}$$

*initial estimate*

*1 Max  
Convergence  
Super-linear Rate  
Convergence*

*Steepest descent  
Simple  
Iteration*

*conjugate  
gradient*

finite dimensional operator

errors from measurements

Initial data with errors

$$A_h u = f_\delta, \quad u \in U, \quad f_\delta \in F, \quad (23)$$

where  $A_h \in \mathcal{L}(U, F)$ ,

$\{f_\delta, A_h\}$  is given approximation to initial data:

$$\|A_h - A\| \leq h; \quad f_\delta = f + \tilde{f}, \quad \|\tilde{f}\|_F \leq \delta$$

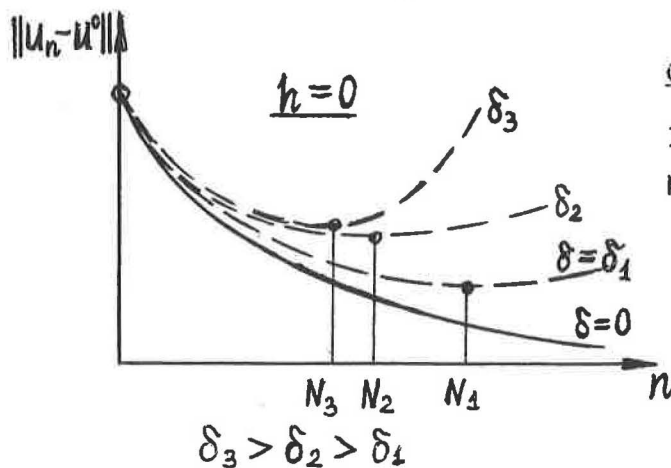
$\sigma = \{\delta, h\}$  is the initial data error

Case 1. The gradient methods for solving ( ) may be even divergent

Case 2. The gradient sequences converge to certain elements  $u_\sigma$

$$\sigma = \{\delta, h\} \Rightarrow u_\sigma \quad u_\sigma$$

$$u_\sigma \xrightarrow{\sigma \rightarrow 0} \bar{u} \in U_f$$



Question:

Is there any way of choosing  $N(\sigma)$  which would provide

$$u_{N(\sigma)} \xrightarrow{\sigma \rightarrow 0} u^0 ?$$

**JES !**

1) converge with exact data necessary, but not sufficient

2)

Sufficient conditions for regularization of a certain iterative method

$$u_{n+1} = \Phi ( u_n, \delta, h ) . \quad ( 24 )$$

Theorem 1. If

- 1) for  $\delta = h = 0 \quad \exists \quad \lim_{n \rightarrow \infty} u_n = \bar{u} \in U_f \quad (\bar{u} = \bar{u}(u_0))$ ;
- 2)  $\Phi ( u_n, \delta, h )$  is continuous at all points  $\{ u, 0, 0 \}$  ~~except~~ maybe  $\{ u, 0, 0 \}$ :  $u \in U_f$ ;
- 3)  $\forall u \in U_f, \quad \Phi ( u, 0, 0 ) = u$ .

Then  $\exists N(\sigma): \lim_{\sigma \rightarrow 0} u_{N(\sigma)} = \bar{u}$ .

Theorem 2. Steepest descent method and conjugate gradient method satisfy conditions of Theorem 1.

Thus, appropriate regularized approximations converge to normal (with respect to initial approximation) solutions of Eq. (20) with  $\sigma$  error tending to zero.

### HOW TO CHOOSE $N(\sigma)$ ?

Residual criterion:

Denote  $\Delta_n = \|A_h u_n - f_\delta\|_F$ ,  $\Delta_r = h \|u^\circ\| + \delta$ .

Theorem 3. For the steepest descent method

$$\exists N_r = \min_n \left\{ n: \frac{\Delta_n^2 + \Delta_{n+1}^2}{2\Delta_n} < C \Delta_r \right\}, \quad C > 1$$

and  $\lim_{\sigma \rightarrow 0} u_{N_r} = u^\circ$ .

$$\|u_n - u^\circ\| \geq \|u_{n+1} - u^\circ\|, \quad \forall n < N_r.$$

Similar criterion has also been obtained for the conjugate gradient method.

$$h \|u^\circ\| \ll \delta$$

### Generalized Residual Criterion

If solution to (20) is unique, then  $u^\circ$  in  $\Delta_r$  may be replaced by  $u_n$

$$\Delta_{rn} = h \|u_n\| + \delta$$

*usually not known*

*useful when met*

Nonlinear case

The validity of this approach for solution of ill-posed problems in nonlinear formulations has been demonstrated by the computer-experiment technique.

Frechet derivative  
a linear operator

$$Au = f, \quad u \in U, \quad f \in F,$$

where  $A: U \rightarrow F$  is a nonlinear continuous Frechet differentiable operator;  $U$  and  $F$  are Hilbert spaces

The gradient  $J'u = (A'u)^*(Au - f),$

where  $A'u$  is the Frechet derivative of the operator  $A$  at the point  $u$ ;

$(A'u)^*$  is the operator adjoint of the operator  $A'$

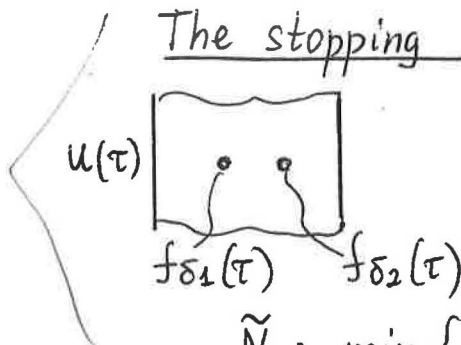
The steepest descent method:

$$u_{n+1} = u_n - \beta_n J'u_n, \quad n = 0, 1, \dots,$$

$$\beta_n : J(u_{n+1}) = \min_{\beta \geq 0} J(u_n - \beta J'u_n)$$

① || If the input data are first smoothed it is possible to use the traditional iteration-stopping methods ( e.g.  $\|u_{n+1} - u_n\|_U \leq \epsilon$  ) .

The stopping by additional measurement



$u(\tau)$  is unknown

$$f_{\delta_1}(\tau) = f_1(\tau) + \Delta f_1(\tau)$$

$$f_{\delta_2}(\tau) = f_2(\tau) + \Delta f_2(\tau)$$

additive  
random  
errors

$$\tilde{N} : \min_n \left\{ \int_0^{\tau_m} [T(u_n(\tau), d_2, \tau) - f_{\delta_2}(\tau)]^2 \right\}$$

②

Determination of the gradient of the residual functional

$$J [ u ] = \frac{1}{2} \| A u - f \|_F^2 \implies J' u .$$

Two analytical methods:

- with help Green's functions ( for linear problems );
- on the base of adjoint problems ( both for linear and nonlinear problems );  $(A'u)^*$ .

An account of a priori information about a solution:

- qualitative information, such as, smoothness of unknown functions;
- quantitative information about the values of the functions and their derivatives.

Two methods:

- 1) A direction of descent is chosen in the initial space  $L_2$  or  $R^n$ , but in such a way that obtained approximations remain in the class of smooth functions.
- 2) The iterative sequence is constructed directly in Sobolev's space  $W_2^1$ .

Modifications of gradient algorithms ( for solution of  
multiparameter inverse problems )

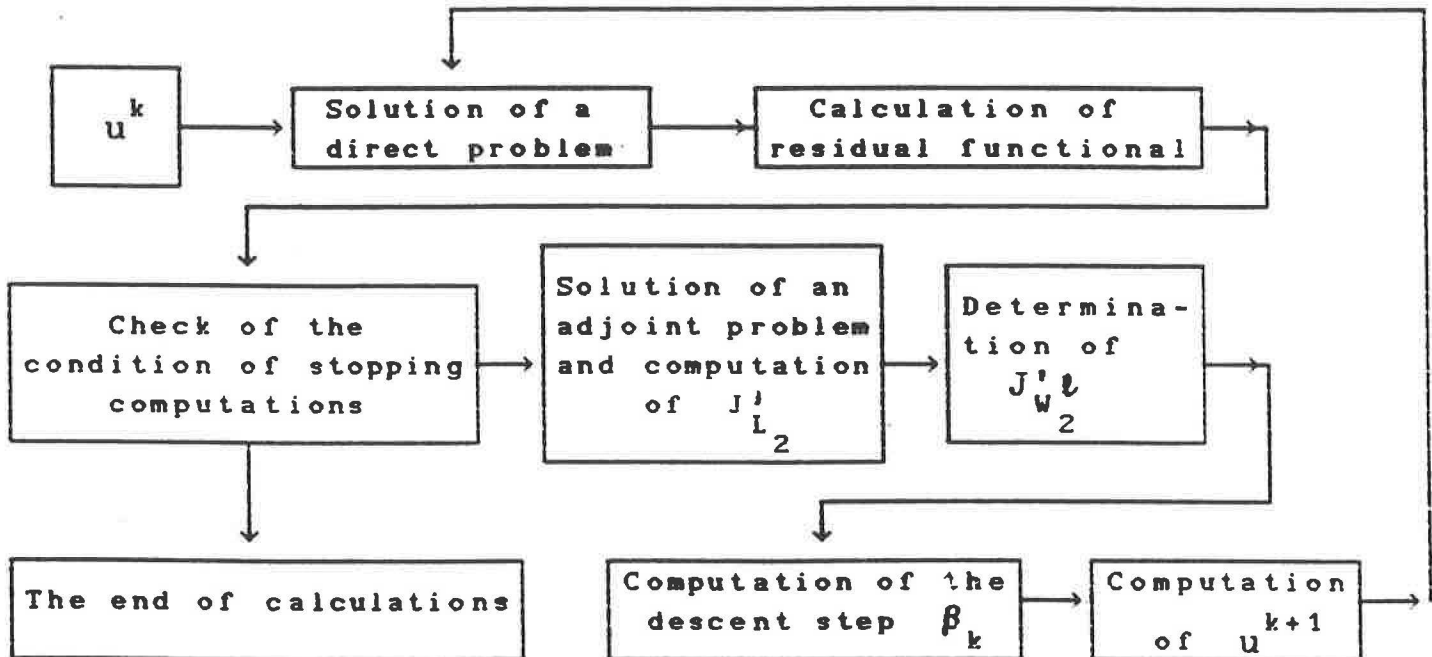
- Two cases:
- 1) To determine simultaneously a certain set of functions and parameters (e.g. several coefficients in equation with partial derivatives, two boundary conditions, boundary and initial conditions, and so on ).
  - 2) To consider smoothness of unknown function when the function is represented in terms of one of its derivatives and in terms of values at specific points.

The gradient-method modifications: instead of the scalar quantity of descent step the descent-step vector is determined at each iteration for each individual component on the basis of residual minimization.

Stopping the iteration, when initial data error is unknown

1. Stopping by additional measurements
2. Stopping by the increment of functional

A general flow-chart of the computational algorithm





## Coefficient Inverse Heat Conduction Problem

$$C(T)T_\tau = (\lambda(T)T_x)_x, \quad (x, \tau) \in Q = (0, b) \times (0, \tau_m];$$

$$T(x, 0) = \xi_0, \quad x \in [0, b];$$

$$T(0, \tau) = T_1(\tau), \quad T(b, \tau) = T_2(\tau), \quad \tau \in [0, \tau_m];$$

$$T(d_i, \tau) = f_i(\tau), \quad i = \overline{1, N}, \quad \tau \in [0, \tau_m],$$

$$0 < d_1 < \dots < d_N < b$$

*only all measurements  
essential for  
uniqueness -  
but more  
is better*

where  $C(T)$ ;  $T_1(\tau)$ ;  $T_2(\tau)$ ;  $f_i(\tau)$ ,  $i = \overline{1, N}$  are known functions;  
 $\xi_0$ ;  $b$ ;  $\tau_m$ ;  $d_i$ ,  $i = \overline{1, N}$  are given numbers

$$\lambda(\tau) - ?$$

$$\underline{\lambda(\tau), \tau \in [T_0, T_M]}$$

$$\lambda(\tau): \min_{\lambda(\tau)} |J(\lambda) - \delta_J^2|,$$

$$J(\lambda) = \sum_{i=1}^N \int_0^{\tau_m} \rho_i(\tau) [T(\lambda, d_i, \tau) - f_i(\tau)]^2 d\tau$$

*residual*

*weights for different  
measurements*

## Approximation of $\lambda(T)$ by cubic B-splines

Uniform grid for  $[T_0, T_M]$ :

$$\{T_j = T_0 + jH\}, j = \overline{0, M}, \quad \text{step } H = \frac{T_M - T_0}{M}$$

$$T_{-3} = T_0 - 3H, \quad T_{-2} = T_0 - 2H, \quad T_{-1} = T_0 - H;$$

$$T_{M+1} = T_0 + (M+1)H, \quad T_{M+2} = T_0 + (M+2)H; \quad T_{M+3} = T_0 + (M+3)H$$

Cubic B-splines:  $\{B_j\}_{-1}^{M+1}$

$$B_j(\bar{T}) = B_0(\bar{T} - jH), \quad j = -1, 0, 1, \dots, M+1;$$

$$B_0(\bar{T}) = \frac{1}{6H^3} [(\bar{T} - 2H)_+^3 - 4(\bar{T} - H)_+^3 + 6(\bar{T})_+^3 - 4(\bar{T} + H)_+^3 + (\bar{T} + 2H)_+^3];$$

$$\text{where } \bar{T} = T - T_0; \quad (\bar{T} - g)_+^3 = \begin{cases} (\bar{T} - g)^3 & \text{при } \bar{T} \geq g \\ 0 & \text{при } \bar{T} < g. \end{cases}$$

$$\tilde{\lambda}(T) = \sum_{j=-1}^{M+1} \lambda_j B_j(\bar{T}),$$

where  $\lambda_j$  are unknown parameters

## Variational formulation:

$$\lambda = [\lambda_{-1}, \lambda_0, \dots, \lambda_{M+1}]^T : \min_{\lambda} |\hat{J}[\lambda] - \delta^2_j|, \quad (L)^*$$

$$\text{where } \hat{J}(\lambda) = \sum_{i=1}^N \int_0^{\tau_m} \rho_i(\tau) [T(\tilde{\lambda}, d_i, \tau) - f_i(\tau)]^2 d\tau$$

## Iterative algorithm

$$\lambda^{k+1} = \lambda^{\bar{k}} - \beta_k p^k, \quad k = 0, 1, \dots, \bar{k},$$

$$\bar{k} : \hat{J}(\lambda^{\bar{k}}) \approx \delta^2_j; \quad \beta_k : \min_{\beta} \hat{J}(\lambda^k - \beta p^k),$$

*residual condition*

$$\text{where } p^k = \vec{J}'(\lambda^k) + \gamma_k p^{k-1},$$

$$\gamma_0 = 0; \quad \gamma_k = \frac{\sum_{j=-1}^{M+1} J_{\lambda_j}^{\prime k} (J_{\lambda_j}^{\prime k} - J_{\lambda_j}^{\prime k-1})}{\sum_{j=-1}^{M+1} (J_{\lambda_j}^{\prime k})^2}, \quad k > 0$$

*Can use same method for direct adjoint problem*

The gradient components:  $J'(\lambda)$

$$J'_{\lambda_j} = \sum_{i=1}^{N+1} \int_0^{\tau_m} d\tau \int_{d_{i-1}}^{d_i} \frac{\psi_i(x, \tau)}{C(x, \tau)} [T_{xx}(x, \tau) B_j(\bar{T}) + T_x^2(x, \tau) B_j'(\bar{T})] dx$$

$$j = -1, 0, \dots, M+1,$$

*adjoint variable*

where  $\psi(x, \tau)$  is adjoint variable

Descent step:

from linear estimator

$$\beta_k = \frac{\sum_{i=1}^N \int_0^{\tau_m} [T(\lambda^k, d_i, \tau) - f_i(\tau)] v(\Delta \tilde{\lambda}^k, d_i, \tau) d\tau}{\sum_{i=1}^N \int_0^{\tau_m} v^2(\Delta \tilde{\lambda}^k, d_i, \tau) d\tau}$$

where  $v(\Delta \tilde{\lambda}^k, d_i, \tau)$  is the temperature increment:

$$v_\tau = a_1 v_{xx} + a_2 v_x + a_3 v + \frac{1}{C} (\Delta \tilde{\lambda}^k T_{xx} + \Delta \tilde{\lambda}^k T_x^2),$$

$$(x, \tau) \in Q;$$

$$v(x, 0) = 0;$$

$$v(0, \tau) = v(b, \tau) = 0;$$

$$\Delta \tilde{\lambda}^k = \sum_{j=-1}^{M+1} P_j^k B_j(\bar{T}).$$

Solution sequence (each iteration)

Step 0  $\rightarrow$  data  $L, \rho, c, T_0$   $\overbrace{T_1, T_2}^{\text{boundary temps}}$   
 $(T_i, f_i), \rho_i \approx 1$  (can be)

Need some  $\lambda_0(T) = \lambda^0 = \text{const}$  (maybe)

Step 1  $\rightarrow$   $k = k+1$  iteration # increment  
 - Solve direct problem using current  $\lambda$   
 - Calculate residual, if  $\leq \delta^2 \rightarrow$  done

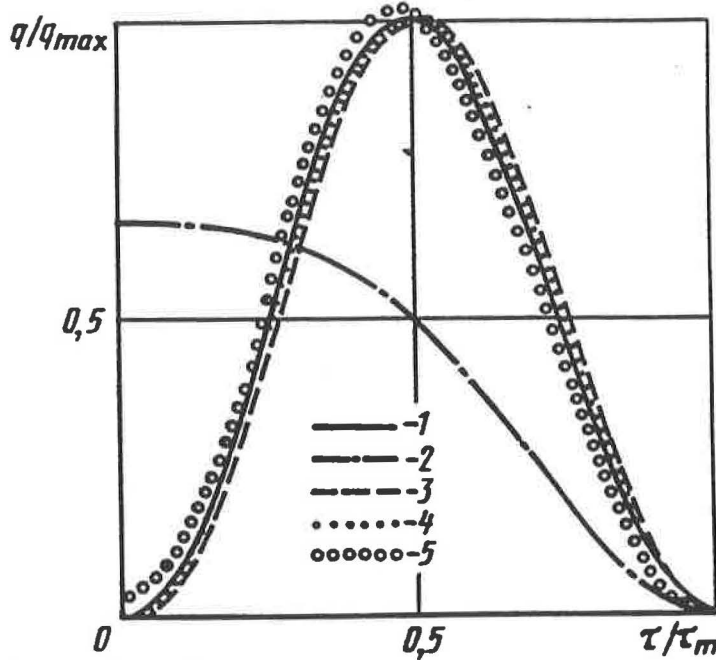
Step 2 Solve adjoint problem for  $\Psi(x, t)$  requires  $T(d_i, \tau) - f_i(\tau)$   
 from direct problem and data.

Step 3 if  $k \geq 1$  compute  $\gamma_k$  ( $\gamma_0 = 0$ )

Results of calculations

I. Boundary IHCP

Linear cases and non-disturbed data (space  $L_2$ )

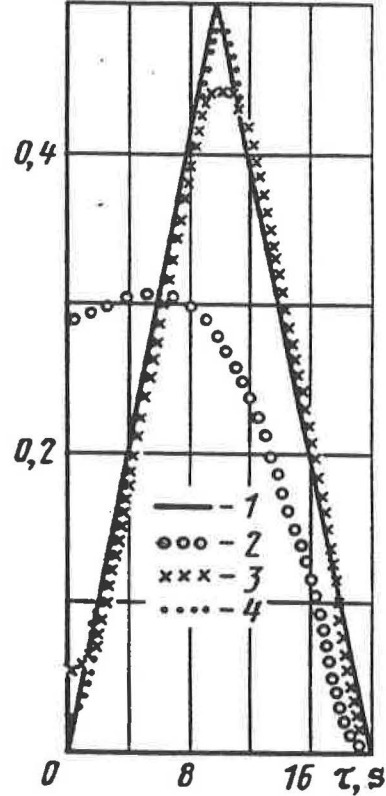


$b = d, \Delta Fo_b = 0.01$

1 - a true solution

2, 3, 4 - the 1st, 9th and 50th approximations (conjugate-gradients); 5 - 50th approximation (steepest descent)

$q \cdot 10^{-6}, W/m^2$

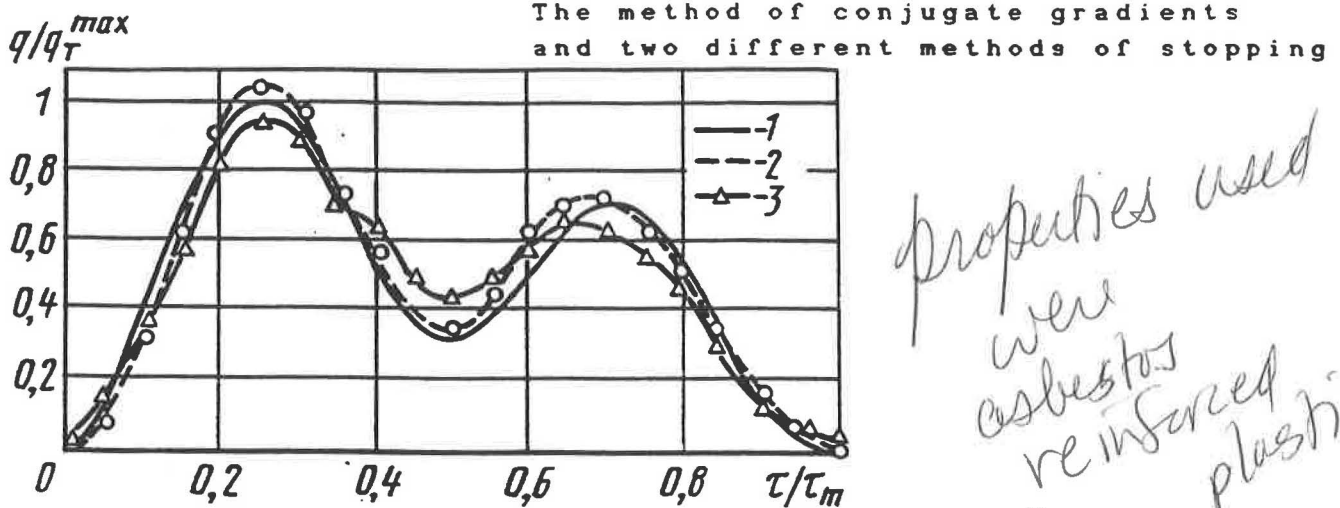


$b = 0.003 \text{ m}, d = 0.002 \text{ m}$   
 $\Delta Fo_b = 0.015$

2, 3, 4 - the 1st, 3d and 100th approximations (conjugate gradients)

*It is less than  
 10% - "Step regularization"  
 effect was not present*

Nonlinear cases and disturbed data (space  $L_2$ )



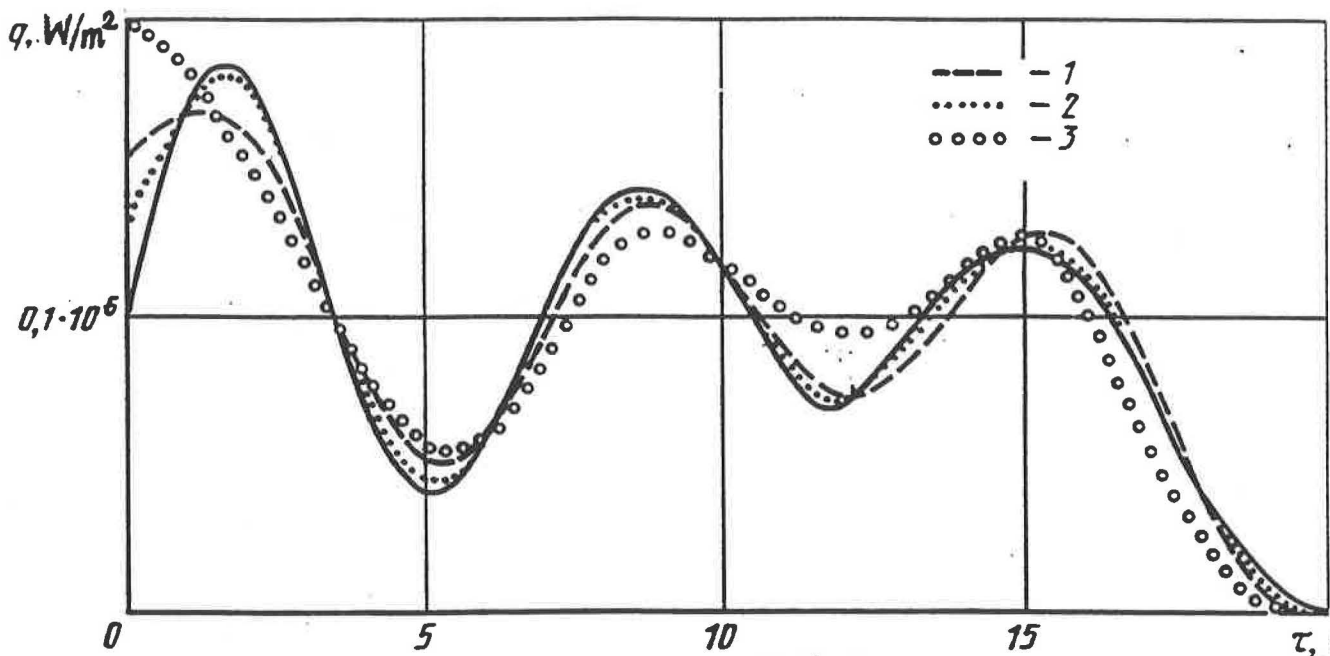
*properties used  
were  
asbestos  
reinforced  
plastic*

Normal law with dispersion of errors,  $3\sigma = 0.05 T_{max}^*$ ;  
 $d = 0.42 b$ ,  $0.06 \leq \Delta F_{o_d} \leq 0.1$

1 - the unknown function; 2 - stopping by the additional measurement at point  $d' = 0.08 \cdot b$  (  $N = 10$  ); 3 - stopping by the criterion of residual (  $N = 7$  )

*data had  
5% of max T  
random error*

Smoothed data



$b = 0.003\text{m}; \lambda = 0.721 + 0.288 \cdot 10^{-3} T, \text{ kW/mK};$

$a = 0.4 \cdot 10^{-6} - 0.143 \cdot 10^{-9} T + 0.408 \cdot 10^{-12} T^2, \text{ m}^2/\text{s}$

(full curve - true solution)

1 and 2 - 30th and 60th approximations for non-disturbed data; 3 - the 60th approximation on smoothed data (initial values of temperature included errors distributed by normal law with dispersion  $3\sigma = 0.05 \cdot T_{\text{max}}^*$ )

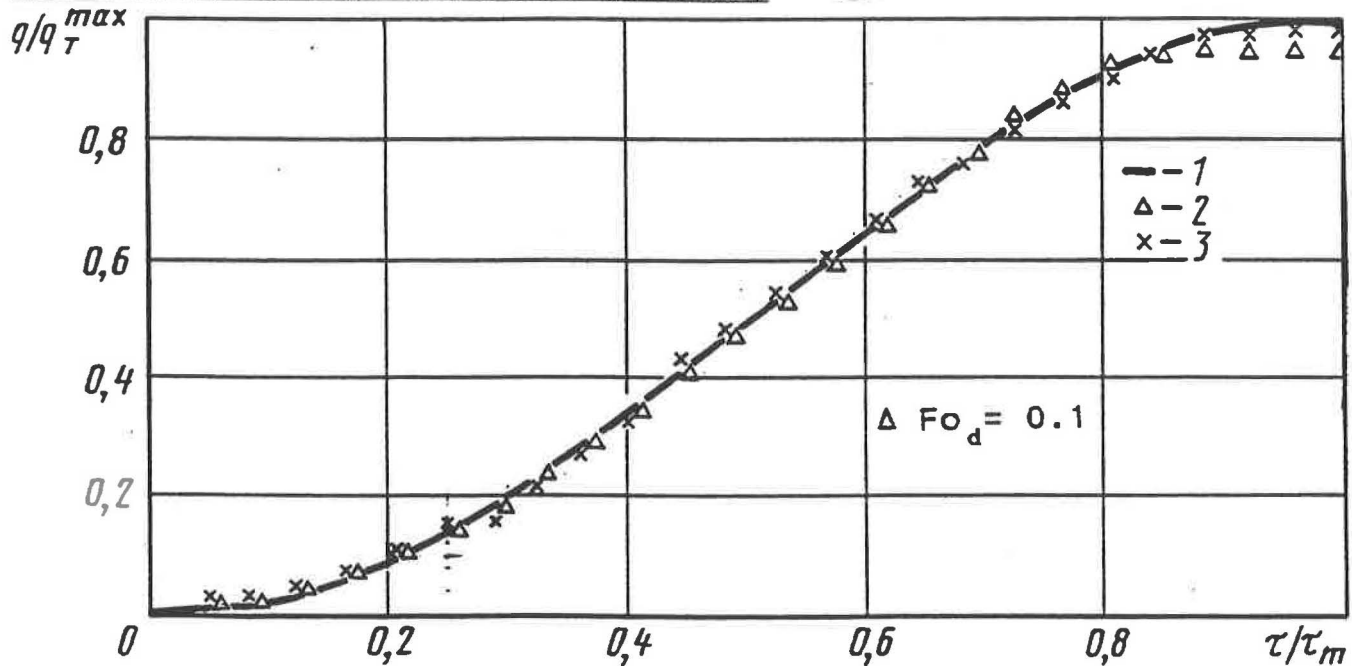
*preliminary smoothing with 2nd order regularization*

*No instability  
Can use usual methods for stopping*

*since data was pre-smoothed!*

*Suboptimal  
Space*

-----  
Solution of the boundary IHCP in space  $W_2^1$  (an account of smoothness of the unknown function)

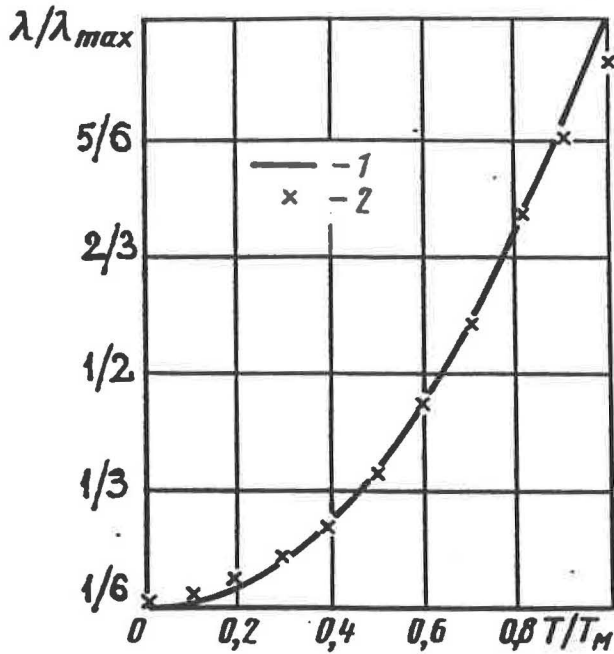


1 - a true solution; 2 - an approximation for disturbed input data by normal law,  $3\sigma = 0.05 \cdot T_{max}^*$  (stopping by criterion of residual,  $N = 7$ ); 3 - an approximation for exact input data,  $N = 50$



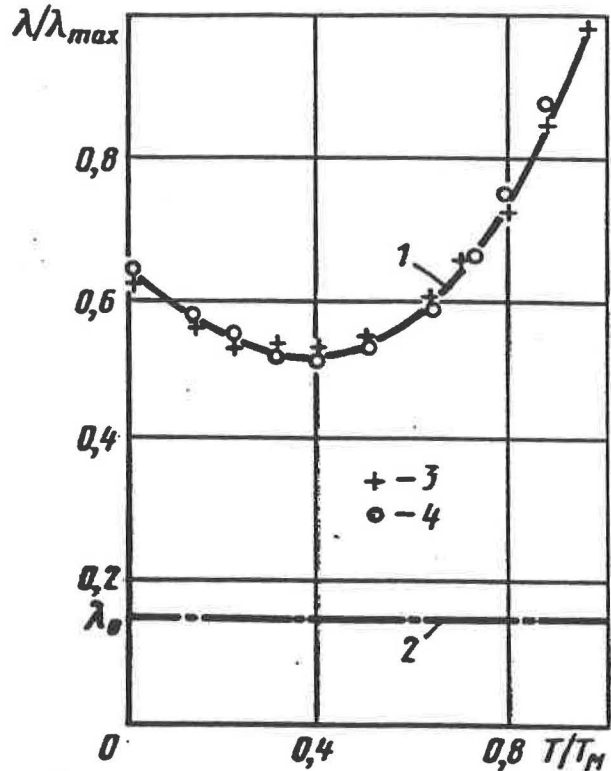
*Cubic  
splines  
and conjugate  
gradient*

II. Nonlinear coefficient IHCP - reconstruction of the thermal conductivity  $\lambda(T)$  with using spline-approximation



Exact input data

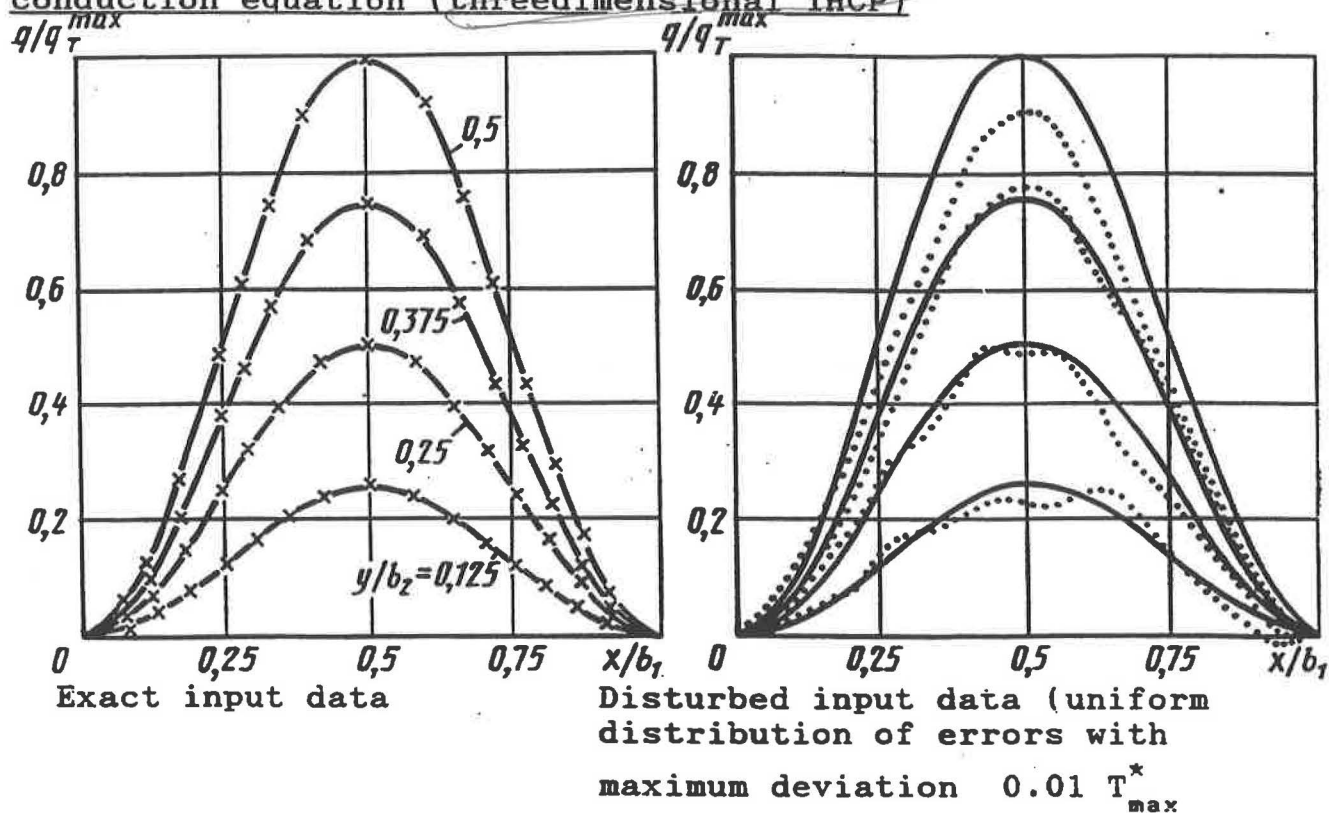
- 1 - the unknown function;
- 2 - the solution of IHCP.



Exact and disturbed input data

- 1-the unknown function; 2-the initial approximation; 3,4-the solution of IHCP for exact and disturbed data respectively.

III. The reconstruction of a source  $Q(x, y, \tau)$  in the heat conduction equation (three-dimensional IHCP)



Results of computation for four cuttings by coordinate  $y$  and one time point  $\tau = \tau_m / 2$  . .

**XIV.**  
**Comparison of Methods for Solving**  
**Boundary IHCPs**

*Just, can be used even for real time*  
*Direct analytical and semi-analytical*

*Most universal*

Table

The conditions of effective application of the methods for the solution of boundary IHCPs

| 1                       | 2                            | 3                           | 4                                   | 5                                | 6                                | 7 |
|-------------------------|------------------------------|-----------------------------|-------------------------------------|----------------------------------|----------------------------------|---|
| Distinctions of methods | Direct analytical method (2) | Direct numerical method (3) | Iterative regularization method (5) | Regularized algebraic method (4) | Regularized numerical method (4) |   |

The peculiarities of a formulation of IHCP

|                                            |                                 |     |     |                                 |     |
|--------------------------------------------|---------------------------------|-----|-----|---------------------------------|-----|
| 1. Linear with constant thermal properties | yes                             | yes | yes | yes                             | yes |
| 2. Nonlinear of linear with variable TP    | no                              | yes | yes | no                              | yes |
| 3. Homogeneous heat-conduction equation    | yes                             | yes | yes | yes                             | yes |
| 4. Generalized heat-conduction equation    | no                              | yes | yes | no                              | yes |
| 5. Fixed boundaries of a body              | yes                             | yes | yes | yes                             | yes |
| 6. Moving boundaries of a body             | in onedimensional case          | yes | yes | in onedimensional case          | yes |
| 7. Fixed temperature gauges                | yes                             | yes | yes | yes                             | yes |
| 8. Travelling temperature gauges           | no                              | yes | yes | no                              | yes |
| 9. Onedimensional                          | yes                             | yes | yes | yes                             | yes |
| 10. Twodimensional                         | for the domains of simple shape | yes | yes | for the domains of simple shape | yes |
| 11. Overspecified                          | no                              | no  | yes | no                              | no  |

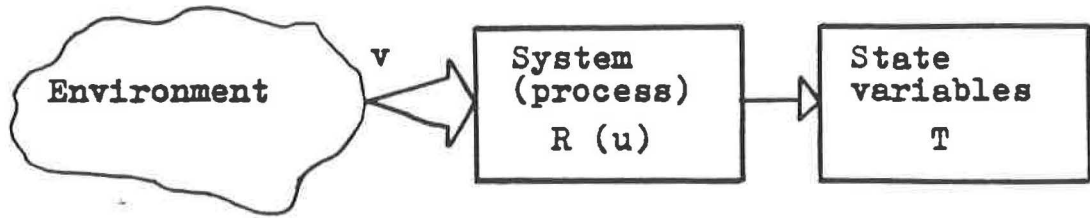
General condi-  
tions of appli-  
cation

|                                                             |     |     |     |     |     |
|-------------------------------------------------------------|-----|-----|-----|-----|-----|
| 12. The determination of heat loads                         | yes | yes | yes | yes | yes |
| 13. The computation of temperature fields                   | no  | yes | yes | no  | yes |
| 14. The slowly alternating heat-exchange processes (HP)     | yes | yes | yes | yes | yes |
| 15. The quickly alternating and short-term HP               | no  | no  | yes | yes | yes |
| 16. Low-temperature HP                                      | yes | yes | yes | yes | yes |
| 17. High-temperature HP with essentially variable intensity | no  | yes | yes | no  | yes |



**XV.**  
**Development and Validation of  
Mathematical Models of Heat  
Transfer**

## Mathematical model

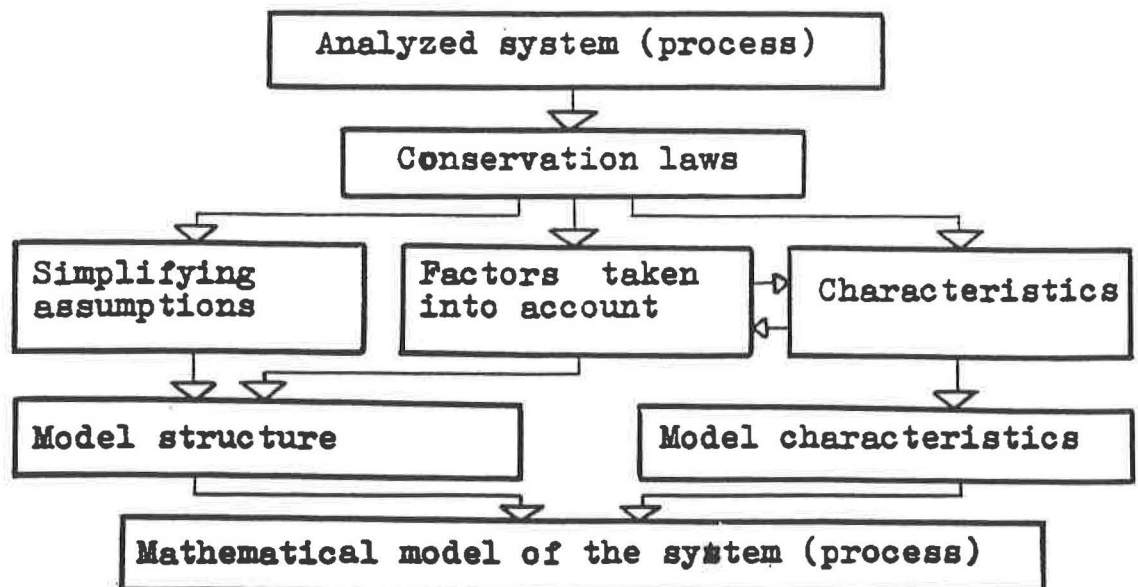


- $v$  - external (input) action;
- $u$  - vector of system characteristics;
- $R(u)$  - operator of the system;
- $T$  - state (output) variable.

Mathematical model - transformation of the external actions into state variables

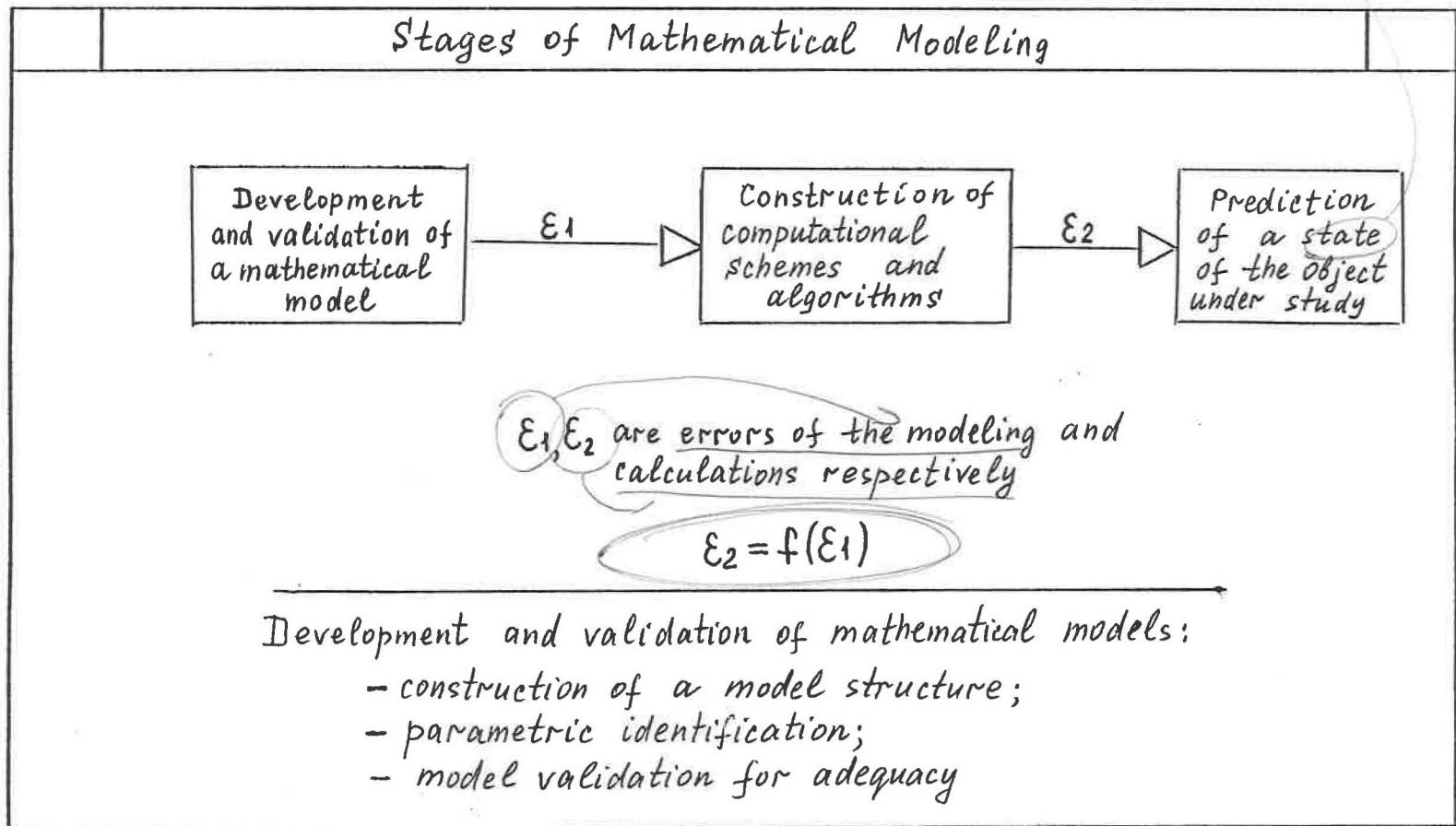
$$R(u) v = T$$

## Mathematical model development

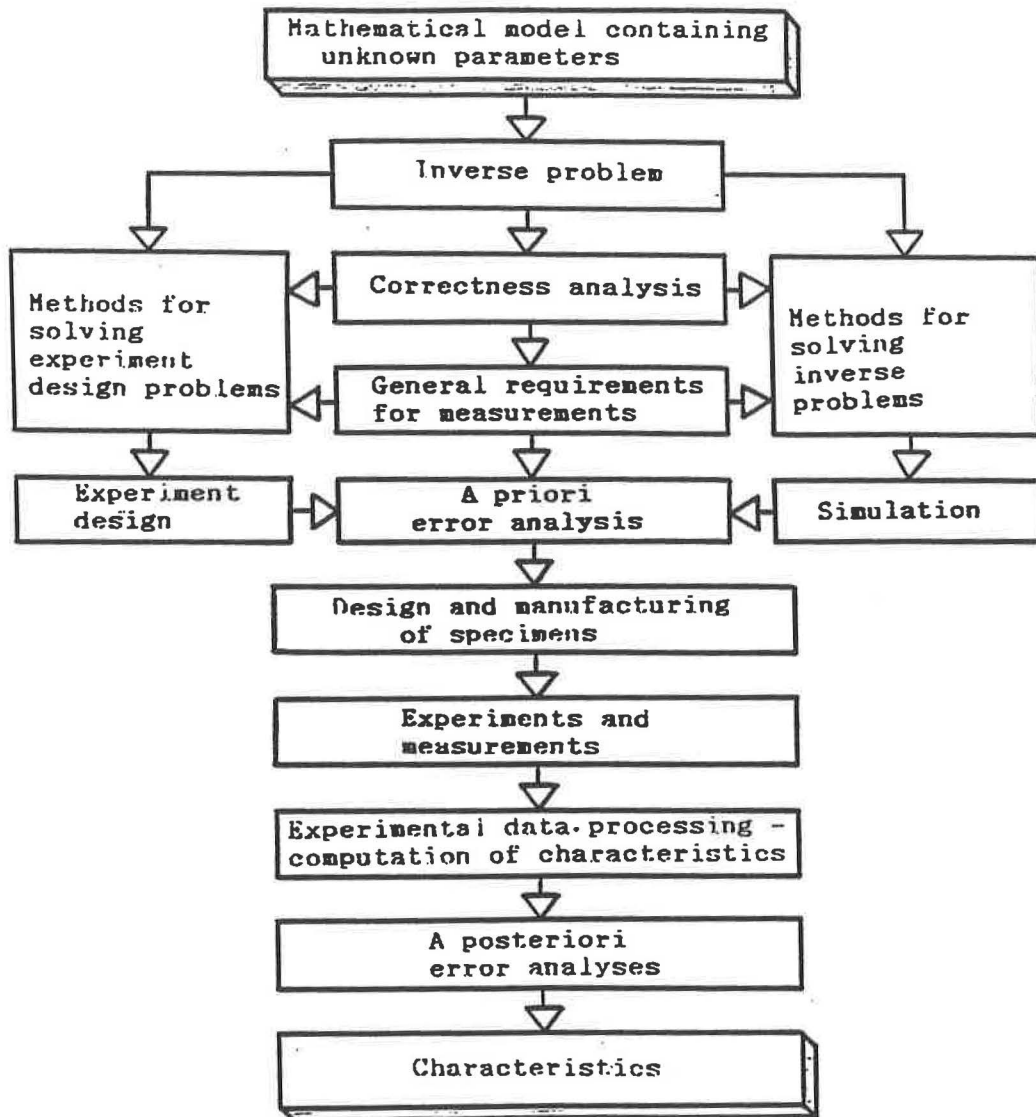




usually  
thermal  
state



Identification of characteristics

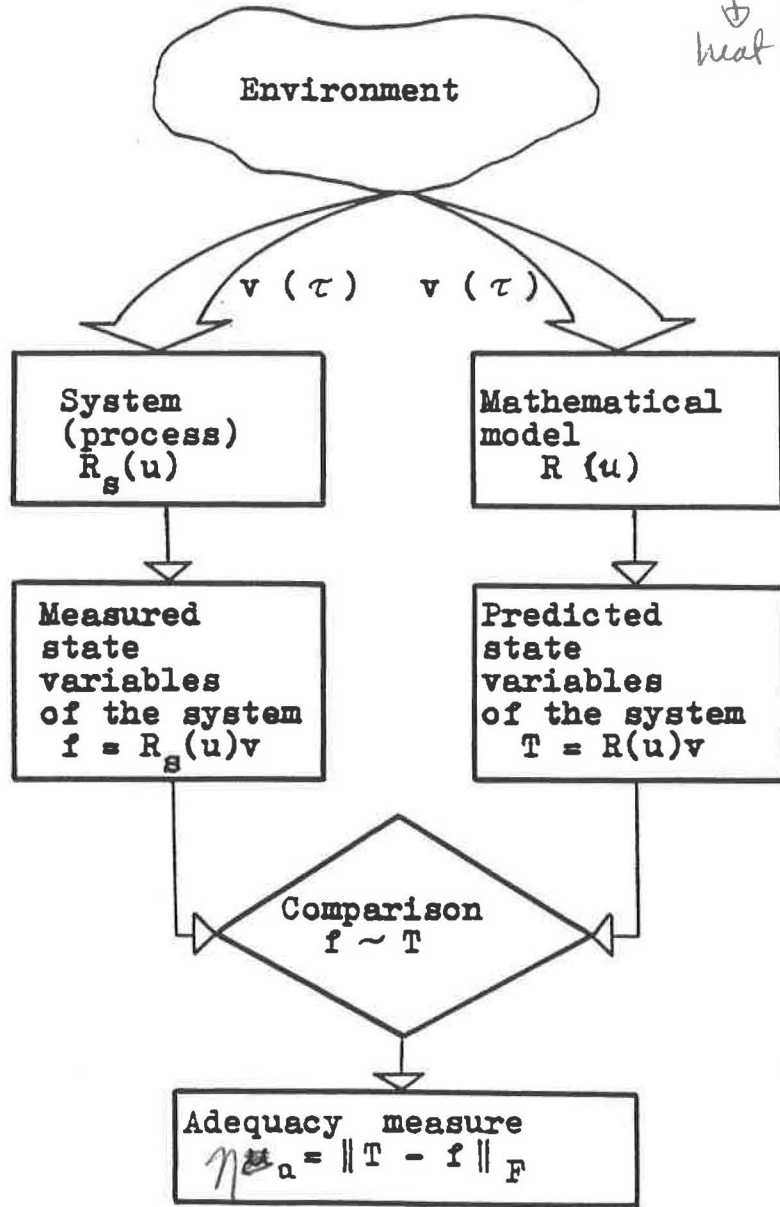


Examination of the model for adequacy

$$\eta(R) = \sup_{v \in V} \inf_{u \in U} \| \underbrace{R(u)}_T v - f \|_F$$

where  $U$  is a solution space;  $V$  is a set of potential loading actions

↓  
heat loads



• The Problem:

$$\eta \leq \epsilon,$$

$\epsilon > 0$  - prescribed level of adequacy

Adequacy measure :  $\eta = \eta(A, f) = \sup_{f \in F_0} \inf_{u \in U} \|Au - f\|_F$

where  $F_0 \subseteq F$  - some set of possible states of the process

For inexact input data :  $\eta_\delta = \eta(A, f_\delta)$

Adequacy criterion :  $\eta_\delta \leq \varepsilon(\eta, \max_{f \in F_0} \delta_f)$

where  $\delta_f = \|f_\delta - f\|_F$  - error of some  $f \in F_0$

Residual  $\Delta = \|z - f_\delta\|_F$ ,  $f_\delta = f_\delta(x, \tau)$ ,  $z = z(x, \tau) = Au$

*model reaction to change in desired quantity u*

I.  $F = L_2$  :

\* if  $f$  is  $n$ -dimensional vector-function :  $\Delta = \left\{ \int_0^{\tau_m} \int_{\Omega} [z - f_\delta]^T [z - f_\delta] d\Omega d\tau \right\}^{1/2}$

\* if  $f$  is scalar field :  $\Delta = \left\{ \int_0^{\tau_m} \int_{\Omega} [z - f_\delta]^2 d\Omega d\tau \right\}^{1/2}$

\* if  $f = f(\tau)$ ,  $z = z(\tau)$  :  $\Delta = \left\{ \int_0^{\tau_m} (z - f_\delta)^T W (z - f_\delta) d\tau \right\}^{1/2}$ ,  $W$  is weight matrix

II.  $F = C$  :  $\Delta = \max_{x, \tau} |z - f_\delta|$

Reasons of nonadequacy of the model and ways of their elimination

Nonadequacy of the model

Characteristics are known with low accuracy

Structure of the model does not take into account the influencing factors

Characteristics specification

Structure specification

Correctness analysis of inverse problems

Correctness analysis

Solution existence

Solution uniqueness

Solution stability

Requirements for measurements

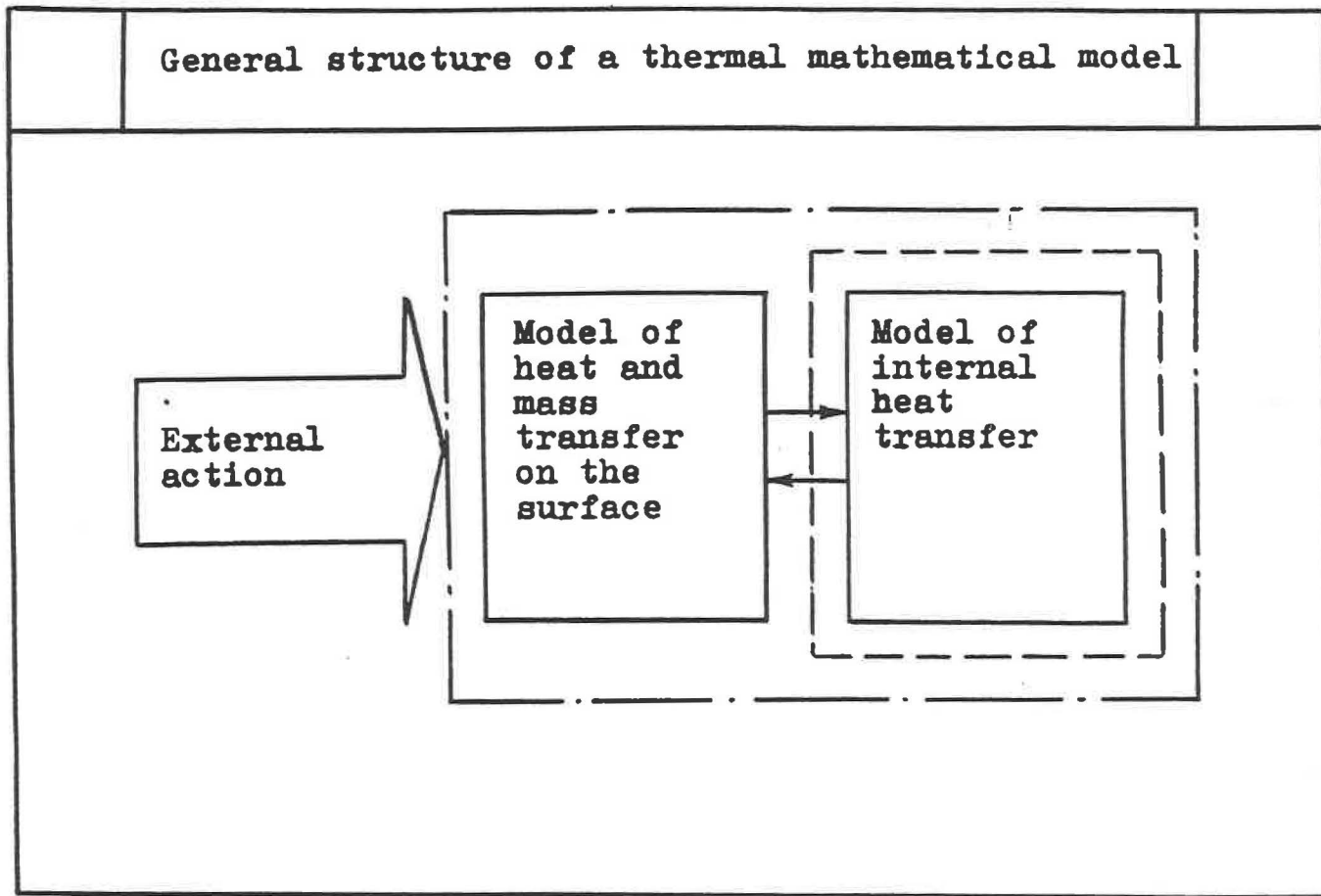
Requirements for methods of solution

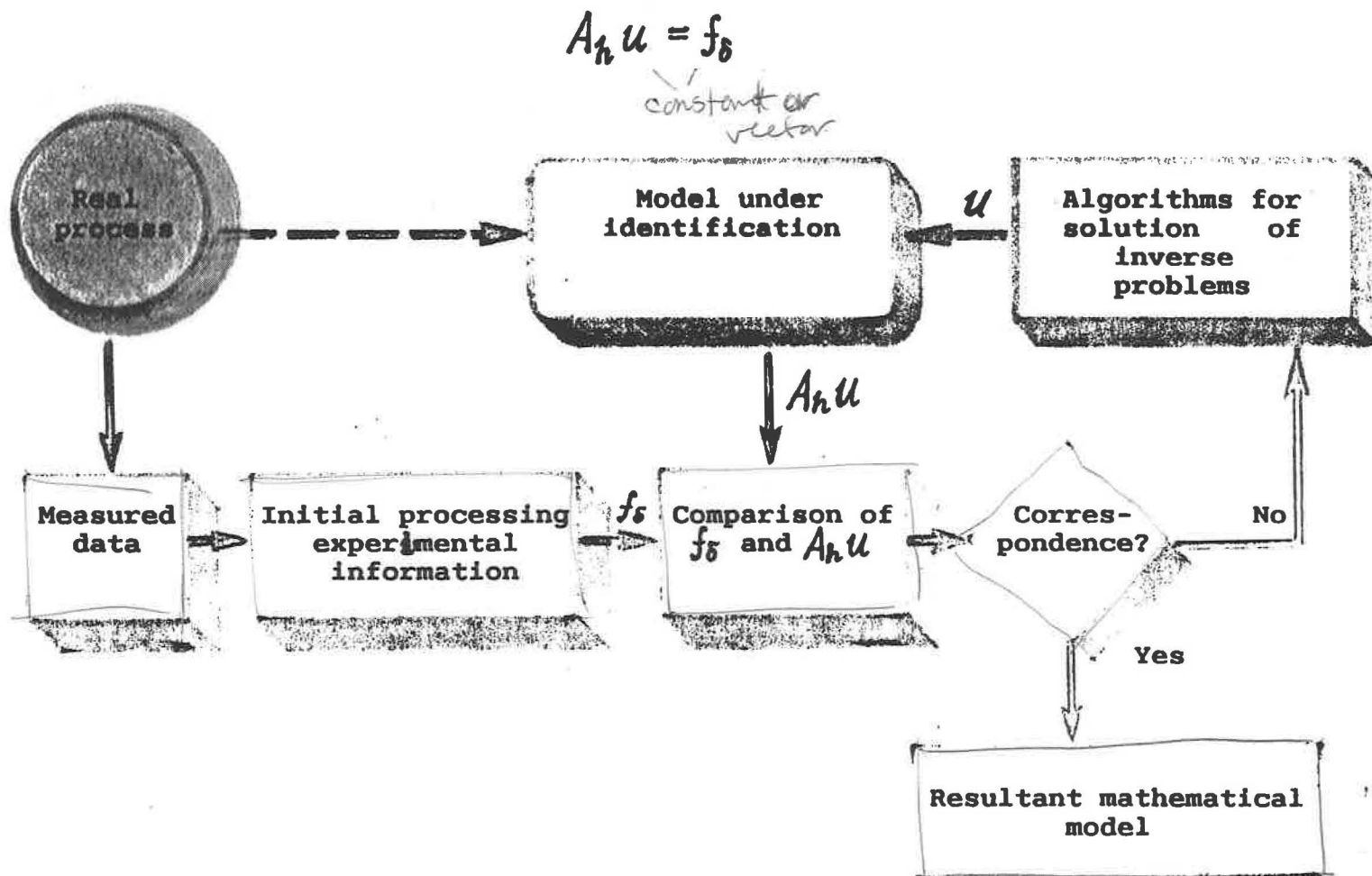
General structure of a thermal mathematical model

External  
action

Model of  
heat and  
mass  
transfer  
on the  
surface

Model of  
internal  
heat  
transfer



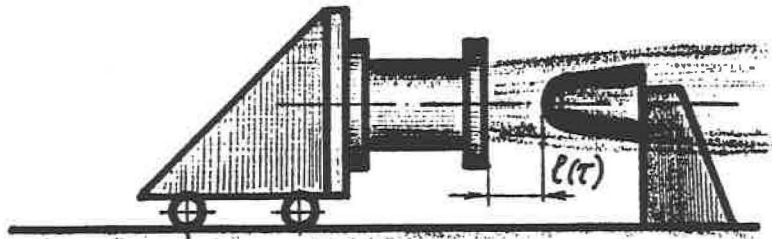


**XVI.**  
**Application Results**

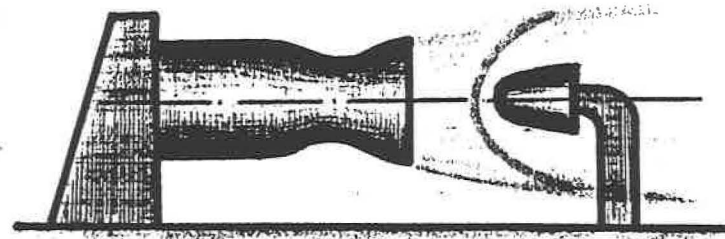


AR1: **Non-Stationary Heat Measuring**

High - Temperature Gas Jets

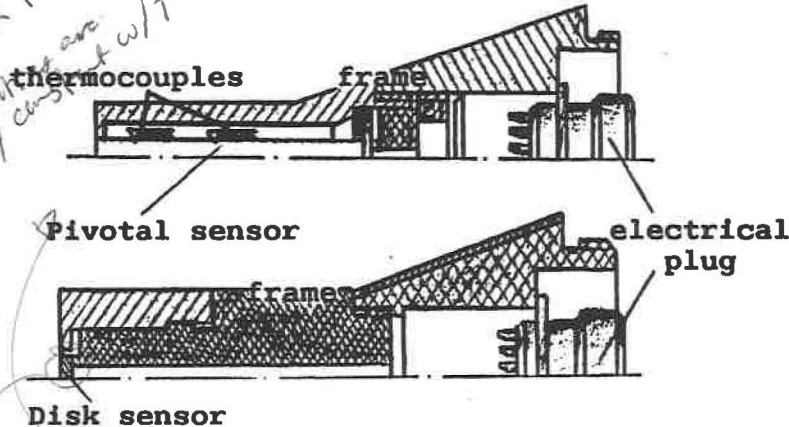


Plasma jets



Jets of rocket engines

Transient Calorimeters



Disk sensor

Pivotal sensor

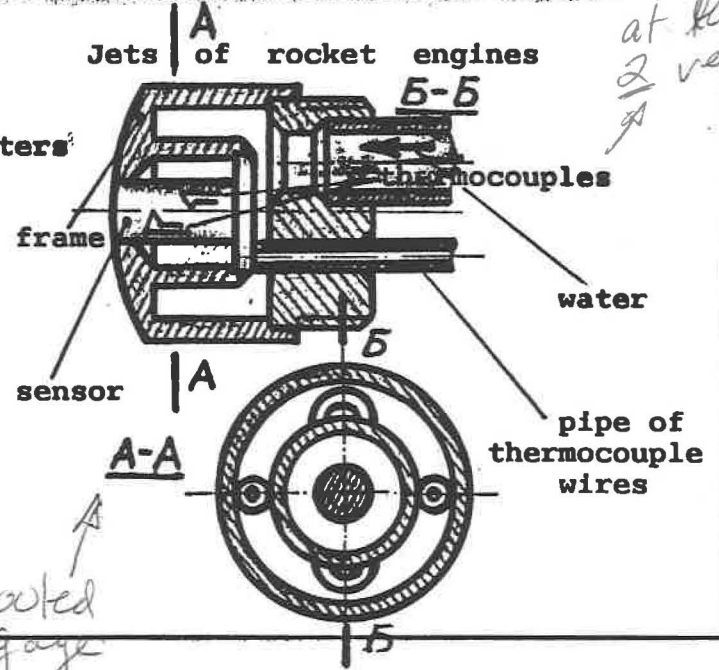
thermocouples

frame

electrical plug

frames

uncooled gages



at least 2 required

coated gage

Cu  
Ni  
Vanadium  
high conductivity  
can operate to high T  
thermocouples are  
different usually constant w/T

3mm

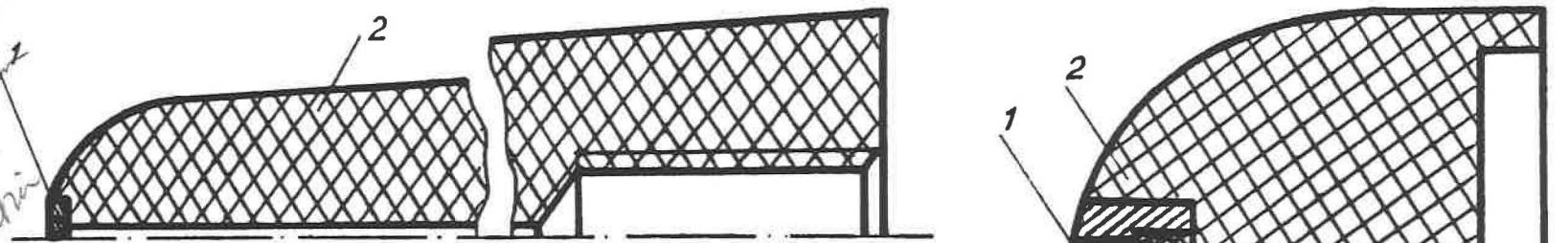
Accuracy of inverse method decreases with increasing distance of first sensor from active surface

TP  
1

AR1 (continuation)

3/2

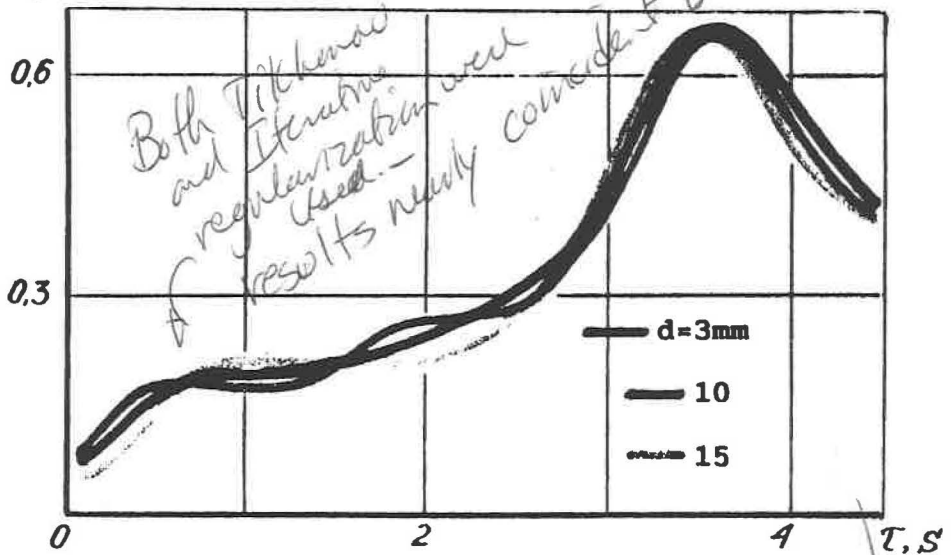
redundant  
Temperatures  
more time than  
needed for  
q estimation



Noncooled calorimeters for engine jets

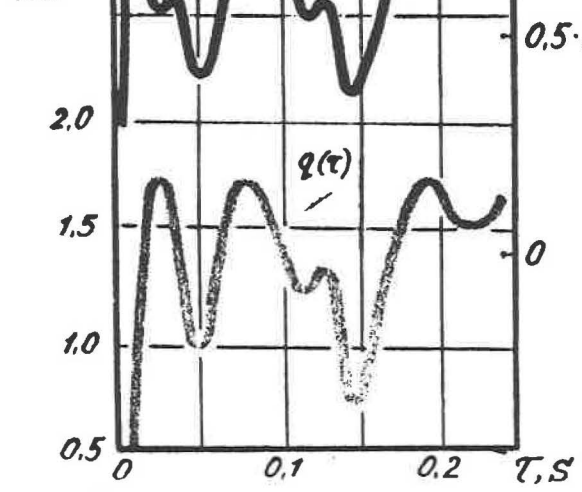
(1 - sensor, 2 - frame, 3, 4 - plugs)

$q \cdot 10^{-4}, \text{ kW/m}^2$



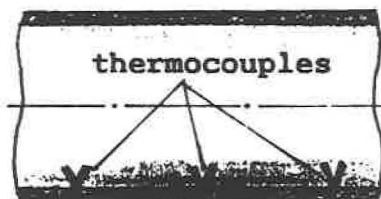
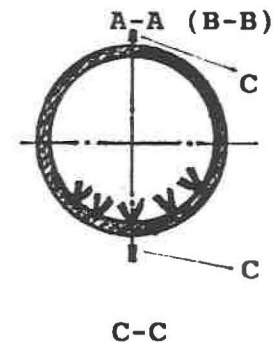
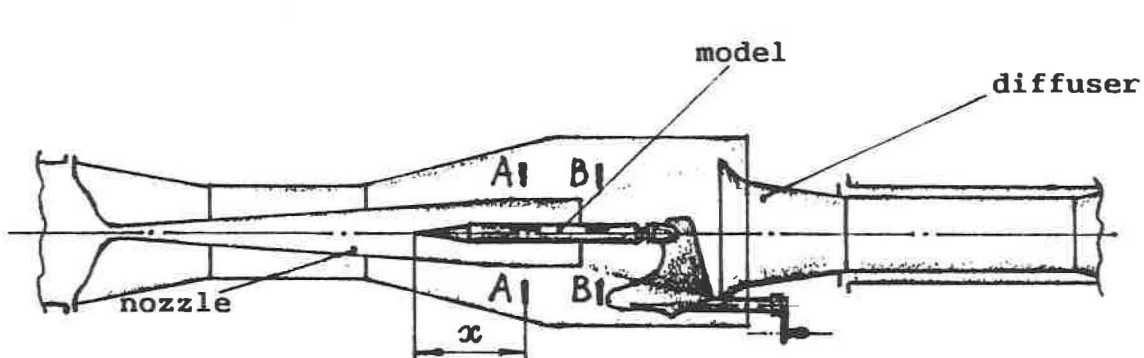
Results of determining of heat flux by pivotal calorimeter, moving along subsonic plasma jet

$q, \text{ kW/Sm}^2$  and  $P, \text{ N/m}^2$



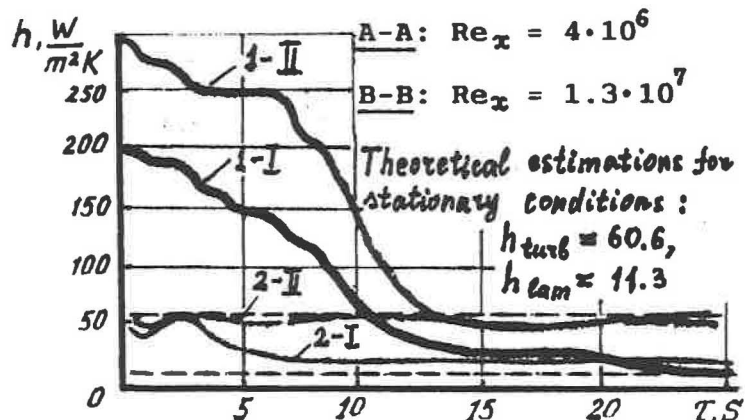
Heat fluxes in nitrogen plasma jet

T data from longer than 45 were used -



Supersonic thermal wind tunnel

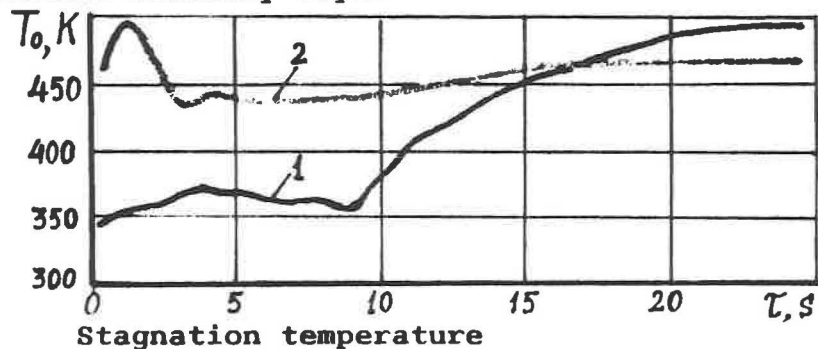
Testing conditions:  $T_{\infty} = 150 \dots 500 \text{ } ^\circ\text{C}$ ;  $p_0 = 8 \cdot 10^5 \text{ Pa}$ ;  $M = 5.0$



Heat transfer coefficients

( 1,2 - numbers of tests; I -  $x = 0.3 \text{ m}$  ; II -  $x = 1.0 \text{ m}$  )


- laminar boundary layer
- turbulent boundary layer

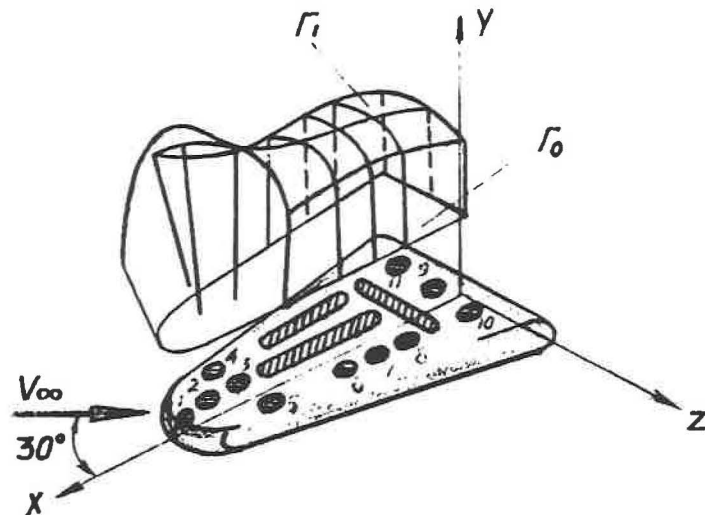


TP  
1

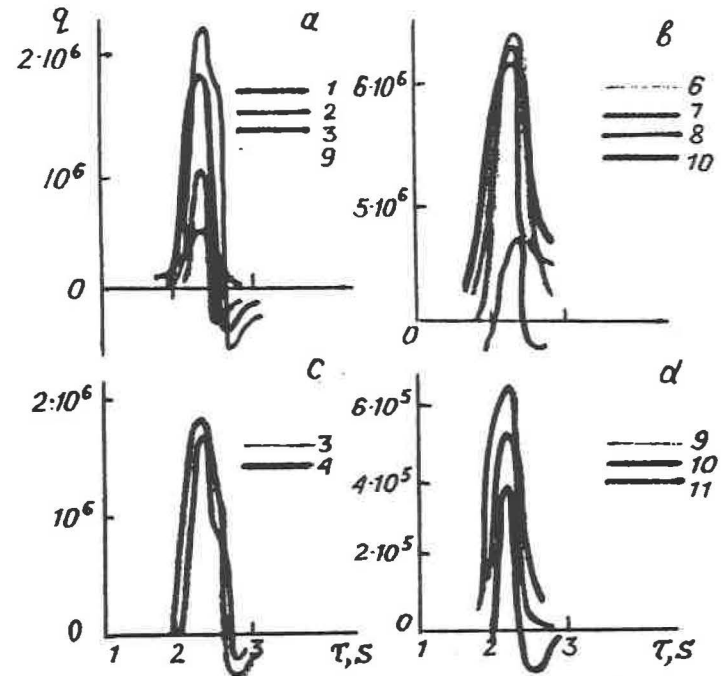
AR3: Heat Transfer Diagnostics on Models Surface during testing at hypersonic wind tunnel with magnetogasdynamic accelerating air stream

3/4

 - one-dimensional sensors  
 - two-dimensional sensors



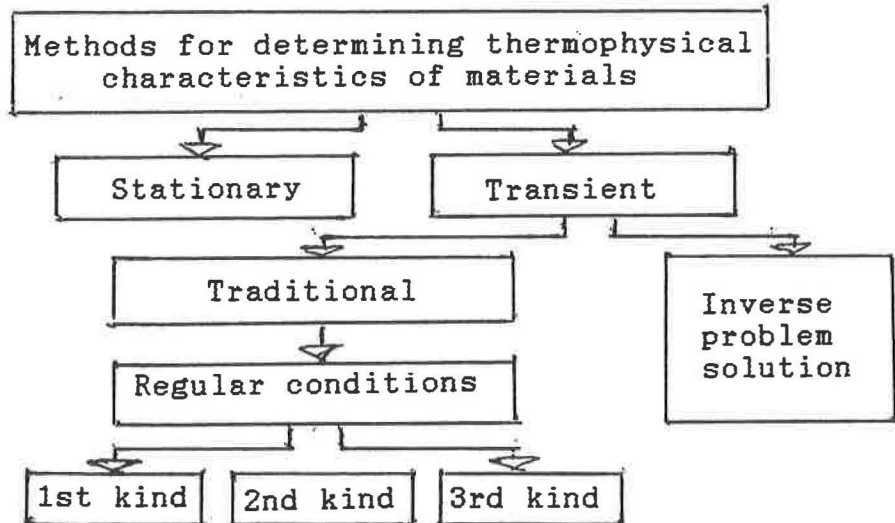
Arrangement of sensors and spacial heat flux distribution on the windward model surface:  $\Gamma_0$ , original base surface;  $\Gamma_1$ , flux distribution surface for the time moment  $\tau = 2.3$  s,  $M = 20 \dots 25$ ,  $Re \approx 10^5$ ,  $\tau_{\text{impulse}} \approx 1$  s



Reconstructed values of heat flux  $q(\tau)$ ,  $W/m^2$  at diagnostics points in different model cross-sections:

- a, at points 1, 2, 3, 9;
- b, at points 6, 7, 8, 10;
- c, at points 3, 4;
- d, at points 9, 10, 11.

## Methods for characteristics determination



### Traditional methods of characteristics

- Traditional methods are based on analytical solutions of the boundary-value problem for the heat conduction equation with constant coefficients.
- Heating conditions for samples used are rather simple and easy to reproduce.
- Rather narrow temperature range is realized in samples to provide constancy of characteristics.

Mathematical Model №1  
(fixed thermosensors and body boundaries)

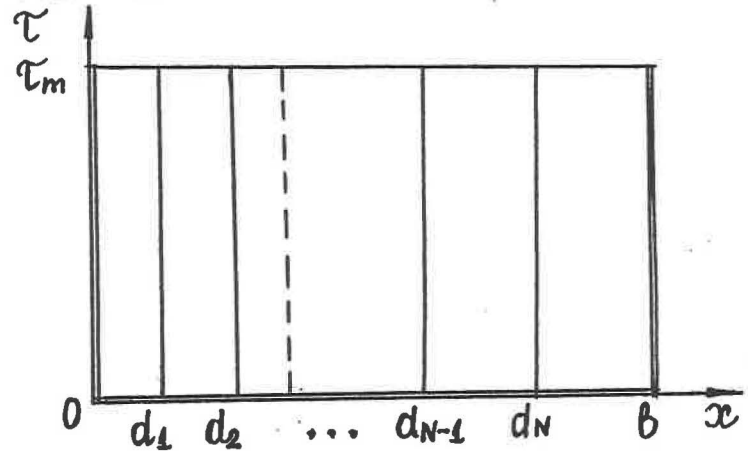
$$C(T)T_\tau = (\lambda(T)T_x)_x, \quad (x, \tau) \in Q = (0, b) \times (0, \tau_m);$$

$$T(x, 0) = \xi(x), \quad x \in [0, b];$$

$$T(0, \tau) = T_1(\tau); \quad T(b, \tau) = T_2(\tau), \quad \tau \in [0, \tau_m];$$

$$T(d_i, \tau) = f_i(\tau), \quad i = \overline{1, N}, \quad \tau \in [0, \tau_m];$$

$$C(T) > 0, \quad \lambda(T) > 0$$



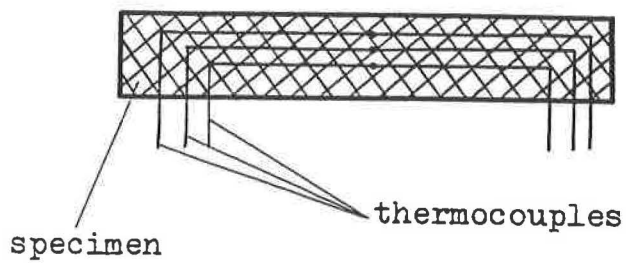
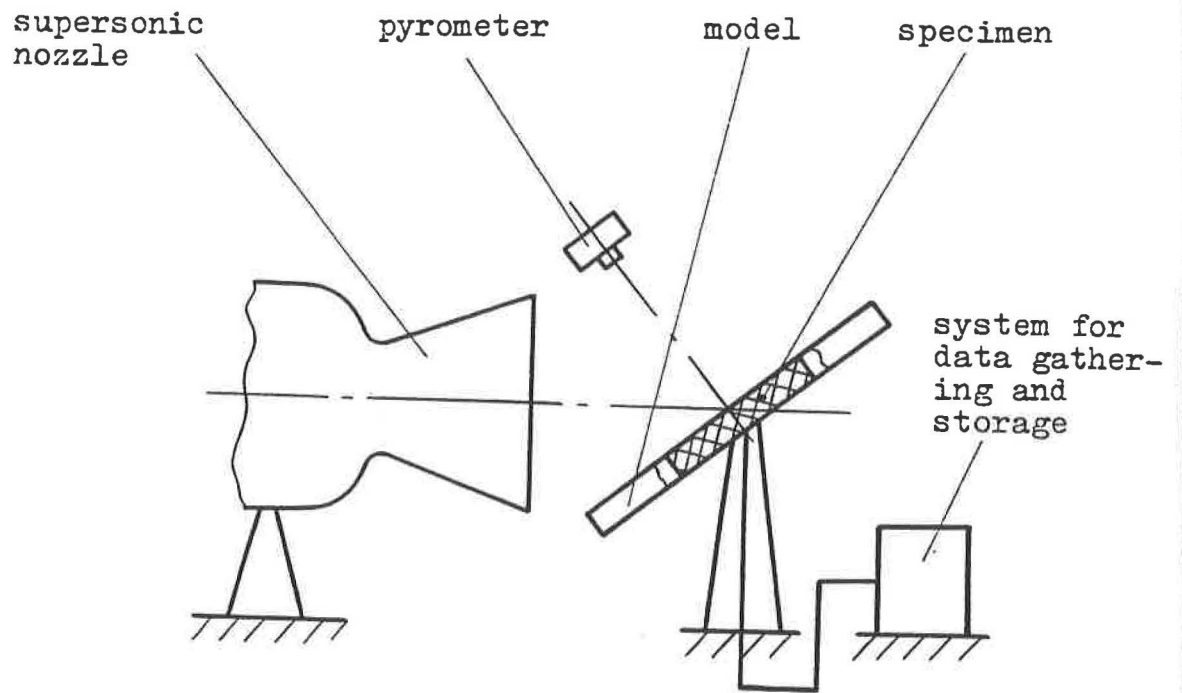
$$0 < d_1 < \dots < d_N < b$$

$$\lambda(T): \min_{\lambda(T)} |J(\lambda) - \delta_J^2|,$$

$$J(\lambda) = \sum_{i=1}^N \int_0^{\tau_m} \beta_i(\tau) [T(\lambda, d_i, \tau) - f_i(\tau)]^2 d\tau;$$

$\delta_J^2$  is a minimal allowable level for residual

Diagram of test facilities



Results of temperature measurements

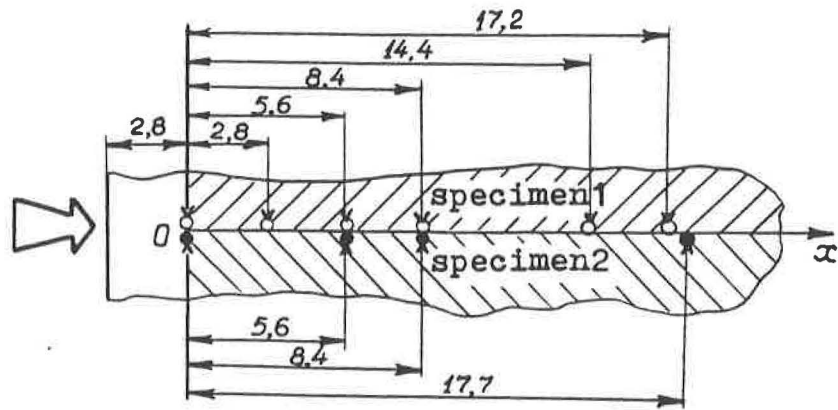
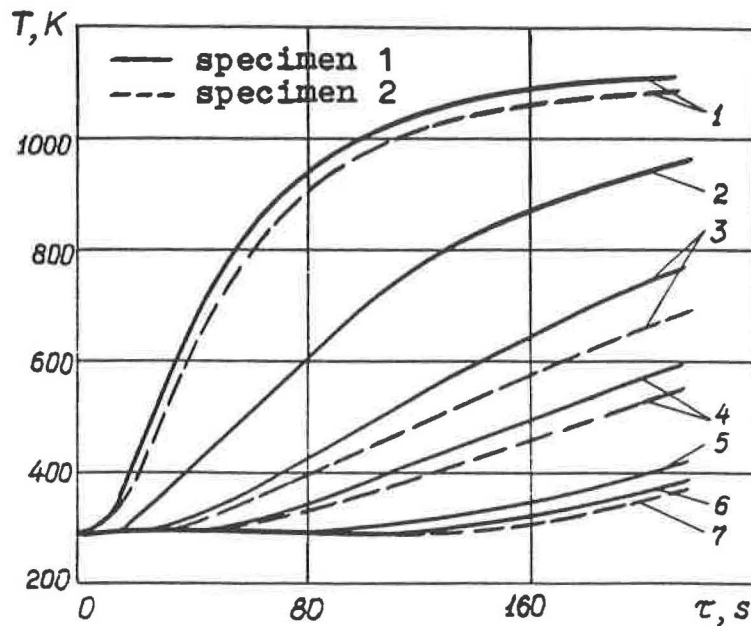


Diagram of thermocouples location.

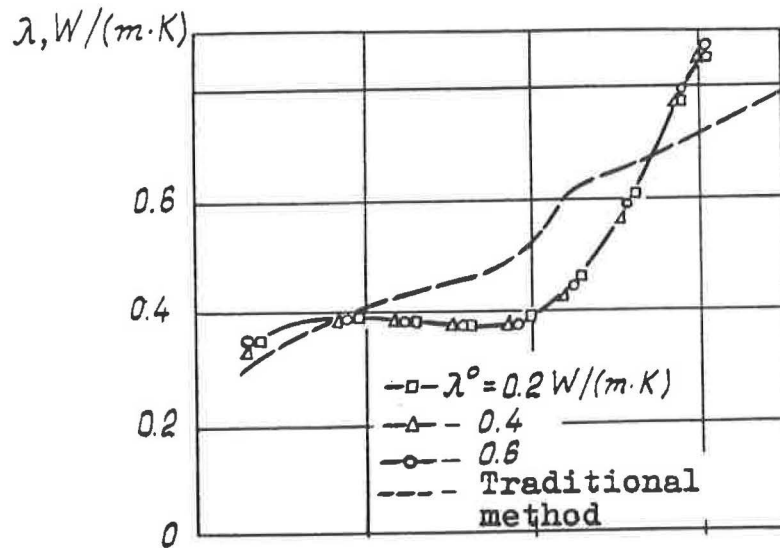


Measured temperatures:

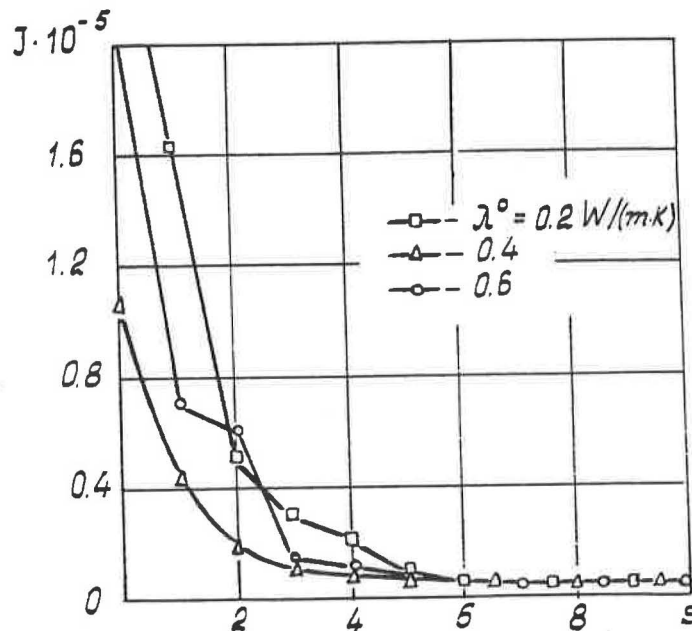
- 1 -  $X=0$ ; 2 -  $X=2.8$  mm; 3 -  $X=5.6$  mm; 4 -  $X=8.4$  mm;  
 5 -  $X=14.4$  mm; 6 -  $X=17.2$  mm; 7 -  $X=17.7$  mm.



Results of experimental data processing,  
specimen 1

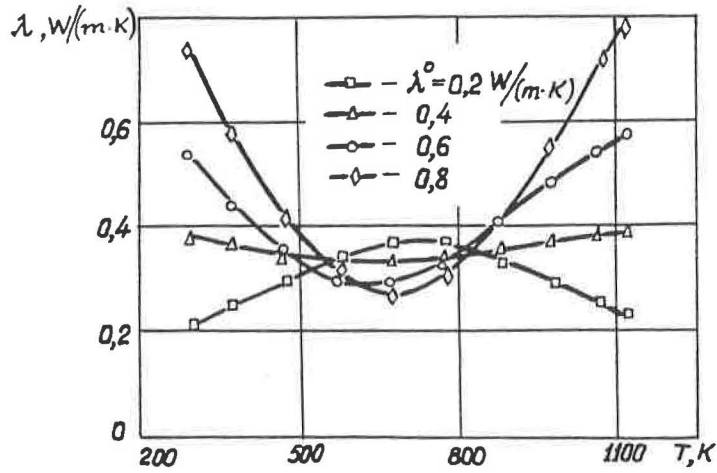


Thermal conductivity  $\lambda(T)$  determination by solving the inverse problem with different values of initial approximation  $\lambda^0$ .

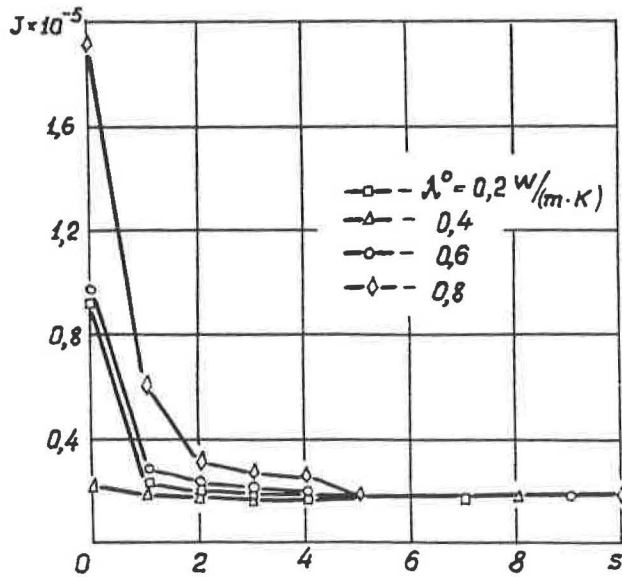


Changing residual functional  $J$  depending on iteration number  $s$ .

Results of experimental data processing,  
specimen 2



Thermal conductivity  $\lambda(T)$  determination by solving the inverse problem with different values of initial approximation  $\lambda^0$ .



Changing residual functional  $J$  depending on iteration number  $s$ .

# Optimal Measurement Design

Measurement design  $\epsilon = \{N, \mathbf{d}\}$ ,  
where  $N$  is the number of thermosensors

$\mathbf{d}$  is the vector of sensor coordinates ( $\mathbf{d} = \{d_i\}_1^N$ )

Problem:  $\epsilon = \epsilon^* : \max_{\epsilon} \Psi[F(\epsilon)]$ ,

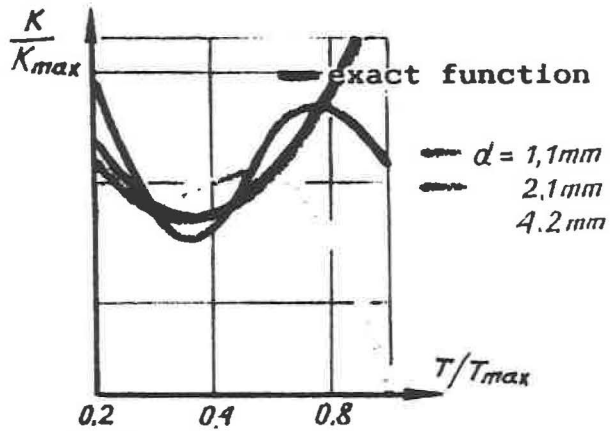
where  $F(\epsilon) = \frac{1}{N} \Phi_{jn}$ ,  $j, n = \overline{1, M}$ ;

$M + 3$  - the number of intervals for  $\lambda(T)$   
approximation by B-splines

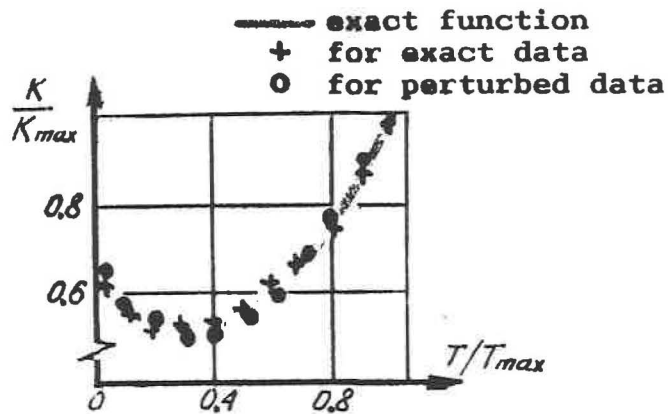
$$\Phi_{jn} = \sum_{i=1}^N \int_0^{\tau_m} \theta_j(d_i, \tau) \theta_n(d_i, \tau) d\tau;$$

$\theta_j(d_i, \tau)$  are the sensitivity functions,

$$\theta_j(d_i, \tau) = \frac{\partial T(d_i, \tau)}{\partial \lambda_j}, \quad j = \overline{-1, M+1}$$



K(T) reconstruction using exact input data for different values at the thermocouple coordinate



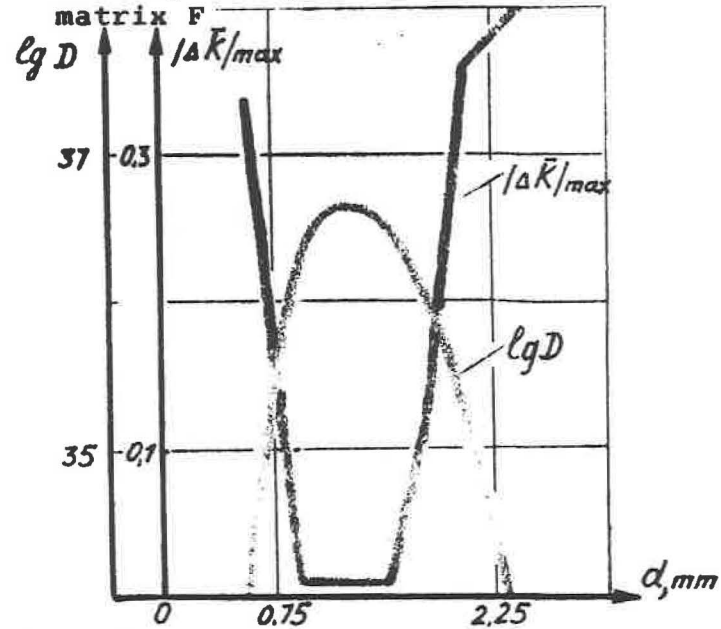
K(T) reconstruction for D-optimal design

The experiment design is a determination of a number of temperature gauges  $N$ , coordinates, of their installation into a body  $\vec{d} = \{d_i\}_1^N$

D - optimal design:  $\vec{\xi} = \vec{\xi}^* = \{N, \vec{d}\}^* : \max_{\vec{\xi}} D[F(\vec{\xi})],$

where

$D[F(\vec{\xi})]$  is a determinant of the corresponding Fisher information matrix  $F$



Dependences of criterion value and relative error maximum from  $d$

Mathematical Model №2  
(movable thermosensors and body boundaries)

$$C(T)T_\tau = (\lambda(T)T_x)_x, \quad (x, \tau) \in Q_\tau,$$

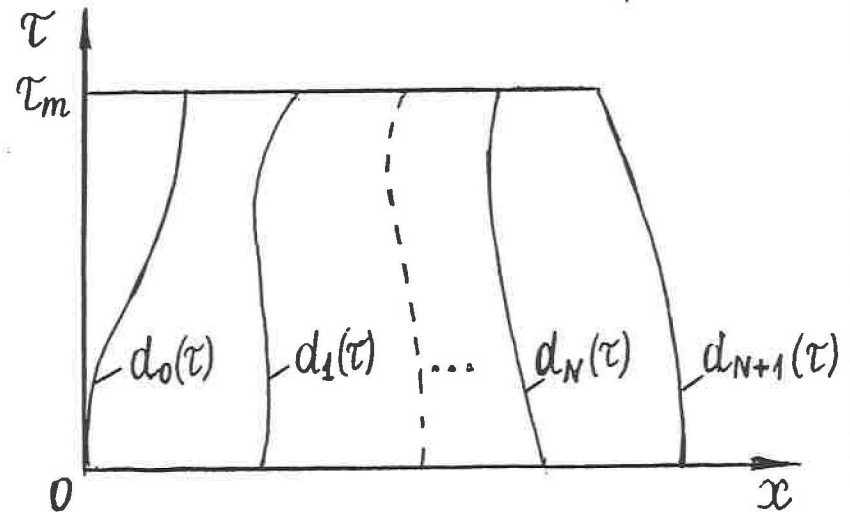
$$Q_\tau = \{d_0(\tau) < x < d_{N+1}(\tau), \quad 0 < \tau \leq \tau_m\};$$

$$T(x, 0) = \xi(x), \quad d_0(0) \leq x \leq d_{N+1}(0);$$

$$T(d_0(\tau), \tau) = T_0(\tau); \quad T(d_{N+1}(\tau), \tau) = T_{N+1}(\tau), \\ \tau \in [0, \tau_m];$$

$$T(d_i(\tau), \tau) = f_i(\tau), \quad i = \overline{1, N}, \quad \tau \in [0, \tau_m];$$

$$C(T) > 0, \quad \lambda(T) > 0$$

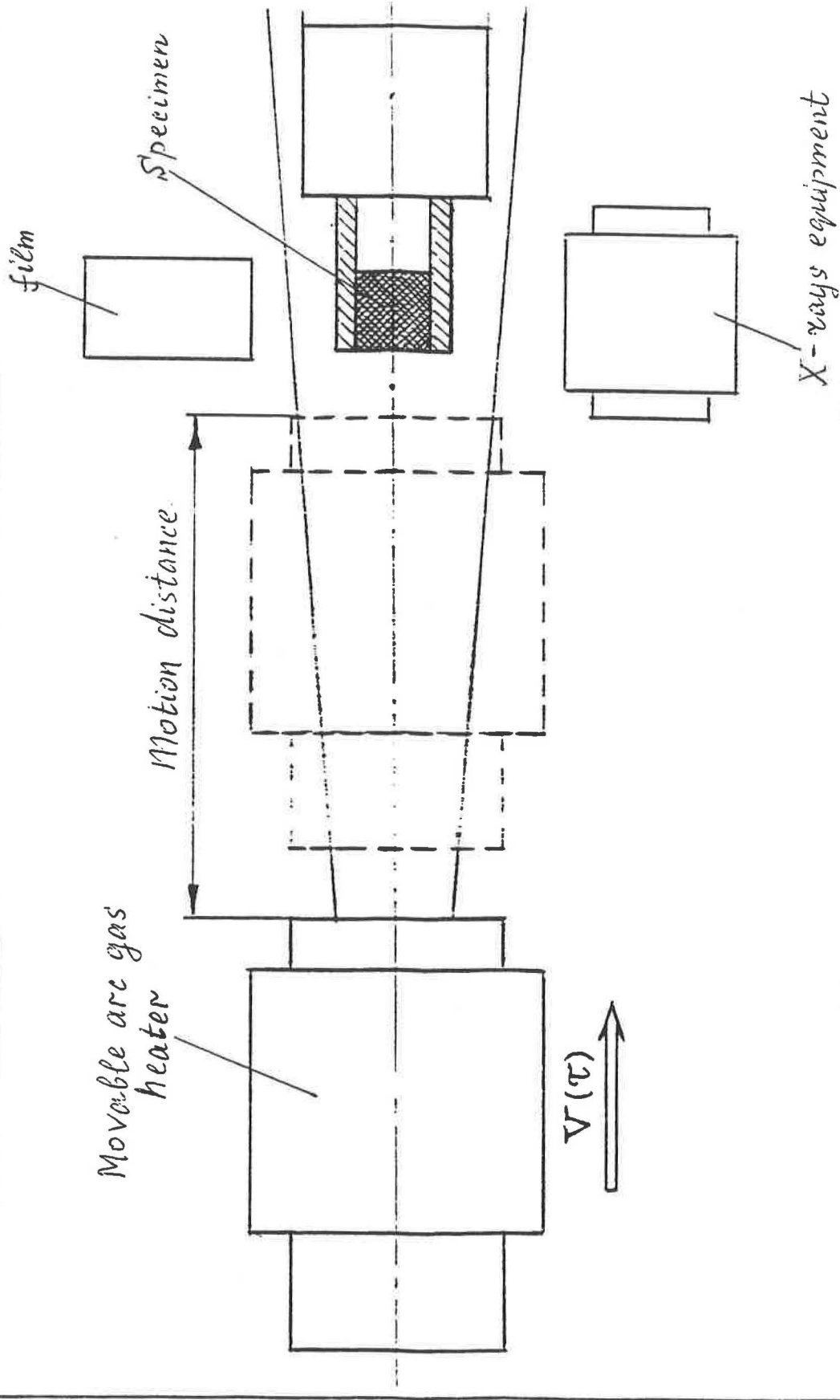


$$d_0(\tau) < d_1(\tau) < \dots < d_N(\tau) < d_{N+1}(\tau)$$

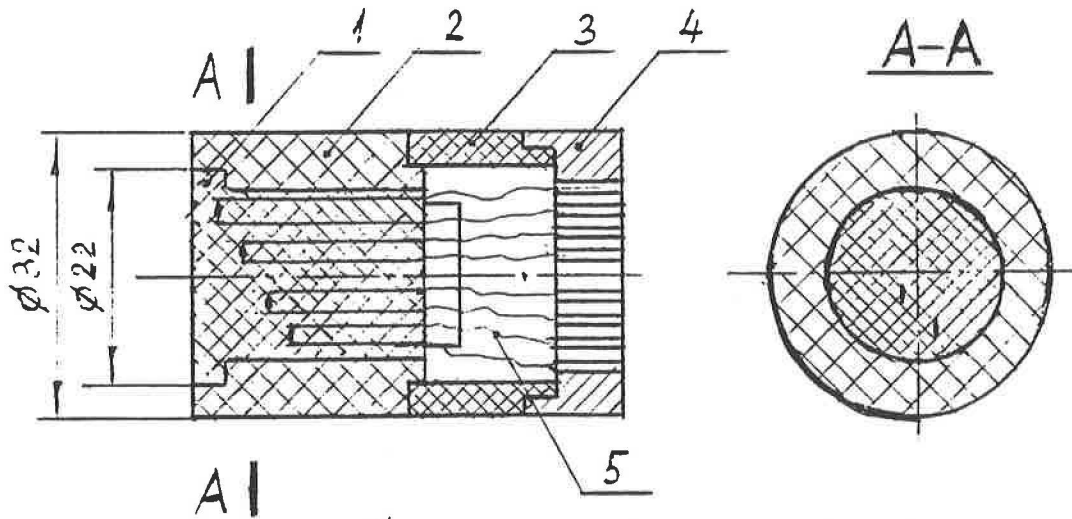
$$\lambda(T) : \min_{\lambda(T)} |J(\lambda) - \delta_T^2|,$$

$$J(\lambda) = \sum_{i=1}^N \int_0^{\tau_m} \rho_i(\tau) [T(\lambda, d_i(\tau), \tau) - f_i(\tau)]^2 d\tau$$

Experimental Facility

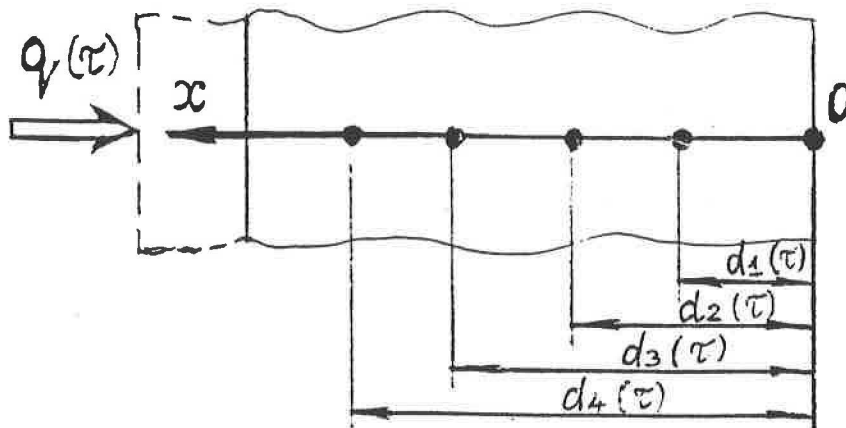


# Thermal Properties Investigations of a decomposing material with moving thermocouples



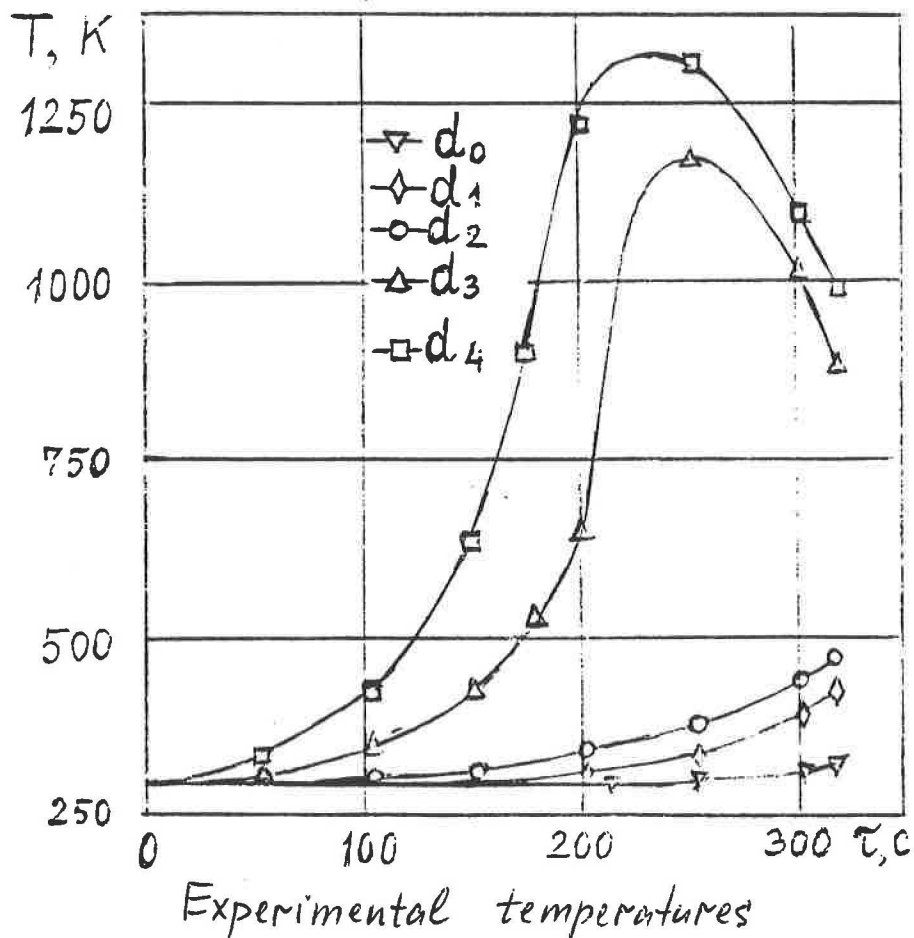
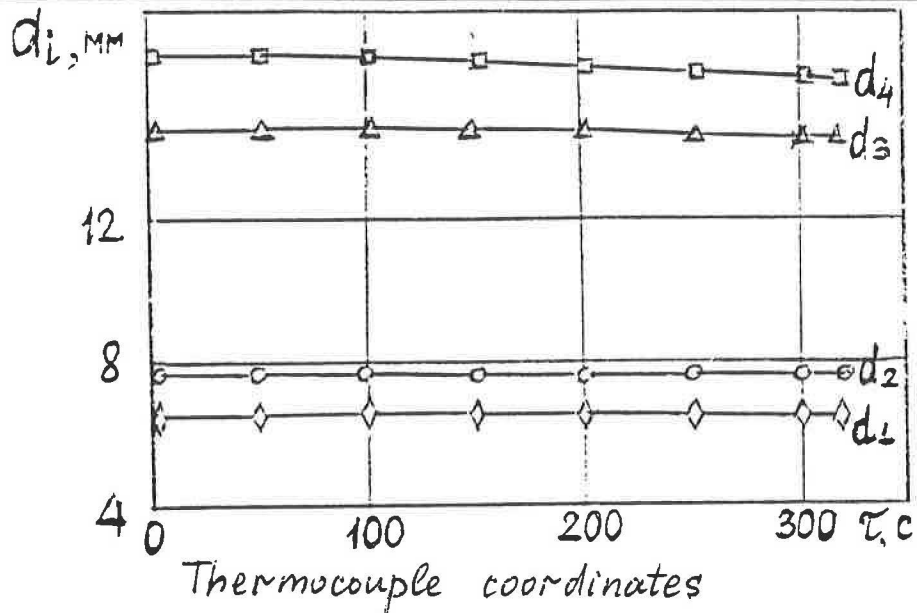
Specimen under investigation

- 1 - sensing element ; 2,3,4 - frame ;
- 5 - chromel - alumel thermocouples



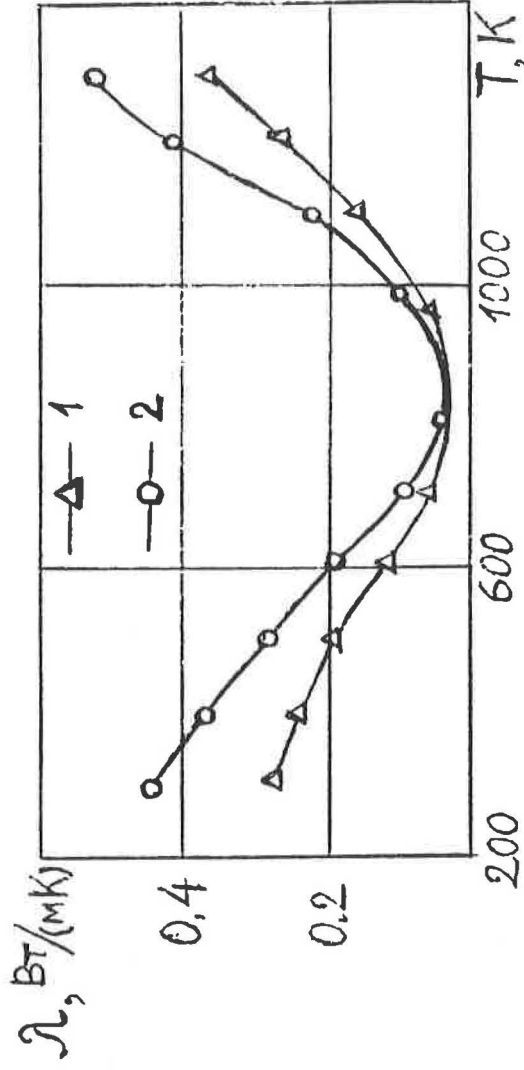
Arrangement of thermocouples in the sensing element

## Measurement Results





# Composite thermal protection material KVT



Estimation results of thermal conductivity

1 - taking into consideration of the thermocouples displacements;

2 - assuming that thermocouples were fixed

TP  
1

AR4: Study of thermal properties of heat protective materials.  
Mathematical model of heat and mass transfer in decomposing materials

3/5

$$c(T) \frac{\partial T}{\partial \tau} = \frac{\partial}{\partial x} \left( \lambda(T) \frac{\partial T}{\partial x} \right) - P \left( T, \frac{\partial T}{\partial \tau} \right) \frac{\partial T}{\partial x} - S \left( T, \frac{\partial T}{\partial \tau} \right), \quad x \in (0, b), \tau \in (0, \tau_m];$$

$$T(x, 0) = T_0, \quad x \in [0, b]; \quad T(0, \tau) = f_0(\tau), \quad T(b, \tau) = f_N(\tau), \quad \tau \in [0, \tau_m];$$

$$P \left( T, \frac{\partial T}{\partial \tau} \right) = \frac{dh_g(T)}{dT} \int_0^b \frac{\partial m_g}{\partial x} dx; \quad S \left( T, \frac{\partial T}{\partial \tau} \right) = h_g(T) \frac{\partial m_g}{\partial x},$$

$$\frac{\partial m_g}{\partial x} = \begin{cases} (1 - K_T) \rho_0 \left( A + \Delta A \frac{\partial T}{\partial \tau} \right) z^n \exp(-E/RT), & T > T_z \\ 0, & T \leq T_z \end{cases}$$

$$T_z = T_{z_0} + a_1 \left( \frac{\partial T}{\partial \tau} \right)^{a_2}, \quad z = (\rho - \rho_0) (\rho_0 - \rho_c),$$

where  $m_g, h_g$  are specific mass flow rate and enthalpy of gaseous products;

$K_T = \rho_c / \rho_0$  is a limiting value of the coke number;

$\rho_0, \rho, \rho_c$  are initial, current and finite values of the material density;

$z$  is a concentration of a decomposing component;

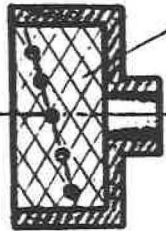
$a_1, a_2, A, \Delta A, n, E$  are thermdestructive parameters;

$R$  is a universal gas constant;

$T_{z_0}$  is a temperature of the start of physico-chemical conversions in the material

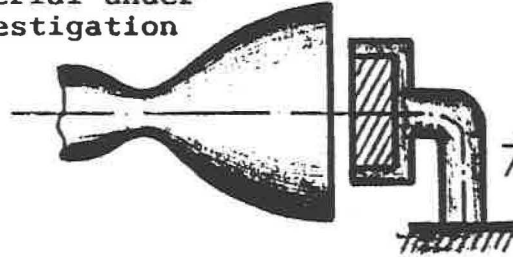
Input data:  $T(d_i, \tau) = f_i(\tau)$ ,  $i = \overline{1, N-1}$ ,  $N \geq 2$ ,  $0 < d_1 < d_2 < \dots < d_{N-1} < b$

$K(T)$  - is an unknown function

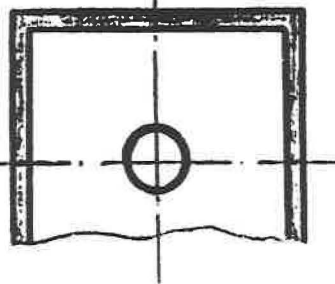
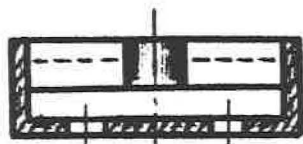


material under investigation

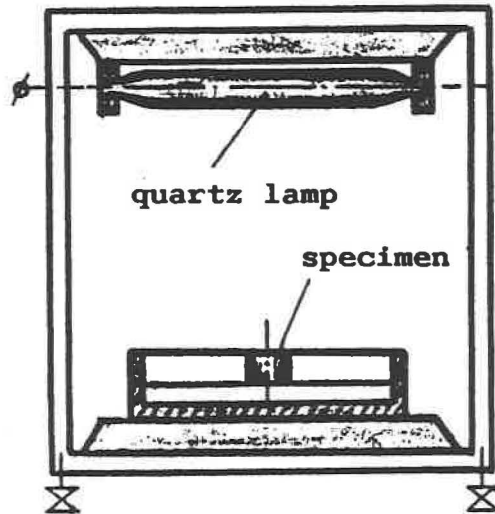
Specimen I



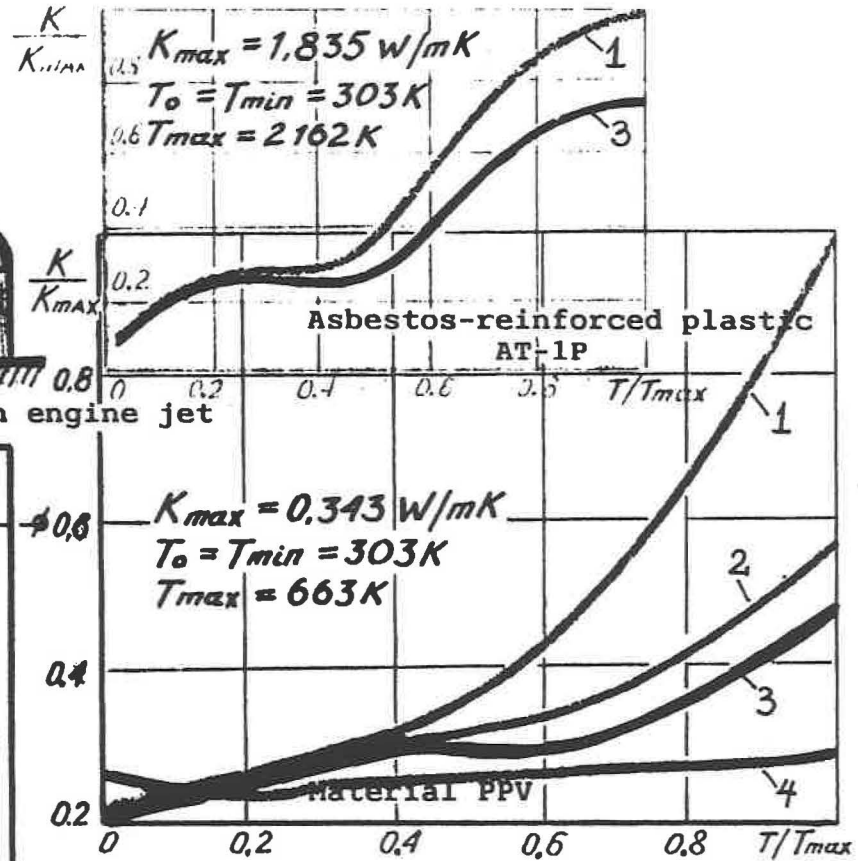
Testing in engine jet



Specimen II



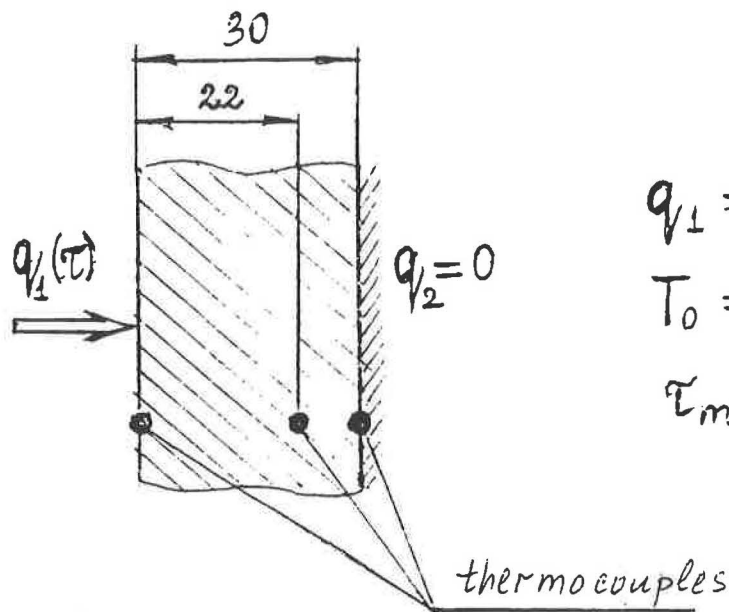
Testing in thermal-vacuum chamber



Processing of experimental data:

- 1 - above-stated model
- 2 - above-stated model at  $\Delta A = 0$
- 3 - uniform heat conduction problem ( $P=S=0$ )
- 4 - monotonic heating method

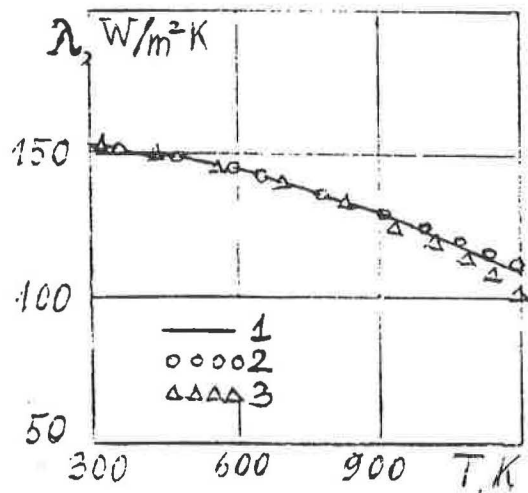
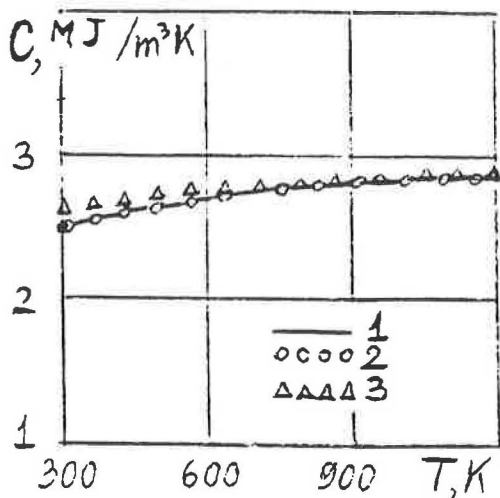
# Simultaneous determination of two thermal properties



$$q_1 = 190 \tau \text{ kW/m}^2,$$

$$T_0 = 300 \text{ K},$$

$$\tau_m = 20 \text{ s}$$



Estimations of volumetric heat capacity  $C(T)$  and thermal conductivity  $\lambda(T)$ :  
 1 - exact solutions; 2 - calculations for exact input data;  
 3 - calculations for perturbed input data,  $3\sigma = 0.05 T_{max}$

TP  
1

AR: Facility Tests

3/8

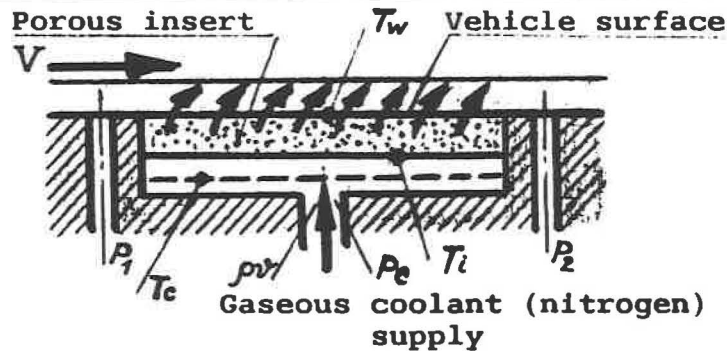
AR5: Thermal and Gas - dynamic Tests

- \* Diagnostics of heat transfer boundary conditions and heat loads on structures during full-scale testing
- \* Identification of thermal properties of heat-shield materials

AR6: Thermal - vacuum Test of Spacecrafts

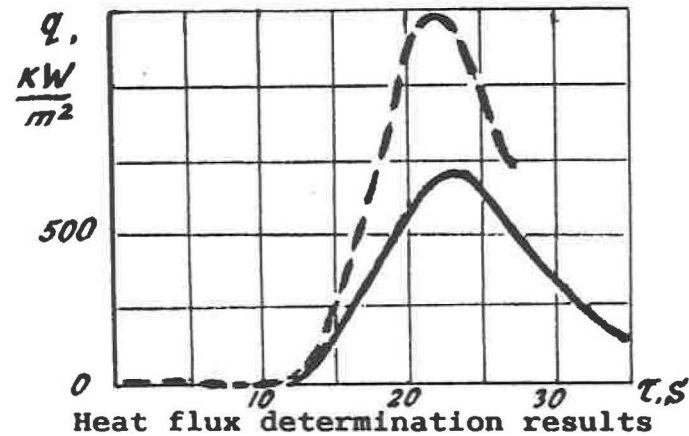
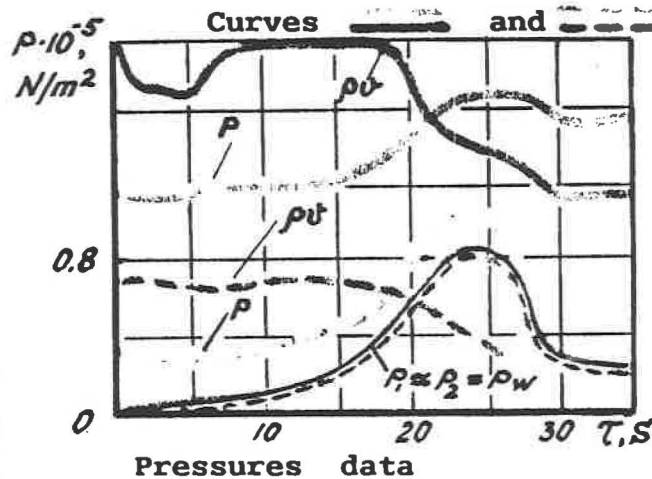
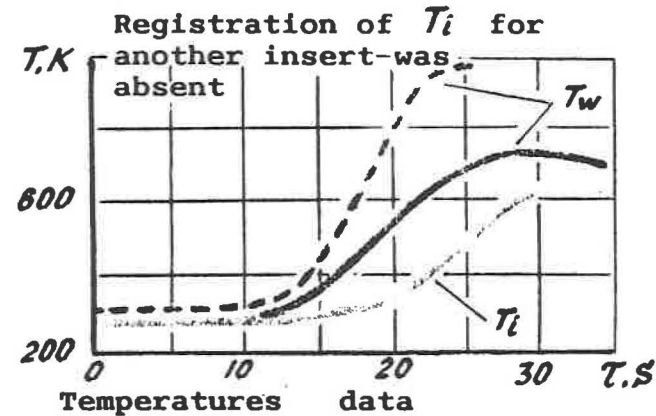
#### PROCEDURE OF TESTING

1. Special preliminary testing of object for the purpose of identification and correction of mathematical models of heat transfer processes
2. Choice of thermal simulator mode ( inverse problem of control type )
3. Regular testing



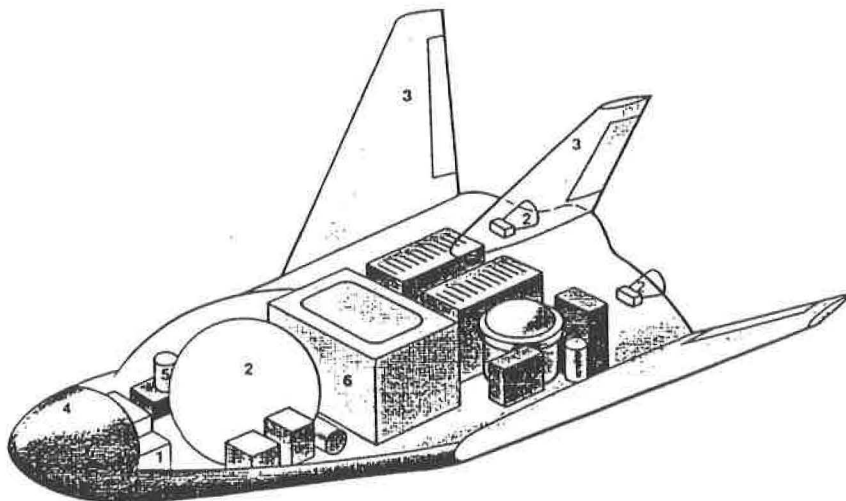
Equipment for investigation of porous cooling

Pressures before ( $P_1$ ) and after ( $P_2$ ) the insert, and pressure of the coolant supply ( $P_c$ ), temperatures of outer ( $T_w$ ) and inner ( $T_i$ ) surfaces, and temperature of supplied coolant ( $T_c$ ), and mass flow rate of coolant ( $\rho v$ ) are measured values.

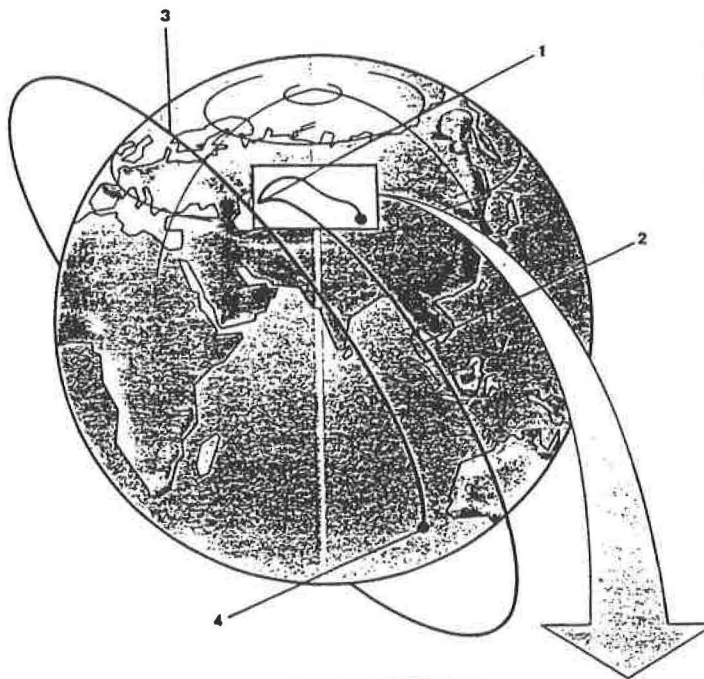


## THE FLIGHT-TEST COMPLEX "BOR"

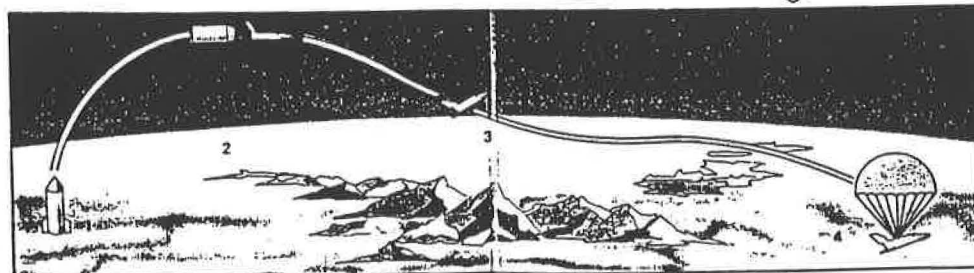
THE COMPLEX FOR FLIGHT RESEARCHES INTO THE PROBLEMS OF AERODYNAMICS, FLIGHT DYNAMICS AND THERMAL PROTECTION OF FUTURE AIR-SPACE PLANES.



1. Power supply source
2. System for gas-dynamic stabilization in space
3. Aerodynamic controls
4. Elements of thermal insulation being tested
5. Research equipment
6. Rescue system
7. Navigation and control system
8. System of radiotelemetry



1. Launch
2. Injection into orbit, separation from booster
3. Atmospheric portion of flight trajectory
4. Rescue on parachute



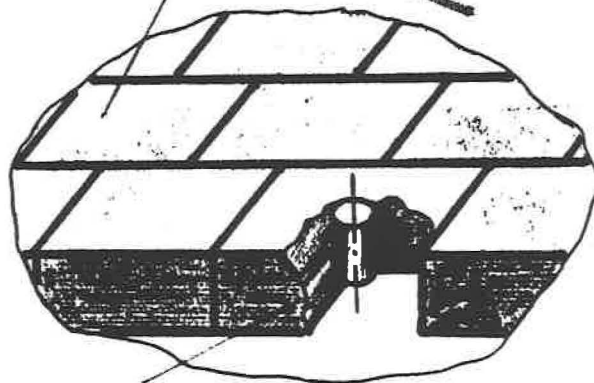
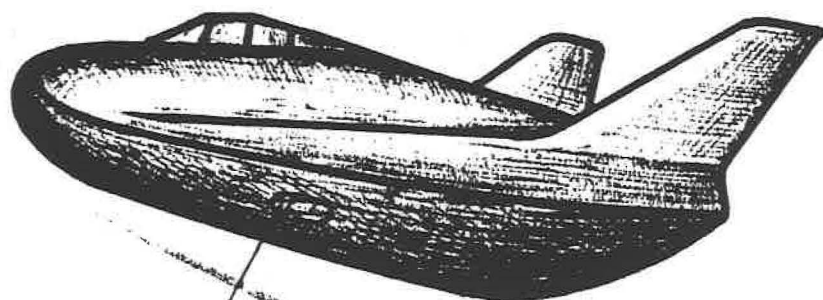
TP  
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AR 8 : Study of thermal modes at course of flight tests  
of "Bor-4" automatic re-entry vehicle

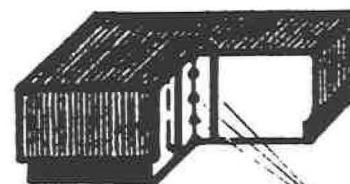
3/10

**B o r - 4**

Tiles with different sensors:

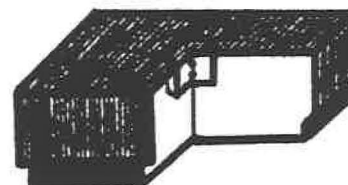


tile with  
sensor

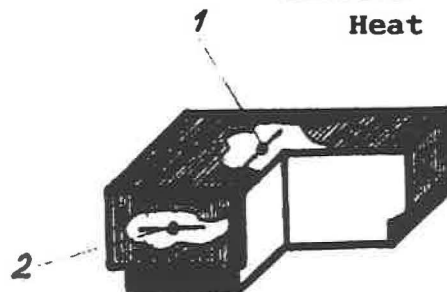


termocouples

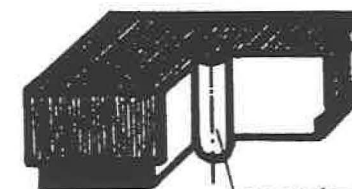
Temperature distribution



Heat flux



Temperatures of outer (1)  
and side (2) surfaces

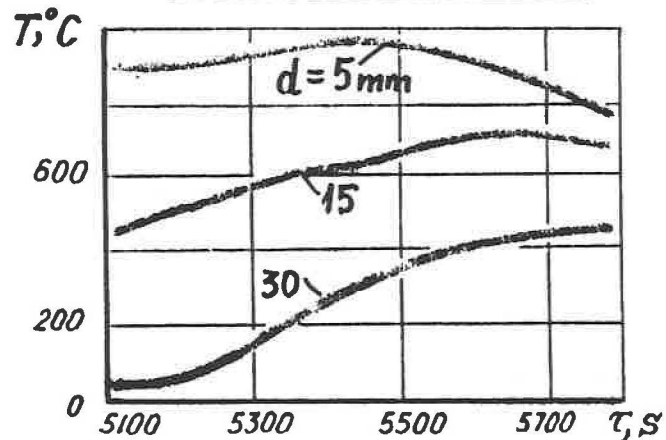


quartz  
pipe

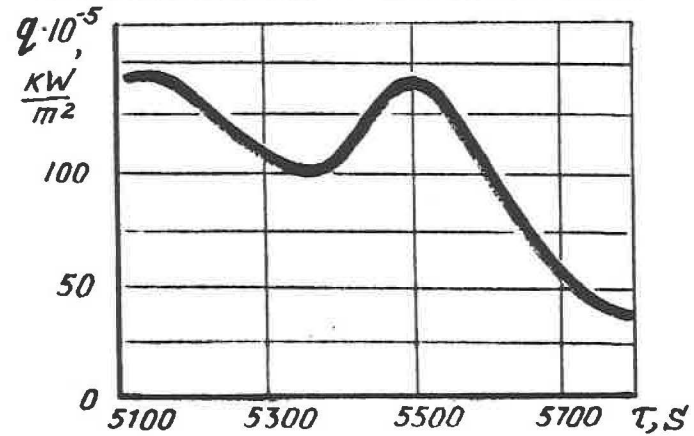
Pressure



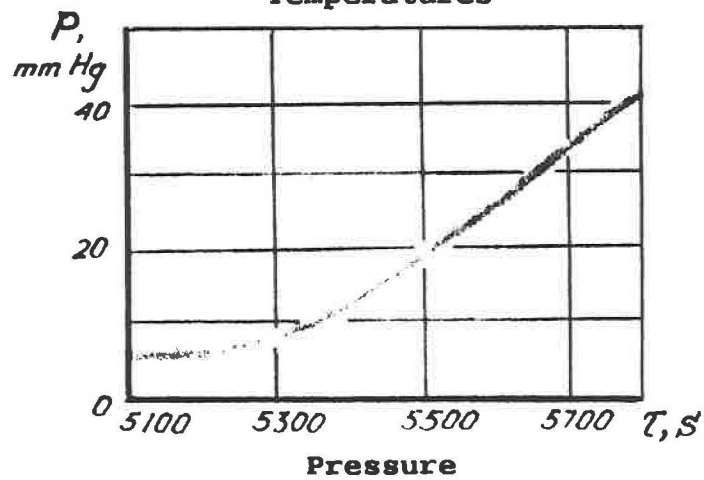
Direct measurements :



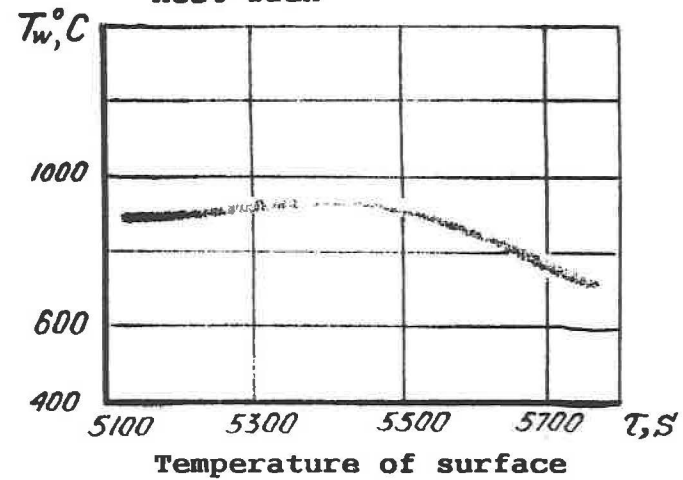
Results of solving of I H C P :



Temperatures



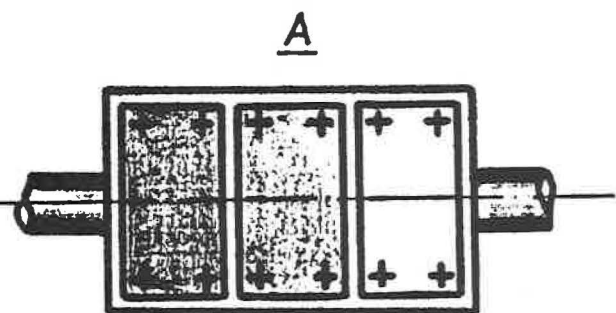
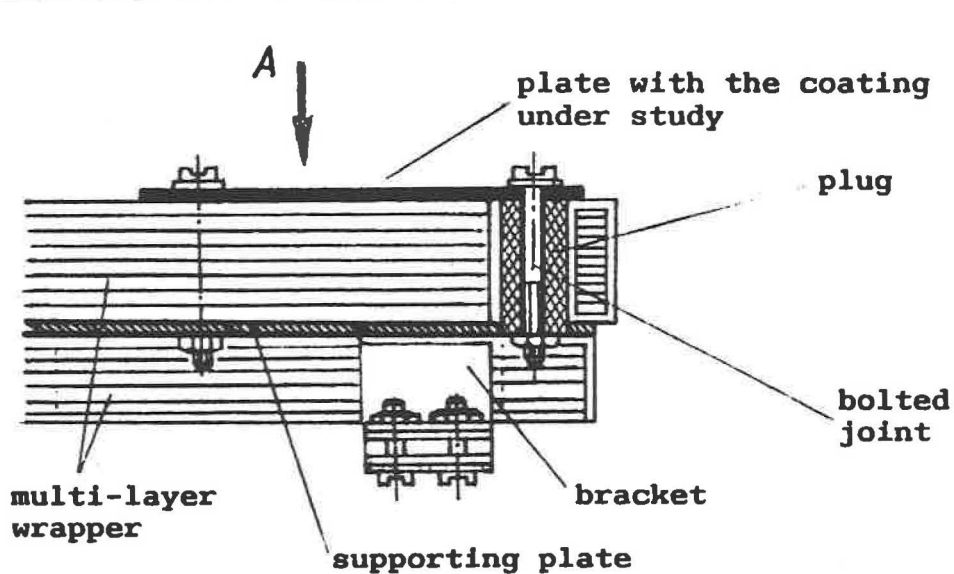
Heat flux



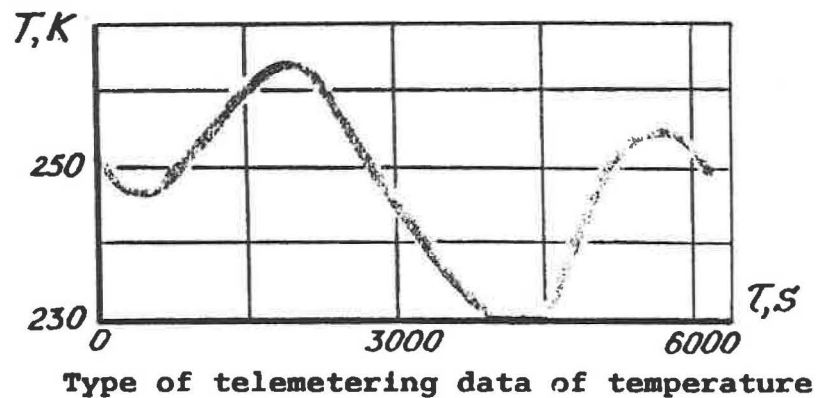
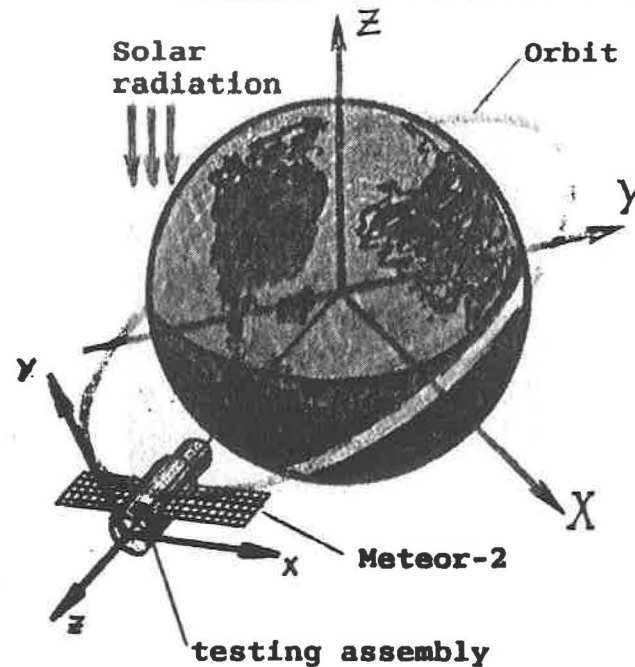
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AR9: Study of stability of the thermocontrol coating (TCC) of spacecraft at orbit conditions

3/12



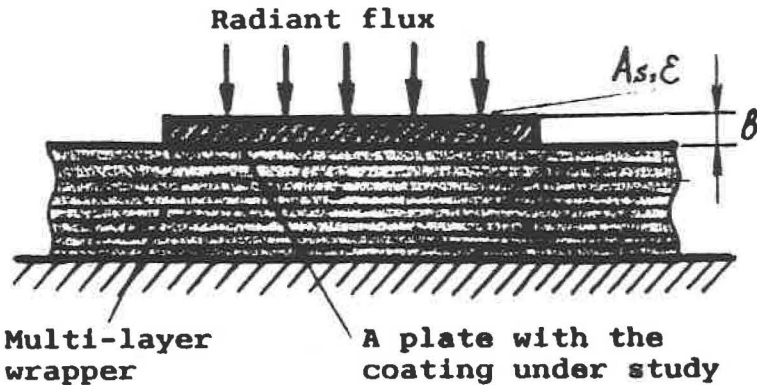
Assembly of the three specimens with different coatings



Example 3 : The Diagnostics of radiation characteristics  
 -----  
 of thermal control coatings

TP  
1

1 / 15



Mounting of a specimen on the  
surface of a spacecraft

The unknown quantities:

$A_s$  is a solar radiation integral absorptivity factor,

$\epsilon$  is an integral semi-spherical emissivity

Mathematical model:

$$C_m \frac{dT}{d\tau} = A_s [q_s(\tau) + q_R(\tau)] + q_E(\tau)\epsilon - \epsilon\sigma_0 T^4(\tau)$$

$$\tau \in (0, \tau_m), \quad C_m = C_p \rho \beta ;$$

$$T(0) = T_0$$

Experimental values of the temperatures:

$$f(\tau_i) = T(\tau_i) + \xi_i ,$$

$$i = \overline{1, N}, \quad \xi_i \text{ are measurement errors}$$

$q_s$  is a direct solar radiation,

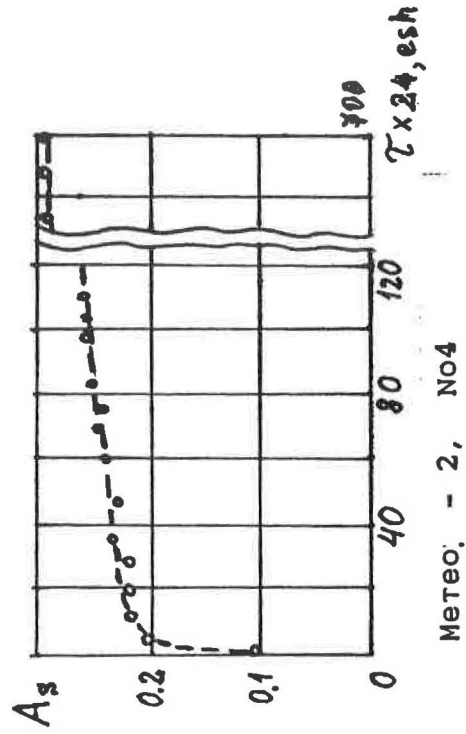
$q_R$  is a reflected from the Earth solar radiation,

$q_E$  is an Earth self-radiation

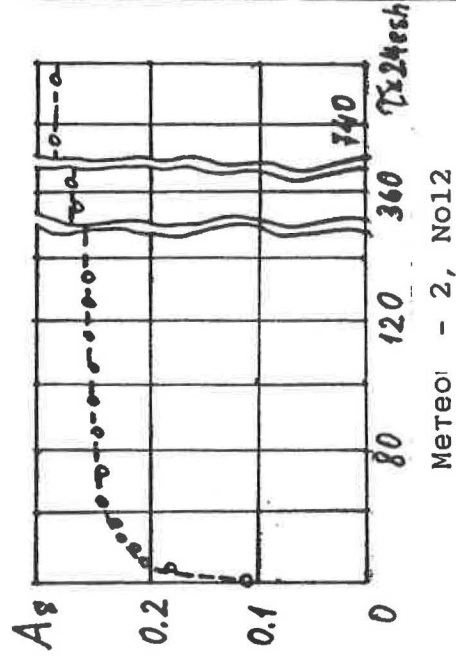
Continuation

27

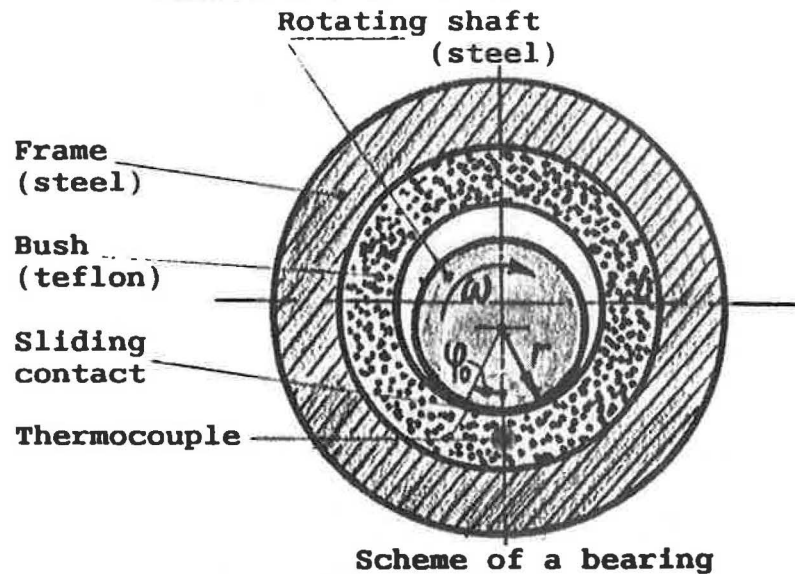
Experimental Results



TCC : 050



TCC : on base of Teflon



There is sources of heat in the contact zone ( $-\psi_0 < \psi < \psi_0$ ):

$$Q(\psi, \tau) \approx Q(\tau) \text{ at } \omega > 5 \text{ rad/s}$$

$$Q(\tau) = 2 r_1 \psi_0 q(\tau)$$

- is determined from IHTP solution

Specific rate of heat flow:

$$q(\tau) = k_f p(\tau) v(\tau),$$

where  $k_f$  is a friction coefficient;  
 $p$  is a pressure in sliding contact;  
 $v$  is a sliding velocity

Friction moment:

$$M_f(\tau) = Q(\tau) \cdot r / v$$

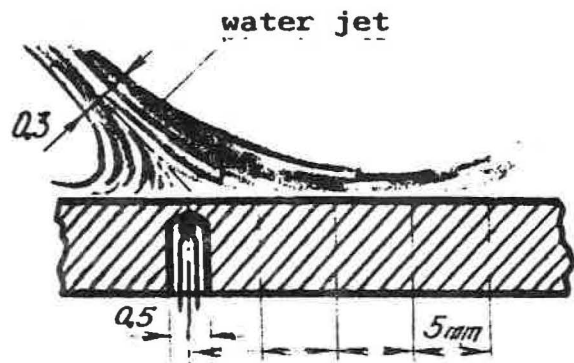
EXPERIMENT:

$v = 0.39$  m/s ; diameters of the bush:  $\phi 32 \times \phi 26$  mm  
 diameter shaft:  $\phi 25.5$  mm

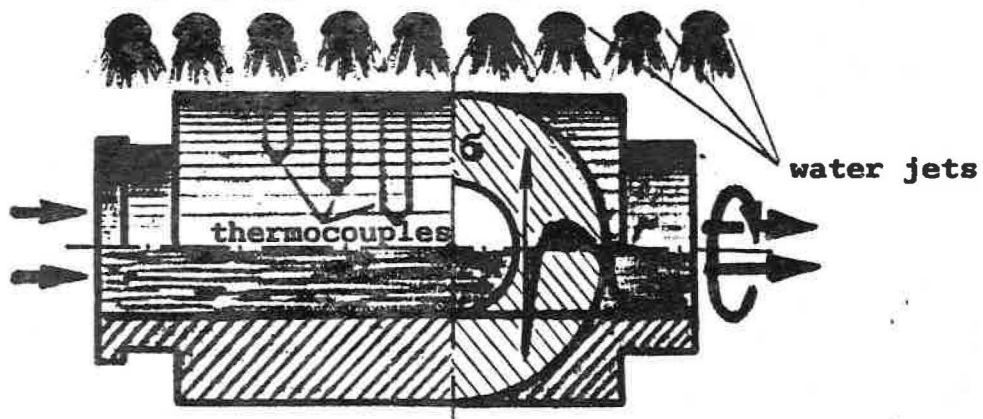
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AR 11: An experimental study of the cooling of hot metal with water jets

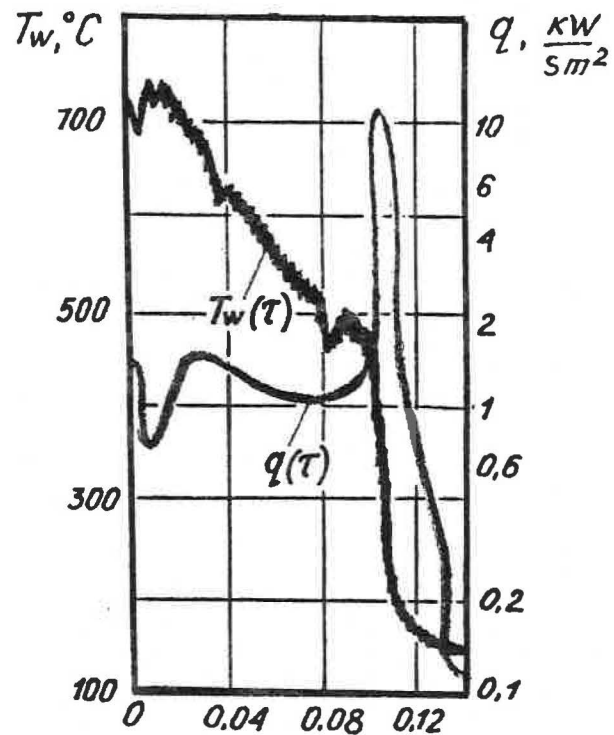
3/16



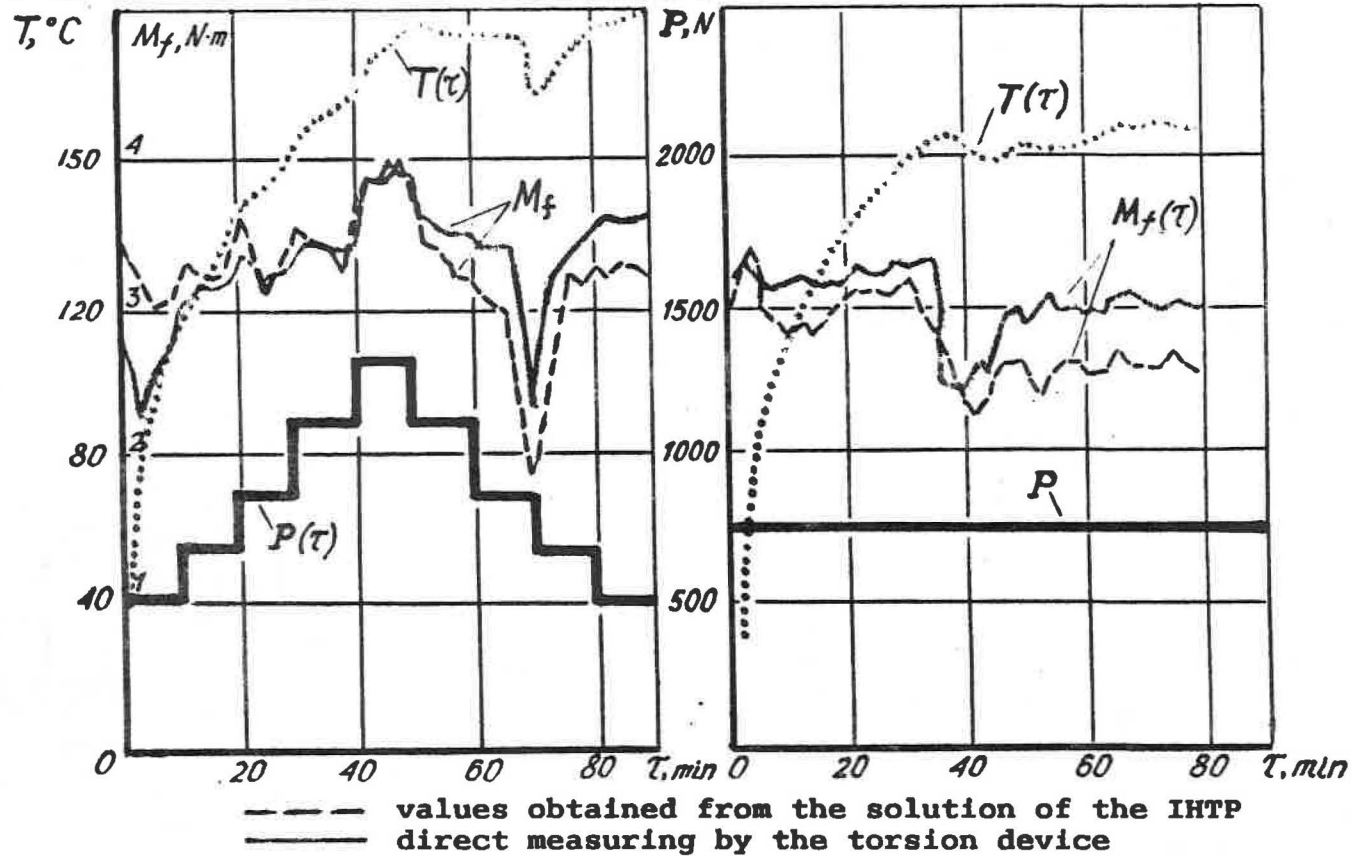
The cooling of high-temperature steel strip equipped with temperature sensors



Thermal treatment of steam turbine rotors



Surface temperature and heat flux at cooling steel strip



Results of determination of the friction moment  
 ( P is a load on rotating shaft )